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INVESTIGATION OF THE IRON OXIDATION KINETICS  
IN MANTUA RESERVOIR

by

Scott H. Lathen

A thesis submitted to the faculty of

Brigham Young University

in partial fulfillment of the requirements for the degree of

Master of Science

Department of Civil and Environmental Engineering

Brigham Young University

August 2007



BRIGHAM YOUNG UNIVERSITY

GRADUATE COMMITTEE APPROVAL

of a thesis submitted by

Scott H. Lathen

This thesis has been read by each member of the following graduate committee and by majority vote has been found to be satisfactory.

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BRIGHAM YOUNG UNIVERSITY

As chair of the candidate's graduate committee, I have read the thesis of Scott H. Lathen in its final form and have found that (1) its format, citations, and bibliographical style are consistent and acceptable and fulfill university and department style requirements; (2) its illustrative materials including figures, tables, and charts are in place; and (3) the final manuscript is satisfactory to the graduate committee and is ready for submission to the university library.

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## ABSTRACT

### INVESTIGATION OF THE IRON OXIDATION KINETICS IN MANTUA RESERVOIR

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Master of Science

Irrigation of the municipal cemetery in Brigham City, Utah resulted in stained headstones in 2001 and 2002. The water used in the irrigation came from Mantua reservoir, a medium sized impoundment situated near the mouth of Box Elder Canyon. In order for Brigham City to establish a city wide secondary pressurized irrigation system using water from Mantua reservoir, the cause and the source of staining problem must be determined. Previous research (Wallace 2006) determined that the source of the staining was the reduction of iron found in Mantua Reservoir sediments that occurred when seasonal variations in the reservoir caused anaerobic conditions. The reduced iron then dissolved in the water and was used in the irrigation system, causing re-oxidation of the iron. The oxidized iron then precipitated out on the headstones causing the staining. The





purpose of this investigation is to determine the iron oxidation kinetics after the re-aeration of the water which will help determine appropriate mitigation methods. A secondary purpose is to confirm the Mantua reservoir's capacity to become anaerobic, resulting in the conditions which cause staining.

Using laboratory investigations and computer modeling, I determined that on re-aeration, fifty percent of the dissolved iron in the water precipitates in five hours. Using first-order kinetics to model this process, I found the rate constant of the kinetic reaction to be  $0.0029 \text{ min}^{-1}$ . Fitting a geochemical computer model of the iron oxidation kinetics in Mantua reservoir, which uses a higher-order kinetics model to better model this process, to experimental kinetic data yielded a rate constant of  $4 \times 10^{13} / \text{atm} \times \text{min}$ .

I also recreated the staining process in the laboratory using concrete. This was successful and provided visual evidence that the iron precipitates out of the water and stained the concrete within a couple of hours of application. Field data collected from Mantua reservoir showed that the dissolved oxygen concentration in the reservoir drops regularly below levels consistent with equilibrium to the atmosphere. While my field measurements did not record anaerobic conditions, based on the patterns shown, this study shows that it would be possible for anaerobic conditions to occur during warmer weather.



## ACKNOWLEDGMENTS

First, I wish to thank Dr. Gus Williams for his advice and technical assistance throughout the entire duration of this study. I would also like to thank Rob Wallace for finding this project and conducting the initial research that provides the basis for this study.

The project was funded in its entirety by the Division of Public Works of Brigham City, Utah.

Finally, I would like to thank my wife for her support and her sacrifice to support and assist me in this project.



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# 1 Introduction

Brigham City, Utah installed a pressurized irrigation system to provide more effective water use and make irrigation more efficient. The system was restricted to just irrigating the city cemetery in the initial installation, though expansion to the rest of the City was planned. The system ran without serious problems until 2001, when workers found the headstones in the municipal cemetery were stained a dark reddish brown (Bigelow 2002). Ferric iron ( $\text{Fe}^{3+}$ ) had precipitated from the irrigation water, caused the staining on the headstones, and is the source of the red color of the stain (Wallace 2006). The water used in the pressurized irrigation system comes from Mantua Reservoir.

After the first appearance of the staining, the city shock treated the pipeline with bactericides in order to eliminate a biofilm observed to be lining the pipes. At this time, it was thought that the biofilm was the main factor causing the staining. The city also introduced iron and manganese sequestering agents, as well as chlorinated the water in an effort to prevent a recurrence of the staining. The staining did not occur during the remainder of that watering season, however the staining did return during the 2002 irrigation season despite the continued water treatments initiated the previous year.

Due to the continued staining from the system, Brigham City refrained from using Mantua water in the irrigation system and has switched to culinary water (Bigelow 2002).

Figure 1-1 is a photograph taken from the Brigham City cemetery sexton's report on the staining.



**Figure 1-1: Headstone staining (Wood 2002)**

The staining has not occurred in a predictable pattern or at a constant frequency and it has been difficult to establish common links between the staining events, this caused significant difficulty in determining the source and cause of the staining so they

can use the Mantua water in the pressurized irrigation system and expand the irrigation system beyond the cemetery.

In 2005, Brigham City initiated a feasibility study to explore the possibility of creating a city wide pressurized irrigation system. Mantua Reservoir was identified as one potential and preferred source for the irrigation water (Bigelow 2005). This proposed expansion is not feasible using water from Mantua Reservoir until the threat of iron staining is removed. The city wants to understand the source of the staining, the mechanisms and situations that cause staining, and develop potential measures that can be taken to eliminate or minimize the problem.

### **1.1 Mantua Reservoir Background**

Mantua Reservoir, shown in Figure 1.2, is a medium-sized reservoir located at the top of Box Elder Canyon just east of Brigham City. Table 1-1 summarizes the significant attributes of Mantua Reservoir (Loveless *et al* 1997).

**Table 1-1: Attributes of Mantua Reservoir**

Elevation (ft):	5159
Surface Area	554
Watershed Area	5559
Capacity (acre-	10450
Mean Depth (ft):	14
Max Depth (ft):	20
Length (miles):	1.12
Width (miles):	1.02
Shoreline (miles):	2.1

Mantua Reservoir is a shallow reservoir that has a fairly large surface area. These two characteristics make the water unusually warm, exceeding the state guidelines of 20°C for a cold water fishery, promoting the growth of a myriad of aquatic life (Loveless *et al* 1997). Mantua also has a high loading of nutrients including phosphorus loadings that usually exceed regulations. The reservoir, shown in Figure 1-2, supports large blooms of blue-green algae and the production of macrophytes. The large quantity of aquatic organisms contributes to a low amount of dissolved oxygen (DO) in the system (Loveless *et al* 1997). The lake's beneficial use classification is 3A, a cold water fishery, 2B, for recreational use, and 4, protected for agricultural irrigation uses (Utah Department of Environmental Quality 2000).



**Figure 1-2 : Mantua Reservoir**

In the course of the Clean Lakes Study (Loveless *et al* 1997) it was observed that during the period from May to September, the DO concentration within one meter of the reservoir bottom was depressed below acceptable levels which were 3.0 mg/L. The DO conditions improved between July 18<sup>th</sup> and August 10<sup>th</sup> because of increased wind action, resulting in better mixing in the reservoir, mixing the aerated surface water with the lower waters. The low DO concentrations in the summer resulted from the hot stagnant conditions, decomposition of organic matter, and photosynthesis by aquatic vegetation (Loveless *et al* 1997).

The area surrounding the reservoir contributes to the characteristics in Mantua Reservoir that result in low DO. The Mantua Fish Hatchery is located at the head waters of Maple Creek, a major contributor to Mantua Reservoir. The hatchery is a major point source for total phosphorus loading to the reservoir which supports the high level of biological activity observed. Also of significance to this study is the composition of the sediments surrounding the reservoir and forming the bed of the reservoir. These sediments have a very high quantity of iron (III) minerals in the soil. Loveless *et al* (1997) gives the iron concentration in the lake bed sediments as 16,600 and 13,300 (mg/kg) respectively in the North and South arms of the reservoir. Wallace (2006) found the concentration of ferric iron in the reservoir sediments to be 16,500 mg/kg dry weight in sediment samples taken near the outlet and dam.

Big Creek is the outlet for Mantua Reservoir and has an average flow of 21 cubic feet per second. Brigham City captures Big Creek at the reservoir outlet and pipes the water into the city for power and irrigation uses. The head difference between the



reservoir and the city also allows the water to be used as a power generating source (Loveless *et al* 1997).

Previous research by Wallace (2006) determined that the iron found in the sediments of Mantua Reservoir is responsible for the staining of the Brigham City. The research concluded that when conditions cause the hypolimnion of the reservoir to become anaerobic, the ferric iron in the sediments is reduced to ferrous iron. Ferrous iron has a solubility constant sixteen orders of magnitude higher (Sawyer *et al* 2003) than ferric iron and therefore readily dissolves into the reservoir water. This dissolution process is catalyzed by biological activity which greatly increases the rate at which the iron dissolves. The iron-rich water is then taken into the reservoir outlet and piped to Brigham City in a closed system that is not re-aerated. When the iron saturated water leaves the Brigham City irrigation system and is sprayed onto the cemetery lawn, the water is re-aerated causing the ferrous iron to oxidize to ferric iron. At this point, the water becomes over saturated with respect to iron which then precipitates onto the headstones of the cemetery causing the observed staining (Wallace 2006). The reason the observed staining occurred intermittently was because the exact conditions which would cause the reservoir to go anaerobic are not common. These conditions occur at night during low-water, high-temperature, and low-wind conditions. Under these conditions degradation of biological matter in the reservoir uses the available oxygen and under these conditions there is no mechanism for re-aeration of the hypolimnion waters at the bottom of the reservoir.

## 1.2 Objectives

The objective of my research is to determine the kinetics of the oxidation of ferrous iron to ferric iron and the subsequent precipitation of the ferric hydroxides, the source of the staining in Brigham City. Understanding the kinetics of this reaction will allow various treatment and mitigation alternatives to be evaluated. Previous research (Wallace 2006) determined that iron in the reservoir water does undergo reduction and oxidation based on the dissolved oxygen conditions in the water and is potentially catalyzed by microorganisms, speeding up the dissolution of the iron from the sediments to the water. The knowledge of the iron chemistry which occurs and causes this problem allows Brigham City to focus on remediation of the iron at the source. Modeling the kinetics of the oxidation reaction will allow Brigham City to choose the most effective treatment method and aid in design of a chosen treatment system.

In order to determine the reaction kinetics, I have used both experimental procedures and theoretical models. The experimental approach involved taking water and sediment samples from Mantua and allowing them to go anaerobic. The anaerobic conditions forced the reduction of ferric iron found in the sediments allowing the newly formed ferrous iron to dissolve in the water. I then re-aerated the water, causing the oxidation of the ferrous iron back to the ferric state, and recorded the amount of ferrous iron remaining after established time periods had elapsed. By repeating the experiment at various times, I generated a rate curve which describes the iron oxidation kinetics for the combination of Mantua Reservoir water and sediments.

In an effort to confirm the findings of Wallace (2006) who determined the staining mechanism, I recorded the reservoir DO levels over an extended period of time

to determine if DO levels near the bottom of the reservoir were significantly depleted at night. Also using the water and sediment samples collected from the reservoir I have replicated the staining seen in the Brigham City cemetery.

I developed the theoretical geochemical model using PHREEQC, developed by Parkhurst and Appelo (1999), to model the oxidation kinetics. The parameters used to create and define this model were taken from the Clean Lakes Study (Loveless *et al* 1997) performed on Mantua Reservoir. After the development of a preliminary model based on these data, I used the experimental data obtained from the laboratory procedures using Mantua Reservoir water and sediments to refine the model to fit the measurements I had which characterize Mantua Reservoir. A model of the iron oxidation kinetics allows a number of different scenarios to be evaluated and recommendations can be made to determine the treatment options available to Brigham City.

## **2 Chemistry**

### **2.1 Chemical Conditions of Mantua Reservoir**

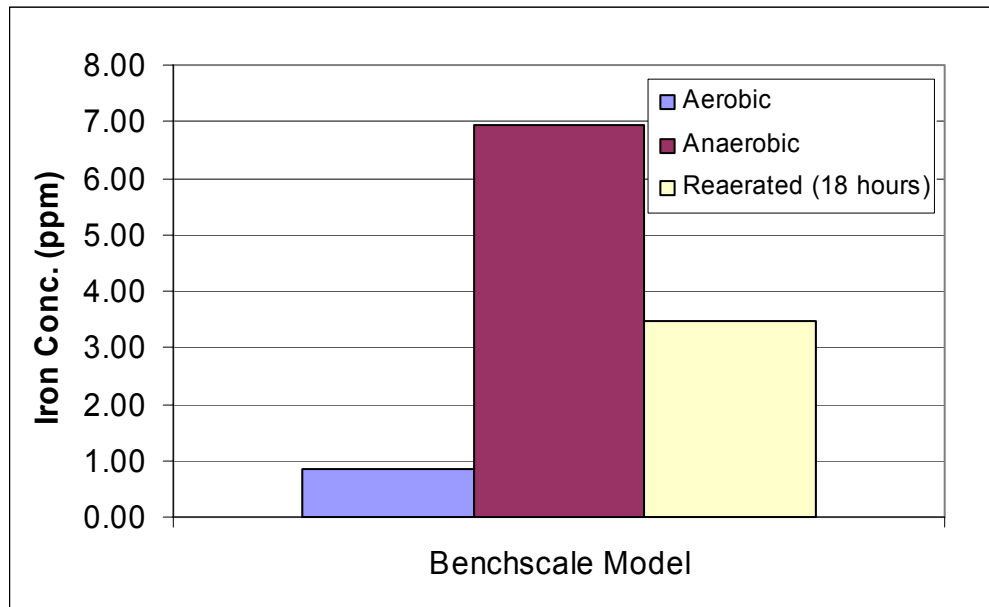
Previous studies conducted on Mantua Reservoir (Loveless *et al* 1997 and Wallace 2006) determined the general geochemistry that governs the reservoir. The Clean Lakes Study (Loveless *et al* 1997) described the nutrients, metals, and chemicals found in the reservoir, the inlets to the reservoir, and in the sediments forming the lake bed. Of particular interest to my research is the amount of iron that was found in the sediment and water of the reservoir and the DO conditions of Mantua. The study found that iron levels in the reservoir water averaged less than 20 µg/L over the course of the study. However, the iron levels in the lake bed sediments were quite high in both the north and south arms of the reservoir with measurements of 16,600 mg/Kg and 13,300 mg/Kg respectively (Loveless *et al* 1997).

The Clean Lakes Study (Loveless *et al* 1997) also recorded the DO in Mantua Reservoir. The DO levels found in this study were a source of extra concern during the summer months, May through September, because they were low. This is the same time of the year as when the cemetery staining occurred. During these months the DO was measured to be less than 3.0 mg/L within one meter of the reservoir bottom. The water above one meter from the bottom generally had measured DO levels within acceptable parameters. Exceptions occurred on several days, most notably July 18<sup>th</sup>, when low DO

levels were measured farther from the reservoir bottom. On July 18<sup>th</sup> the DO was measured at only 1.0 mg/L two meters from the bottom. This indicates that under some conditions, the DO levels in the bottom of the reservoir could become anaerobic.

Research by Wallace (2006) concluded that low DO, especially completely anaerobic conditions, would cause the iron in the sediments to reduce to the ferrous state and dissolve in the reservoir water. Iron reduction is a geochemical process that is probably accomplished by the microorganisms in the water using iron (III) as the terminal electron acceptor instead of oxygen (Sawyer *et al* 2003). This biological process also speeds up the iron dissolution. Ferrous iron ( $\text{Fe}^{2+}$ ) has a solubility product (ksp) that is fifteen orders of magnitude higher than ferric iron allowing the ferrous iron to dissolve into the reservoir water at significantly higher amounts that are possible under aerated conditions (Sawyer *et al.* 2003). Once the anaerobic reservoir water, with the dissolved ferrous iron, is re-oxygenated, such as through the action of being sprayed out of a sprinkler system, the iron (II) oxidizes to form the insoluble iron (III) which is over-saturated with respect to iron. The excess iron then precipitates as ferric hydroxide compounds causing the staining observed in the cemetery (Wallace 2006). In order to characterize and replicate these natural conditions Wallace (2006) collected water and sediment samples from Mantua. These samples were placed in BOD bottles, allowing the water to become anaerobic. The bottles were opened and DO was measured to confirm anaerobic conditions. At this point the water was stirred in order to accomplish aeration. At each stage, the original water, the anaerobic water in contact with the sediments, and the re-aerated water, the concentration of ferrous iron in solution was measured using the phenanthroline method and a spectrophotometer. Figure 2-1 is a bar

chart showing the concentration of ferrous iron in the water under the various DO conditions measured in this study to characterize the processes observed using water and sediment collected at Mantua reservoir.



**Figure 2-1: March 31st results (Wallace 2006)**

The water under anaerobic conditions contains a significantly higher concentration of ferrous iron, this represents the conditions that could occur during warm, wind-free summer nights at Mantua. Upon re-oxygenation the ferrous iron concentration in solution drops from almost 7 ppm to about 3.5 ppm, the iron is precipitated from solution. This drop in iron concentrations from the anaerobic water conditions to the re-aerated water conditions is attributed to the oxidation of the ferrous iron creating insoluble ferric iron that precipitates out of the reservoir water and causes the problematic staining on the headstones (Wallace 2006).

## 2.2 Iron Oxidation Kinetics

The research of Wallace (2006) demonstrated that the mechanism for the headstone staining was the change in the aerobic condition of the water and the subsequent reduction and oxidation of the iron found in the lake bed sediments. In addition to knowing the staining mechanism, it is important to know the kinetics of the reaction in order to provide treatment recommendations.

Only minor changes in environmental conditions are necessary to initiate the oxidation or reduction of iron in natural systems (O'Neil 1985). The mixing of oxygen, at even small amounts, with the ferrous iron oxidizes the iron, forming the insoluble ferric iron ( $Fe^{3+}$ ) which then will precipitate out of the water and cause staining (Sawyer et. al. 2003). Equation 2-1 is the reaction describing the oxidation of ferrous iron and the precipitation of ferric hydroxides:



Iron oxidation kinetics has been vigorously studied resulting in established mathematical models used to predict the rate of iron oxidation in various systems. Singer and Stumm (1970) investigated iron oxidation kinetics, determining that the rate of oxidation follows a predictable model. Their research yielded the widely accepted equation (equation 2-2) describing the kinetics of ferrous iron oxidation.

$$\frac{-d[Fe^{2+}]}{dt} = k[Fe^{2+}][OH^-]^2 P_{O_2} \quad (2-2)$$

$P_{O_2}$  is the partial pressure of the atmospheric oxygen exerted on the water surface and can be replaced with the DO concentration in the water (Stumm and Lee 1961). The rate constant,  $k$ , varies with the experimental method used to determine it. Equation 2-2 is first order with respect to the ferrous iron concentrations and second order with respect to the concentration of the hydroxyl ions. As a result, the greater the pH of the water, the faster the ferric iron forms and can precipitate (Houben 2004). Table 2-1 summarizes different values used for the rate constant.

**Table 2-1: Rate Constants for Iron Oxidation<sup>2</sup>**

Rate Constant <sup>1</sup> k (1/mol <sup>3</sup> x min)	Temperature (°C)	Reference
0.8-1.7x10 <sup>16</sup>	10	Davison and Seed (1983)
1.4x10 <sup>16</sup>	25	Tamura et al. (1976)
0.7x10 <sup>16</sup>	10	Millero et al. (1987)
1.7(±0.4)x10 <sup>16</sup>	10	Laxen and Sholkovitz (1981)
6.0x10 <sup>16</sup>	25	Stumm and Morgan (1996)

<sup>1</sup> rate constant for concentration of dissolved oxygen

<sup>2</sup> Modified from Houben (2004)

Equation 2-2 can be arraigned to be a function of pH instead of the hydroxyl ion concentrations (Houben 2004). This results in equation 2-3 which shows the oxidation rate as a function of both the DO concentration and the pH (or [H<sup>+</sup>]):

$$\frac{-d[Fe^{2+}]}{dt} = k[Fe^{2+}][H^+]^2[O_{2(aq)}] \quad (2-3)$$



where  $k$  is the kinetic rate constant,  $[\text{Fe}^{2+}]$  is the concentration of the ferrous iron dissolved in the water,  $[\text{H}^+]$  is the concentration of the hydrogen ions, and  $[\text{O}_{2(\text{aq})}]$  is the concentration of DO in the aqueous solution. At pH values less than 3.5, the rate of iron oxidation is independent of the pH and that term is dropped from the equation. When this term is dropped, the rate constant increases to  $1.0 \times 10^{-7}$  (Singer and Stumm 1970).

Since the oxidation of ferrous iron is proportional to the concentration of ferrous iron in the reservoir, when other parameters are held constant, first-order kinetics can be used to determine the experimental rate constant ( $k$ ). Equation 2-4 is the equation that describes these first-order kinetics (Sawyer *et al* 2003).

$$C = C_0 e^{-kt} \quad (2-4)$$

where  $C$  is the final concentration of the substance,  $C_0$  is the initial concentration at  $t = 0$ ,  $t$  is the time that the reaction proceeds, and  $k$  is the kinetic rate constant for the reaction. It should be noted that while all these equations use  $k$  as the rate constant, it is different for each equation used.

### 2.3 Factors Affecting Iron Oxidation Kinetics

A number of factors can influence the rate of ferrous iron oxidation (Liang 1993). Various environmental conditions, the presence of other ions, and the presence of iron oxidizing bacteria can all increase the rate of oxidation. Of the possible environmental factors, an increase in pH has the most dramatic effect on the kinetics of the system. A unit increase in the pH will result in a 100-fold increase in the oxidation rate of the

ferrous iron (Morgan and Stumm 1996). Though less dramatic, a 15 degree Celsius change in the system, for a constant pH, will result in a 10-fold increase in the oxidation rate (Morgan and Stumm 1996). At high pH levels, greater than 7, the oxidation of the soluble ferrous iron in the system can happen in just minutes (Appelo and Parkhurst 2005). The increased oxidation rate resulting from a higher pH is a consequence of enhanced electron-transfer capacity (Houben 2004).

The presence of other metal ions can also have a catalytic effect on the oxidation of ferrous iron; particularly  $\text{Cu}^{2+}$  and  $\text{Co}^{2+}$  in trace amounts increase the reaction rate (Morgan and Stumm 1996). Other anions that form complexes with iron will also speed up the reaction (Morgan and Stumm 1996). Of particular note, when ferric iron is added to the water, it acts as a catalyst for the ferrous to ferric iron reaction (Tamura *et al* 1976). As a result, the more ferrous iron oxidized to the ferric state, the faster the reaction proceeds. Tamura *et al* (1976) proved that the catalytic effect of ferric iron happens as the ferrous iron in solution sorbs onto the suspended ferric iron particles. The ferrous iron is then oxidized on the surface of the ferric iron particles. Rising pH linearly increases the sorption of ferrous iron due to the higher amount of negative surface charge of the oxide. The increased rate of oxidation from the inclusion of ferric iron in the system leads to a new kinetic model based on equations 2-2 and 2-3 (Tamura *et al* 1976). Equation 2-5 is the revised kinetic model:

$$\frac{-d[\text{Fe}^{2+}]}{dt} = k_1 [\text{Fe}^{2+} [\text{H}^+]^{-2} [\text{O}_{2(aq)}] + k_2 [\text{Fe}^{3+} [\text{Fe}^{2+} [\text{H}^+]^{-2} [\text{O}_{2(aq)}] \quad (2-5)$$

where  $k_2$  is the product of the equilibrium constant for the sorption of  $\text{Fe}^{2+}$  onto ferric oxide and the rate constant of the oxidation at the surface. The value of this constant is given as  $1.71 \times 10^{-5}$  mol/min (Tamura *et al* 1976). Equation 2-5 indicates that the pH has a more significant impact on the homogenous portion of the equation than on the heterogeneous part. Therefore the effect of ferric iron on the reaction rate is more important at lower pH levels. The catalytic effect of ferric iron is significant only when the concentrations of ferrous iron is greater than 3 mg/L otherwise there is insufficient catalytic surface to greatly impact the kinetics (Tamura *et al* 1976). This implies that once precipitation and staining start, it will proceed rapidly.

In addition to metal ions and physical environmental conditions, the presence of iron oxidizing bacteria will significantly increase the rate of the reaction (Okereke and Stevens 1991), just as iron-reducing bacteria can significantly increase the dissolution rate from the sediments (Wallace 2006). The presence of microbes can accelerate the reaction rate by a factor of  $10^6$  (Singer and Stumm 1970). *Thiobacillus ferrooxidans* are the bacteria most responsible for the oxidation of ferrous iron in low DO conditions. *T. ferrooxidans* are acidophilic chemolithotrophs that will increase the oxidation rate of  $\text{Fe}^{2+}$  when the pH values in the water fall below 3.5 (Okereke and Stevens 1991). The effect of the microbes on the kinetics of the reaction varies greatly depending on the environmental conditions present. Included in the variables which can affect the system is the actual concentration of the bacteria present in the system. An increase in the concentration of *T. ferrooxidans* results in an increase in the rate of the reaction. Equation 2-6 describes the oxidation rate of ferrous iron based on the bacterial

concentration, the ferrous iron concentration, and the temperature of the system (Okereke and Stevens 1991):

$$Y = 0.68(B) + 0.02(B)(T) + 1.8 \times 10^{-4}(T^2) - 0.46(B^2) - 5 \times 10^{-5}(F)(T) - 1.2 \times 10^{-3}(F)(B) - 0.22 \quad (2-6)$$

where B is the bacterial cell concentration (mg/mL) and F is the ferrous iron concentration (millimolar) with T being the temperature in degrees Celsius (Okereke and Stevens 1991).



### **3 Methods and Experimental Procedures**

#### **3.1 Sampling Methods and Locations**

In order to determine the kinetic reaction coefficient ( $k$ ) for iron oxidation, water and sediment samples were collected from Mantua Reservoir and used in laboratory procedures to determine the ferrous iron content of the reservoir water at various oxidation states. The water entering the irrigation system is the water of highest concern for this study. The reservoir outlet that supplies the irrigation system is located on the west side of the reservoir. The samples collected for this study were taken from a floating pier, also located on the west side of the reservoir, approximately 100 feet from the reservoir outlet. Figure 3-1 is an aerial photo of Mantua Reservoir. The floating pier (not visible in the figure) is located at the south west corner of the reservoir. The outlet is approximately 100 ft to the north from the pier, along the western shore of the reservoir.

I used a soil auger to remove samples of the reservoir bottom sediments. These samples were taken from the sediments beneath the floating pier. After collecting the sediment samples in buckets, the remainder of each bucket was filled with water collected from the surface of the reservoir. Surface water has low dissolved ferrous iron due to the aerobic conditions present at the water and air interface (Campbell 1989). After collection, the sediment and water samples were transported back to the laboratory for analysis.



**Figure 3-1: Aerial view of Mantua Reservoir**

The samples used in the laboratory procedures were collected on two separate occasions. The first sample set was taken on September 8, 2006 in the early afternoon. The second sampling date was on October 6, 2006 also in the early afternoon. The procedures used for collecting the samples were the same for both days.

### **3.2 Qualitative Procedures**

The first experiments performed were qualitative methods to confirm the findings of Wallace *et al* (2006) that the change in oxidation state of iron found in the lake bed sediments would cause the observed staining by first dissolving then precipitating iron from the sediments. In order to accomplish this objective, samples of water and sediment

from Mantua Reservoir were subjected to the same conditions that we believe are responsible for the staining and the results were documented.

To perform these experiments, first the sediment and water from Mantua Reservoir was transferred to a BOD bottle. The bottle was a standard 300 mL BOD bottle with 1.25 inches of sediment on the bottom and the remainder filled with reservoir water. The BOD bottle was sealed and placed in a dark cabinet, to prevent photosynthesis from generating oxygen. Prior to the transfer of the water and sediment to the BOD bottles, a 16 oz bottle of Sprite was added to the water in the 5 gallon bucket, in order to renew the food source for the microbes. This was necessary to compensate for the delay between the time the water was collected from the reservoir and when it was used in the laboratory procedures. During this time, the bacteria used all the available food initially present in the reservoir water.

After allowing the BOD bottles to sit in the cabinet for three days, to completely deplete the DO, the water was sprayed onto a concrete core sample using a pump, simulating the action of a sprinkler in the Brigham City Cemetery irrigation system. I photographed the concrete core samples immediately before spraying with the Mantua water and several times over the next day to compare the amount of visible staining. These results are presented in Section 5.2.

### **3.3 DO Testing in Mantua Reservoir**

Along with laboratory procedures to confirm the findings of Wallace (2006), we also deployed a sonde in Mantua Reservoir to record the fluctuation of DO levels in the reservoir. The purpose of the DO measurements was to prove that the oxygen state of the



reservoir fluctuates and that the DO levels will reach sufficiently low levels to allow the reduction of ferric iron to soluble ferrous iron (Sawyer *et al* 2003). Wallace (2006) established conditions which could cause staining, but did not confirm that these conditions occur in Mantua Reservoir, which was the goal of these measurements. The data obtained from the sonde was correlated with weather station data in order to prove the hypothesis that temperature and wind conditions (which provides mixing of the reservoir water) contribute to the depletion of oxygen in the lower layers of the reservoir and that under the right conditions, water at the bottom of Mantua Reservoir could become anaerobic, dissolving high levels of iron from the sediments.

I used a YSI 600 OMS (optical monitoring sensor) sonde with an additional DO probe. The sonde is internally powered and capable of storing up to 150,000 bits of data. The DO probe is a YSI 6150 Optical Dissolved Oxygen Sensor. Optical sensors do not require changing a membrane frequently in order to achieve accurate results (YSI Incorporated 2006). Prior to deployment, the sonde and accompanying DO probe were calibrated according to the procedures in the operating manual (YSI Incorporated 2006). The sonde was deployed by swimming underneath the floating pier and using 8 feet of rope to attach it to a brace on the underside of the pier. This positioned the sonde about 2 to 3 feet above the sediment. The sonde was not positioned lower in case the reservoir levels changed during the measuring period, lowering the dock and potentially having the sonde contact the sediments.

The probe was set to record for a period of thirty days starting on September 8<sup>th</sup>, 2006. The sonde took readings every 15 minutes over this time period. The parameters measured were time, temperature, DO concentration, resistivity, total dissolved solids

(TDS), and salinity. Of these parameters, the DO concentration and temperature were the only data used in this study. The probe was retrieved on October 8<sup>th</sup>, 2006 using a DO probe recovery device that I constructed using a broom and an old metal hanger. The data was uploaded from the sonde to a computer and analyzed using the software included with the probe. The results of these measurements and discussions are included in Section 5.1.

### **3.4 Laboratory Procedures**

In order to determine the iron oxidation kinetics of Mantua Reservoir I used the collected samples to determine the kinetics rate constant ( $k$ ). The laboratory procedures involved forcing the water samples to go anaerobic while in contact with the sediments, re-aerating the samples, and simultaneously recording the concentration of ferrous iron remaining in the water during the re-aeration period. The following sub-sections detail the steps required to accomplish each phase of the laboratory procedures.

#### **3.4.1 Anaerobic Conditions**

After transporting the samples from Mantua Reservoir to the lab, they were kept stored in sealed buckets until there was sufficient time to conduct the experimental procedures. The samples collected on September 8<sup>th</sup>, 2006 (the day the probe was deployed) were run on October 21<sup>st</sup>, 2006. The delay between collecting the samples and running the experimental procedures necessitated the addition of a food source for the microbes in order for them to use the available oxygen in the water and aid in the oxidation and reduction processes. The food source added was a 16 oz. bottle of Sprite. The sample bucket, which included two inches of sediment, was then sealed and stored in

a dark refrigeration room at normal room temperature of about 20 degrees Celsius. The bucket and water samples were then left overnight to allow time for the microbes to use all of the DO in the water as well as oxygen in the headspace of the bucket. In order to confirm the anaerobic state of the Mantua water samples, a YSI model DO probe was used to confirm the DO oxygen state of the water, which for these tests was zero.

### 3.4.2 Standards

To measure the concentration of ferrous iron in the Mantua water as it was re-aerated, a set of standards was prepared with known concentrations of iron. These standards were used to create a calibration curve to quantify experimental results.

To create the calibration curve I needed to determine the iron concentration range needed to fit the experimental data. For each trial, conducted with samples gathered on different days, new standards and calibration curves were created. Wallace *et al* (2006) found the maximum concentration of iron to be slightly less than 7 ppm for the samples collected on March 31<sup>st</sup>, 2006 with the minimum being essentially 0 ppm within the ranges of the method used. As a result, the four points I used for the calibration curve were nominally 1 ppm, 2 ppm, 5 ppm, and 8 ppm, which provided a smooth curve and bracketed the iron concentration range I required.

The standards were created by dissolving ferric chloride ( $\text{FeCl}_3$ ) in de-ionized (DI) water in a 1000-mL volumetric flask. In order to achieve an iron concentration of 100 ppm, 0.495 grams of ferric chloride were dissolved in the DI water. This produced an iron concentration of 102.265 mg/L in the 1000 mL flask. This concentrated standard was then diluted to the desired concentrations necessary for the calibration curve by mixing 1, 2, 5, and 8 mL, respectively from the concentrated 100 ppm standard into a 100

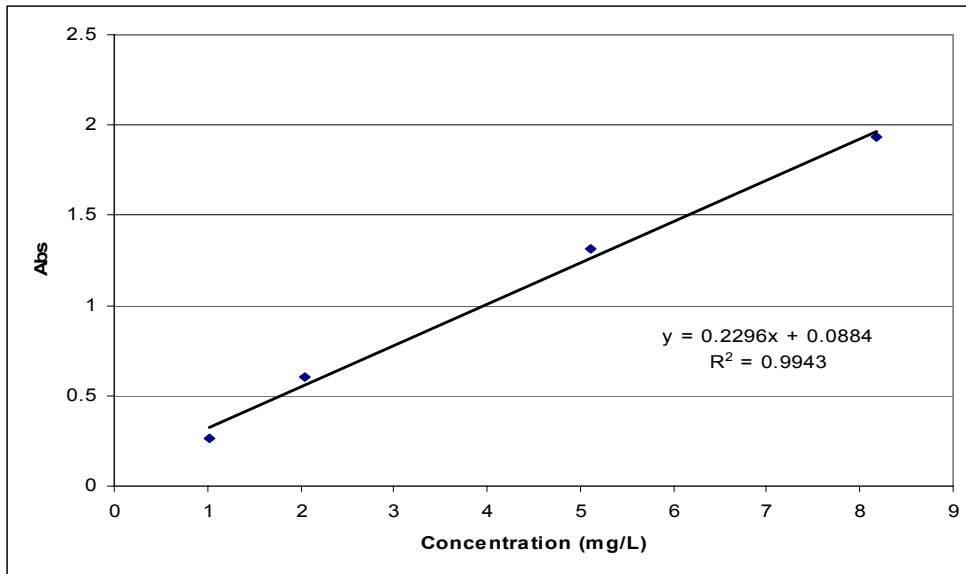
mL volumetric flask and filling with DI water. The actual concentrations of the four points on the calibration curve are given in Table 3-1. The spreadsheet used to calculate the necessary iron concentrations for the points on the calibration curve and the calculations used is included in Appendix C.

**Table 3-1: Standards**

Desired Concentration (ppm)	Actual Dilution (ppm)
1	1.023
2	2.045
5	5.113
8	8.181

The calibration curve was created by measuring the known iron standards concentrations using the same procedures that the iron concentrations in the Mantua samples were measured. First, ten mL from each of the four standard concentrations were placed in test vials that fit the spectrophotometer. A packet of FerroVer Iron Reagent was then added to each vial. The reagent is a phenanthroline based powder that dissolves and creates a colorimetric change in the sample, the strength of which varies based on the concentration of the iron present. Each standard was measured in the spectrophotometer at a wavelength of 510 nanometers, the necessary wavelength to accurately determine the iron concentration (APHA 1995). The amount of light absorbed by each standard was recorded and a calibration curve was created based on the absorbance and the associated concentration of iron. Normally the calibration curve would be piecewise linear, using each measured data point. However, for these data, the curve approximated a straight line. To make calculations simpler, a linear trend line was

fit to the calibration points creating a linear equation that determines iron concentration based on the absorbance of a sample. Figure 3-2 is the calibration curve created using the ferric chloride standards.



**Figure 3-2: Iron standards calibration curve**

### 3.4.3 Re-aeration and Iron Measurement

To measure the experimental results, the anaerobic state of the Mantua water sample was first confirmed, and then the procedure used to measuring the iron concentration in the standards was followed to measure the iron concentration in the Mantua water. First the water in the sample bucket was decanted from the sediment by pouring it into a smaller container. Immediately upon opening the bucket of anaerobic water, a sample was removed and the iron was measured. This sample was an attempt to measure the amount of dissolved iron before any aeration. A mixer was then placed in this bucket to provide adequate re-oxygenation to the entire water sample.

At specified times, a sample of the Mantua water was removed from the mixing bucket and filtered using a bottle top filter and a vacuum pump. The purpose of the filtration was to ensure that the ferric iron that had already precipitated was removed from the sample and measure only the remaining ferrous iron in the reservoir water. After the sample was filtered, two ten mL test vials were prepared with the FerroVer reagent. The absorbance of these two vials were then measured in the spectrophotometer at the required wavelength of 510 nanometers. The recorded absorbance for each sample was compared to the calibration curve in order to determine the concentration of ferrous iron in the water, which was averaged for the two samples taken. This process was repeated as quickly as possible, being constrained by the time required to filter each sample. The result was a kinetics curve relating time since re-aeration to the concentration of ferrous iron remaining in the water. From the kinetics curve, and using the first-order kinetics equation (equation 2-4), the rate constant for iron oxidation kinetics in Mantua Reservoir was determined. This is discussed more fully in Section 5.3.



## 4 Computer Modeling Procedures

### 4.1 PHREEQC

To better understand the iron oxidation kinetics of Mantua Reservoir I created a computer model. The model allowed me to evaluate the kinetics of iron oxidation for any conditions that may be present at the reservoir, based on the kinetic models present. The parameters that can be adjusted in the model related to iron precipitation kinetics include the water temperature, pH, and the loading rates of the various nutrients and inorganic constituents. The current conditions of the water at Mantua reservoir could be used to setup the model and using the experimentally determined  $k$ , the kinetics for iron oxidation can be predicted under various conditions.

The program used to develop the model of Mantua Reservoir was PHREEQC. PHREEQC was developed by Parkhurst and Appelo for United States Geological Survey (USGS). The program was created to conduct low temperature aqueous geochemical calculations (Parkhurst and Appelo 1999). In this case low temperatures are those expected in the surface environment, in many geochemical applications, the reactions take place at high temperatures deep underground. The primary use of PHREEQC is as a speciation program to calculate saturation indices and the distribution of aqueous species. Kinetic reactions can also be modeled using an embedded Basic editor. The kinetic rate



expressions are written using Basic and then PHREEQC interprets the code and runs the kinetic calculations (Parkhurst and Appelo 1999).

## 4.2 Mantua Model Development

To develop a model of the iron oxidation kinetics taking place in Mantua Reservoir water, I used example 9 of the PHREEQC models provided with the program which was created to conduct kinetic calculations for the oxidation of ferrous iron to ferric iron. Example 9 is titled “Kinetic Oxidation of Dissolved Ferrous Iron with Oxygen” (Parkhurst and Appelo 1999) and is included in Appendix B. I used this example model as the basis for the iron oxidation kinetics model developed for Mantua Reservoir.

Example 9 is used in the documentation to demonstrate the ability of PHREEQC to conduct kinetic calculations for the oxidation of  $Fe^{2+}$  to  $Fe^{3+}$  in water (Parkhurst and Appelo 1999). The rate equation, Equation 4-1, used in the model was adapted from Singer and Stumm (1970):

$$\frac{dm_{Fe^{2+}}}{dt} = -(2.91 \times 10^{-9} + 1.33 \times 10^{12} \alpha_{OH^-}^2 P_{O_2}) m_{Fe^{2+}} \quad (4-1)$$

where  $t$  equals the time in seconds,  $\alpha_{OH^-}^2$  is the activity of the hydroxyl ion,  $m_{Fe^{2+}}$  is the total molality of ferrous iron in solution, and  $P_{O_2}$  is the partial pressure of the oxygen (Parkhurst and Appelo 1999). The kinetics rate equation is solved using a 4th- and 5th-order Runge-Kutta-Fehlberg algorithm that is embedded within PHREEQC. PHREEQC calculates equilibrium before starting a kinetic calculation and again when each kinetic

reaction increment is added. The model calculates equilibrium for all solution-species, and for all exchange, equilibrium-phase, solid-solutions, surface assemblages and gas phases that are defined. A check is performed to ensure that the difference between the fourth- and fifth-order estimates of the integrated rate over a time interval does not vary by more than a user-defined tolerance. Failure to achieve results within the user defined tolerances will automatically restart the integration with a smaller time interval (Parkhurst and Appelo 1999).

The model I created of Mantua reservoir was based on the example provided with the program. Like the example, the purpose of the Mantua model is to simulate the oxidation of ferrous iron to ferric iron using oxygen in a natural water system, however the two models use separate geochemical environments. The PHREEQC model of Mantua Reservoir is presented in Appendix B. Several changes were required to adapt the example model to reflect the conditions present at Mantua reservoir. The first section of the Mantua model, SOLUTION\_MASTER\_SPECIES and SOLUTION\_SPECIES, decouples the valence state of iron and defines the possible iron species found in the water (Parkhurst and Appelo 1999). This section of the code remained unchanged from the example in the Mantua model.

The next section of the model, starting with EQUILIBRIUM\_PHASES 3, defines the conditions at Mantua Reservoir and defines the species that have the potential to precipitate out of the water, in this case ferric hydroxide. This section is followed by the SOLUTION1 section which defines the concentrations, in mmol/kilograms of water (kgw), of the applicable constituents and the physical characteristics of the water; this section was modified to match measured conditions at Mantua. Of particular importance

is the concentration of ferrous iron in the water, also expressed in mmol/kgw. The EQUILIBRIUM PHASES 1 heading defines the partial pressure of atmospheric oxygen that serves to aerate the water and cause the oxidation of the ferrous iron. This value is the negative log of the partial pressure for oxygen in the atmosphere at 5000 feet of elevation for the Mantua model (Parkhurst and Appelo 1999).

The final section of the PHREEQC model code is the kinetics calculation. The RATES data block is used to define the kinetics rate equation (see equation 4-1) used in the model calculations. This is followed by the KINETICS data block which invokes the rate expression and defines the parameters, especially the time increments. The final section of the code defines the desired output form of the results. For the Mantua model, a graph is created showing the total concentrations of ferrous and ferric iron versus time was created (Parkhurst and Appelo 1999).

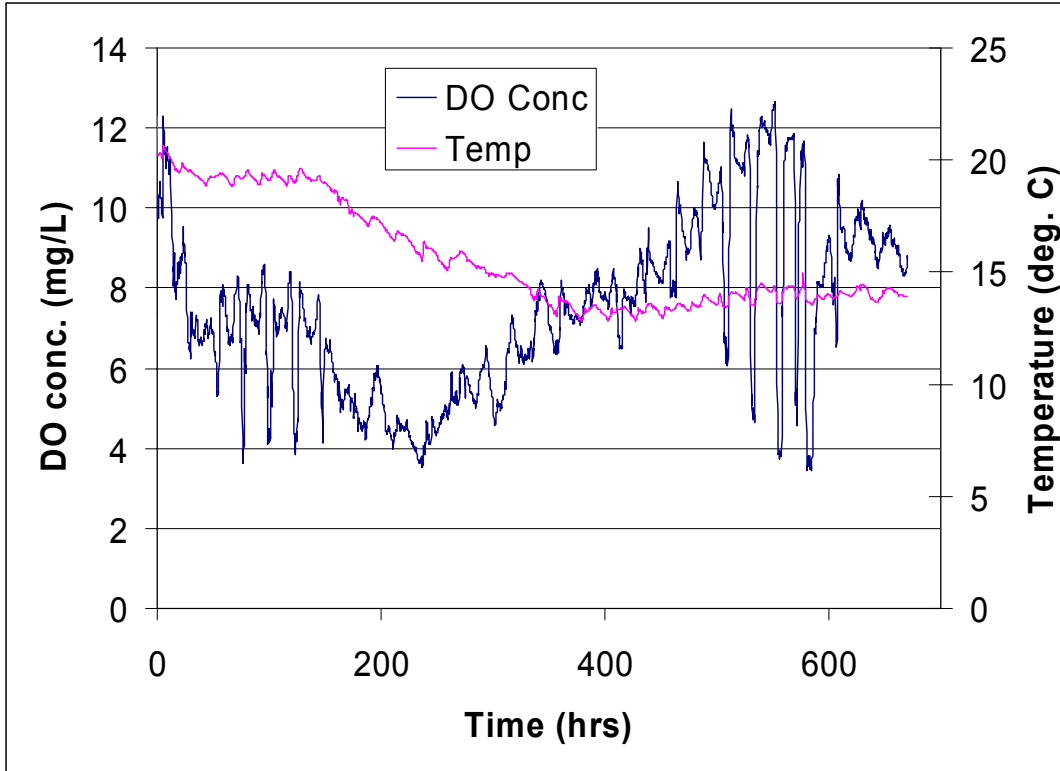
After developing a generic model for Mantua Reservoir which used the measured field environmental data, I refined the model by adjusting the rate constant to fit the observed kinetics data for the oxidation of ferrous iron that was measured in the laboratory. This required adjusting the rate constant in Equation 4-1 by an order of magnitude from the value used in the example model. This rate increase can be attributed to microorganisms catalyzing the reaction, a factor that is not considered in the rate constant provided in the example. Mantua has significant biological activity and the example problem did not consider biological activity.

## 5 Experimental and Modeling Results and Discussion

### 5.1 Field Results

Field measurement of the conditions at Mantua Reservoir was used to support my work and verify previous work. The deployment of the DO probe at Mantua Reservoir to measure DO values over time, served to confirm that the anaerobic conditions necessary to support the conclusions of Wallace (2006) could occur in the field. Data was collected by the sonde every fifteen minutes over a four week period starting the beginning of September, 2006 and ending the first week of October, 2006. A sample of the raw data obtained by the sonde is included in Appendix A. Figure 5-1 is a plot of the DO concentration and the water temperature of Mantua Reservoir over the period tested.

As expected, the DO concentration increases with lower water temperatures. Water has a greater capacity to dissolve and store oxygen at colder temperatures (Sawyer *et al* 2003). Of particular interest for the purposes of this study was the variation in the DO. Large variations, up to 6 ppm, occurred over relatively short periods as seen by the large repetitive changes between 50 to 150 hours and 500 to 600 hours. For example, on September 11<sup>th</sup>, 2006 (75 hours), starting at around 2:00 pm, the DO concentration in the reservoir steadily dropped from about 8.0 mg/L to 3.62 mg/L at 5:30 pm on the same day. The corresponding water temperature at the time only dropped one-tenth of a degree Celsius (from 19.28 degrees to 19.18). Using weather station data obtained from a site in



**Figure 5-1: DO and temp measurements**

nearby Brigham City, the maximum wind velocity during this period peaked at 5 miles per hour (mph) at 5:30 pm and the corresponding temperature at this time was 82 degrees Fahrenheit (Utah Department of Air Quality 2006). Although Mantua Reservoir and Brigham City are only about 5 miles apart (Mantua Reservoir TMDL 2000), the reservoir is located within the sheltered Box Elder Canyon so the wind and temperature profiles could vary significantly between the two locations. Also there is a difference of 782 feet in elevation between the weather station and the reservoir that could result in different wind velocities and air temperature at the two locations. The data collected from Mantua Reservoir includes ten instances in the one-month period, like the one described above, where a sharp drop in the DO concentration occurred over a matter of a few hours.

A number of factors could have significant effect on the data collected and the data might not reflect the exact conditions at the water-sediment interface. Wallace (2006) concluded the reduction of iron in the sediments under anaerobic conditions, and the subsequent dissolution of the ferrous iron into the reservoir water, occurred immediately above the sediments at the bottom of the lake. The DO probe was deployed about two feet off the lake bottom for fear of dropping reservoir water levels, sinking the sonde into the sediments. At a greater depth, the DO concentration most likely drops more during the calm periods than the values measured as there is less mixing and diffusion of the oxygen from the atmosphere (Loveless *et al* 1997).

Another important consideration is the time period when the sonde was deployed. The staining was observed in the middle of summer (Wood 2002), during hot temperatures, stagnant wind conditions, and low water levels in the reservoir. However, the probe collected data at the end of summer and the beginning of fall, when the atmospheric and water temperatures are beginning to drop and there was more wind. This is significant because, based on Henry's law (Sawyer *et al* 2003) as the water temperature drops the water has a greater capacity for dissolved oxygen and the biological processes that use the available oxygen in the reservoir begin to slow. Henry's law, given in equation 5-1, states that the amount of gas that will dissolve into a liquid, at constant temperature, is proportional to the partial pressure of the gas above the liquid (Sawyer *et al* 2003).

$$K_H = \frac{P_{gas}}{C_{equ}} \quad (5.1)$$

$P_{gas}$  is the partial pressure of the gas above the water,  $C_{equ}$  is the equilibrium concentration of the gas dissolved into the liquid, and  $K_H$  is the Henry's law constant at a given temperature (Sawyer *et al* 2003).  $K_H$  for water at 20° Celsius is 0.73 atm·m<sup>3</sup>/mol and the atmospheric partial pressure of oxygen at 5000 feet of elevation is 0.16 atm (Sawyer *et al* 2003). Using equation 5.1, the equilibrium DO concentration for Mantua Reservoir is 0.22 mol/m<sup>3</sup> or 7.19 mg/L. Assuming complete mixing with the atmospheric oxygen, Mantua Reservoir would have the above calculated DO concentration.  $K_H$  is sensitive to temperature however, and slight changes in temperatures significantly affect the solubility limits for oxygen.

Spikes in the recorded DO concentration above the theoretical saturation limit of the reservoir could indicate the possibility that an air bubble was resting on the optical sensor of the probe, inflating the recorded DO concentration or that photosynthesis of the aquatic life caused the DO levels to become supersaturated. The sharp drops in DO concentration indicate that there is a lack of mixing in the lower layers of the reservoir with the saturated upper layers and that biological processes are quickly using the available oxygen.

Though the field measurements did not record the hypolimnion in an anaerobic state, the dips indicate that there are regular periods of reduced mixing between the water layers of the reservoir and under the correct conditions could result in anaerobic water in the hypolimnion. Measurements in warmer weather, with warmer water which would reduce the DO capacity of the water, and increased biological activity that would more quickly use the available oxygen would make anaerobic conditions more likely. Deploying the sonde at a greater depth would measure conditions near the sediment-

water interface where there is less mixing of the hypolimnion with the upper reservoir water levels and further increase the likelihood of anaerobic conditions occurring which are favorable for the reduction of ferric iron. Despite the limitations of the field measurements, the regular large drops in DO concentration provide evidence of the ability of Mantua Reservoir to become anaerobic in the lower water levels. This corresponds to the research conducted by Loveless *et al* (1997) which found that the DO levels dropped below acceptable levels in the summer months.

## 5.2 Qualitative Staining Results

I performed qualitative experiments to recreate the staining observed in the Brigham City cemetery and to determine the amount of time necessary for visual staining. This experiment consisted of spraying water saturated with iron onto concrete as described in Section 3.2.

The primary results from this experiment are qualitative observations of the staining evident over a measured period of time. Table 5-1 is the recorded observations at each respective time.

**Table 5-1: Staining Observations**

<b>Time</b>	<b>Observations</b>
11:02	Concrete sprayed
12:05	Concrete still drying, no visual
1:03	Iron precipitates visually
2:00	More precipitates on lid
3:00	Faint staining evident on
10:00	Noticeable staining on

Figures 5-2 and 5-3 are photographs of the concrete before spraying with water and after the staining occurred and are indicative of the results obtained from the staining



experiment. The faint brownish hue, visible in Figure 5-3, is the result of the precipitation of the insoluble ferric iron from the water after being re-aerated by contact with the atmosphere and spraying on the concrete. Though not as visible on the concrete cores, a white surface (a bucket lid), placed under the core to catch the excess water spray, and clearly showed precipitated iron after this experiment. These ferric iron precipitates appeared and caused visible staining approximately two hours after the concrete core was sprayed with anaerobic Mantua Reservoir water. The iron precipitated out of the water before evaporation could take effect to eliminate the water.



**Figure 5-2: Concrete before spraying**



**Figure 5-3: Stained concrete**

One difference between the observed field conditions and the qualitative lab experiment is the duration of the exposure. In Brigham City's cemetery, the headstones are exposed to the Mantua water through the irrigation system. A typical zone in an irrigation system is run for approximately 30 minutes. During that time the headstones will be sprayed every few seconds by one or more nearby sprinklers. In contrast, due to the very limited supply of anaerobic Mantua water, I was only able to spray the concrete core continuously for about two minutes. The effect of this difference is that the headstones have the potential for many times the iron exposure and therefore more evident staining. However, as shown by Wallace (2006) staining will only occur when

the irrigation water is anaerobic and iron-rich, a condition which will only occur rarely, when the correct conditions happen at Mantua Reservoir.

The difference between the materials sprayed could also change the kinetics of the iron precipitation. The materials in concrete contain high carbonate quantities, giving concrete a basic pH (Mindness *et al* 2003). As seen in the equations that describe the iron oxidation kinetics (equations 2-2, 2-3, 2-5, and 4-1), the rate at which ferrous iron is oxidized to ferric iron is a function of the pH of the system. As the water becomes more basic through contact with the concrete the pH rises and the rate of oxidation is increased. Though the concrete has the potential to increase the oxidation rate of the ferrous iron, the water observed on the bucket lid exhibited precipitated iron quicker than the concrete despite having less contact time as it ran off the concrete. This experiment indicates that staining could occur very rapidly, on the order of a few hours, after spraying the headstones with water.

### **5.3 Quantitative Experimental Results**

The purpose of the laboratory experiments was to determine the kinetics of iron oxidation in Mantua Reservoir and provide information that could be used to predict and understand the precipitation reactions. The primary objective was to determine the rate constant ( $k$ ) that governs the oxidation rate in the reservoir water. This rate constant can then be used in models of the reservoir in order to predict the speed of the reaction and assist in the development of remediation options.

Table 5-2 presents the results of these experiments (described in Section 3.4). Table 5-2 contains the amount of iron in the water from Mantua Reservoir after various

time increments. This table includes the date and time that all of the samples were removed from the bucket of water and also the times that they were actually run in the spectrophotometer. The delay was caused by excessive fouling of the bottle top filters from the suspended sediments. The amount of time between each sample is also included. Table 5-2 also includes the average absorbance measured for each sample and the associated concentration as determined using the calibration curve.

**Table 5-2: Spectrophotometer Results**

<b>Date</b>	<b>Sample</b>	<b>Time Removed</b>	<b>Run Time</b>	<b><math>\Delta T</math> (min)</b>	<b>abs</b>	<b>[Fe] mg/L</b>	<b>Average [Fe] mg/L</b>
<b>Oct. 21</b>	1-1	11:25	11:28	0	2.365	9.92	9.87
	1-2				2.344	9.82	
	2-3				NA	NA	8.69
	2-4	11:45	11:55	27	2.083	8.69	
	3-5	12:10	12:20	62	1.706	7.05	7.04
	3-6		12:23	65	1.705	7.04	
	4-7	12:37	12:55	97	1.369	5.58	5.53
	4-8		1:00	102	1.346	5.48	
	5-9	1:35	1:47	149	1.333	5.42	5.43
	5-10		1:50	152	1.339	5.45	
	6-11	3:43	3:55	277	1.662	6.85	6.79
	6-12		3:58	280	1.635	6.74	
	7-13	6:50	7:05	467	0.722	2.76	2.76
	7-14		7:10	472	0.721	2.76	
	8-15	9:10	9:20	542	0.628	2.35	2.33
	8-16		9:23	545	0.619	2.31	
<b>Oct. 22</b>	9-17	3:31	3:48	1650	0.106	0.08	0.07
	9-18		3:51	1653	0.104	0.07	

From these results it is evident that the oxidation and precipitation of ferrous iron in Mantua Reservoir water proceeds quickly. An initial concentration of almost 9.0 mg/L drops to almost nothing in a little over a day. After just two hours, the concentration dropped by about 3.0 mg/L (from 8.69 mg/L to 5.42 mg/L).

The first three samples were discarded because I added a couple drops of hydrochloric acid (HCl) to each vial in an effort to acid digest all of the iron. Acid digestion insures that all of the iron that was in solution after filtration remained in solution and did not precipitate (Sawyer *et al* 2003). However, use of the FerroVer reagent eliminates the need for acid digestion. This was realized when the second batch of water was removed and split into two samples (2-3 and 2-4). I added the HCl to sample 2-3 and only added the reagent to 2-4. The samples with the acid turned a milky white color and precipitates settled to the bottom of the vial; the reagent reacted with the HCl in a way which made the sample unusable. Sample 2-4 and all of the subsequent samples produced the expected colorimetric change. Figure 5-4 is a graph of the total time elapsed versus the iron concentration remaining in the water.

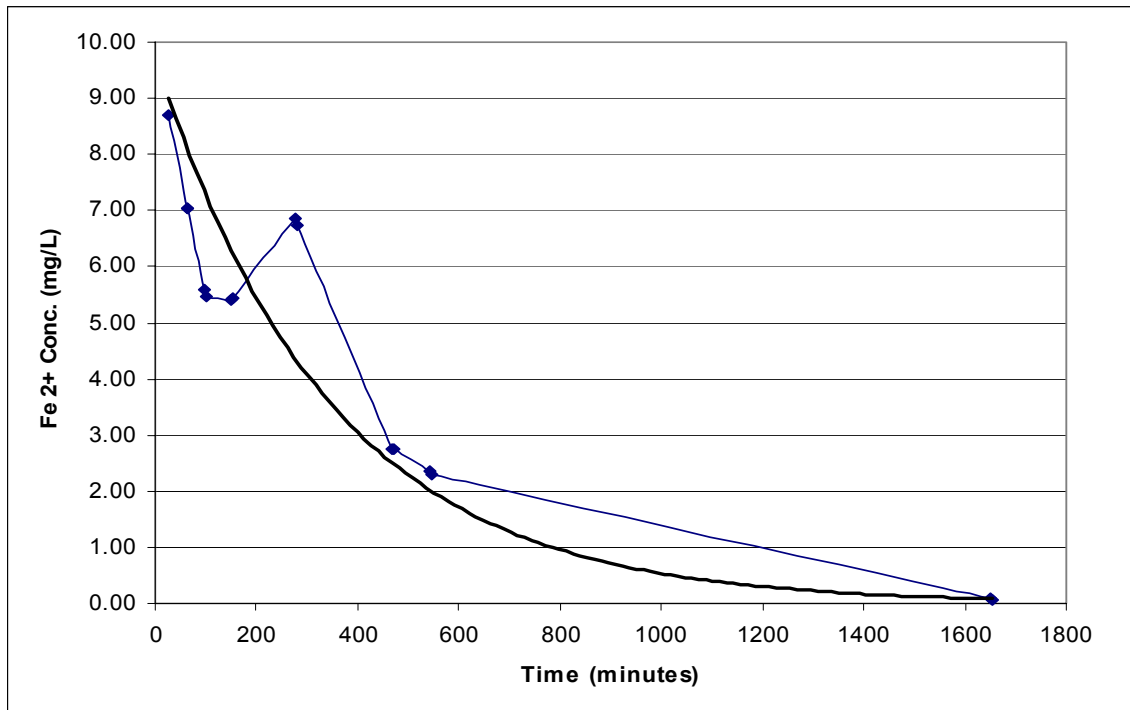
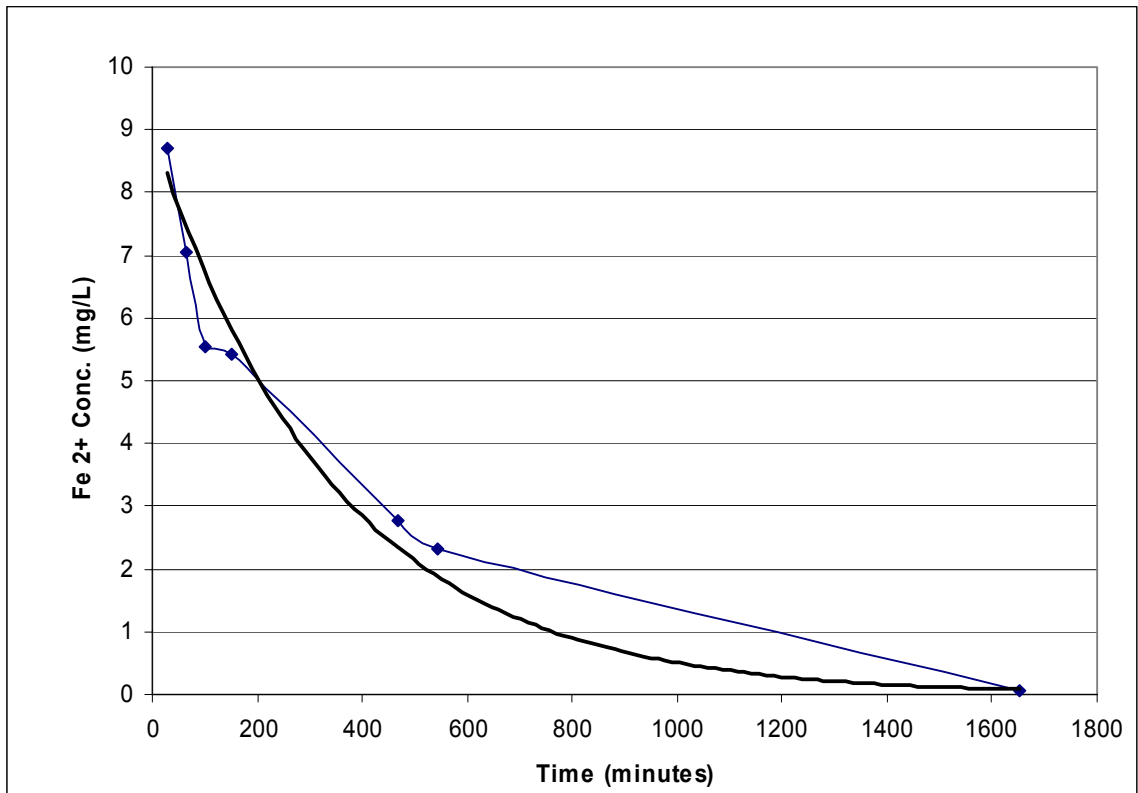


Figure 5-4: Iron oxidation over time

Figure 5-4 includes a trend line, its associated exponential equation, and an R-squared value. R-squared for this trend line is 0.9779. Removing the outlier point and using the average time elapsed and concentration yields Figure 5-5.



**Figure 5-5: Revised iron oxidation over time**

By removing the outlier point the R-squared value moves closer to one, with a value of 0.9918, indicating that the trend line is a better fit to the data. Equation 5-2 is the equation for the revised trend line:

$$y = 8.9877e^{-0.0029x} \tag{5-2}$$

where  $x$  is the time in minutes and  $y$  is the iron concentration in mg/L remaining in the water. This equation is the form of equation 2-4 describing first-order kinetics with  $x$  corresponding to  $t$  and  $y$  to  $C$ . This gives a rate constant  $k$  for Mantua Reservoir water of  $0.0029 \text{ min}^{-1}$ , based on my experimental results

#### 5.4 PHREEQC Model Results

Mantua Reservoir was first modeled using the default rate constant provided with the iron oxidation kinetics example (see equation 4-1 and Section 4.2). The model-produced result is a plot of the change in concentration of both ferrous iron ( $\text{Fe}^{2+}$ ) and ferric iron ( $\text{Fe}^{3+}$ ) versus time. Figure 5-6 is the plot produced using the default rate constant.

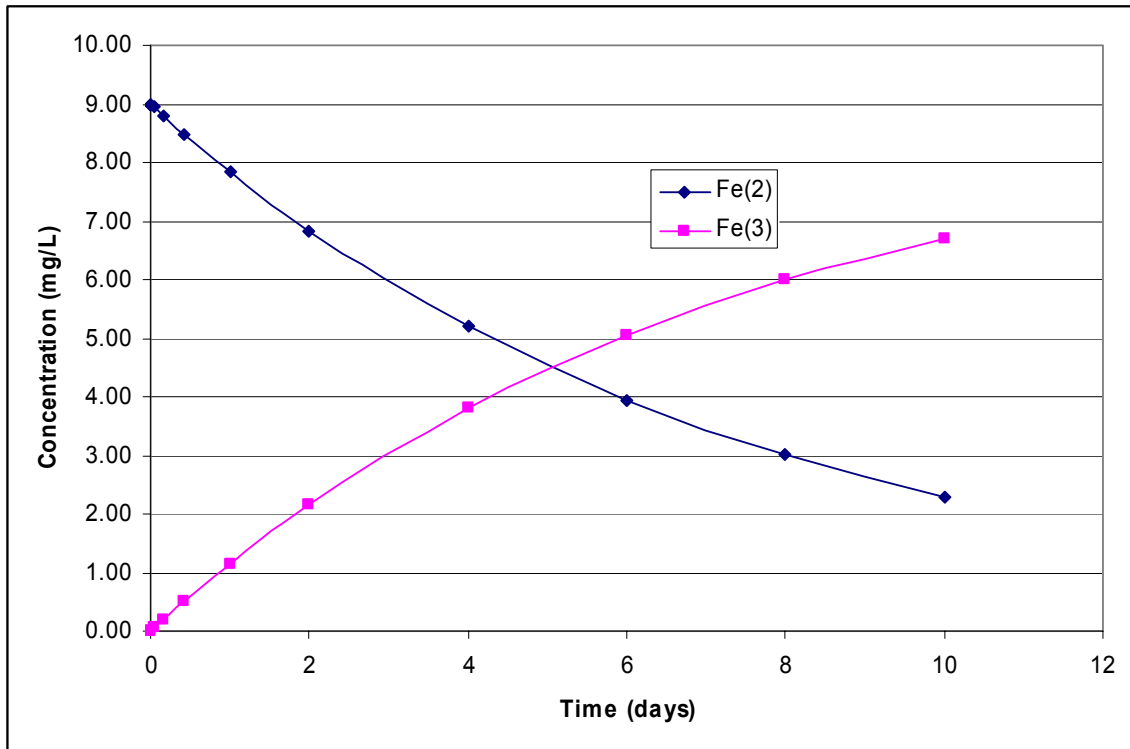


Figure 5-6: Change in iron concentration using default  $k$



As the ferric iron concentration rises, due to the solubility product being extremely low ( $K_{sp} = 2.79 \times 10^{-39}$ ), the aqueous solution becomes supersaturated with respect to iron (III) (Sawyer *et al* 2003). The insoluble ferric iron will then begin to precipitate out of the solution. Using the default rate constant, after five days the ferrous iron concentration in the water has dropped by fifty percent. However, this model does not cause the oxidation to occur at close to the same rate as seen experimentally, with the experimental and observed reaction rates being much faster. Again, this discrepancy is probably the result of a biological component to the iron oxidation as was discussed in Section 2.3.

In order to more accurately predict the iron oxidation kinetics in Mantua Reservoir water, the model was modified to use the measured kinetic data from my laboratory experiments. Through a trial and error process of adjusting the rate constant, I created a model that closely matched the experimental data. Figure 5-7 is a plot of the concentration of ferrous iron over time based on the revised model and on the experimental data.

The rate constant found was  $4 \times 10^{13} / \text{atm} \times \text{min}$ , thirty times bigger than the default value. This value is different than the one shown in Figure 5-5 because a different kinetics equation was used in the PHREEQC model rather than the first-order model presented above. Using the fitted theoretical rate constant from calibrating the PHREEQC model to the laboratory results, the complete oxidation of ferrous iron in Mantua Reservoir water was modeled.

Figure 5-8 presents the same parameters as Figure 5-6, but the data were calculated by applying the calibrated rate constant from the Mantua water experimental



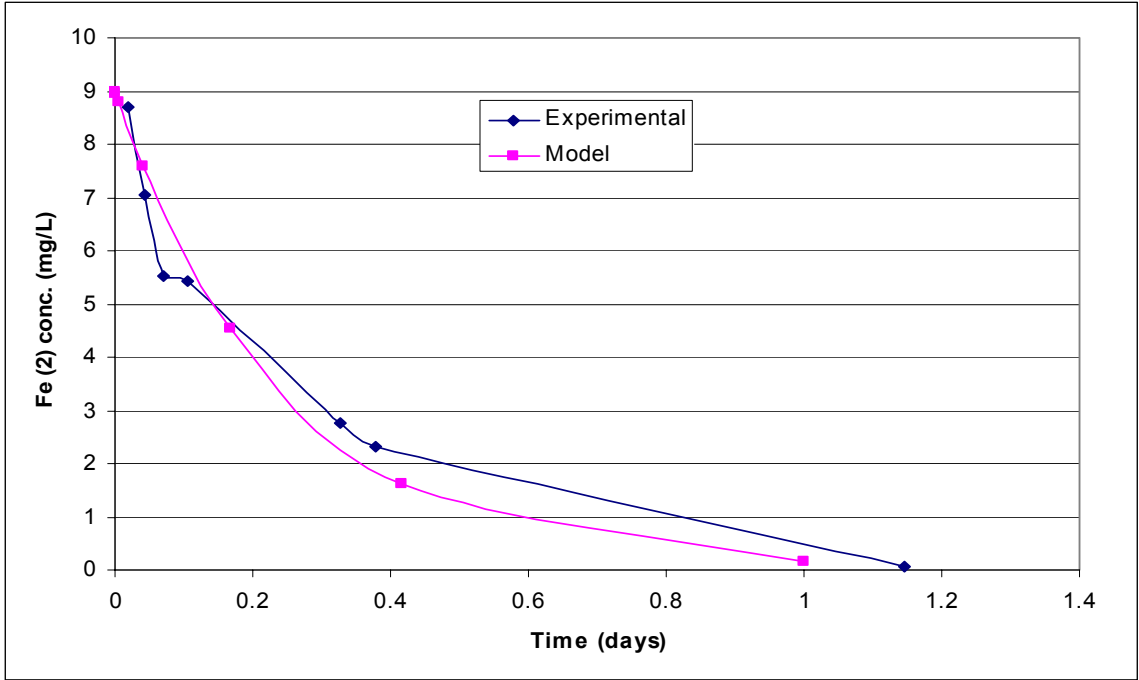


Figure 5-7: Model vs experimental iron concentrations

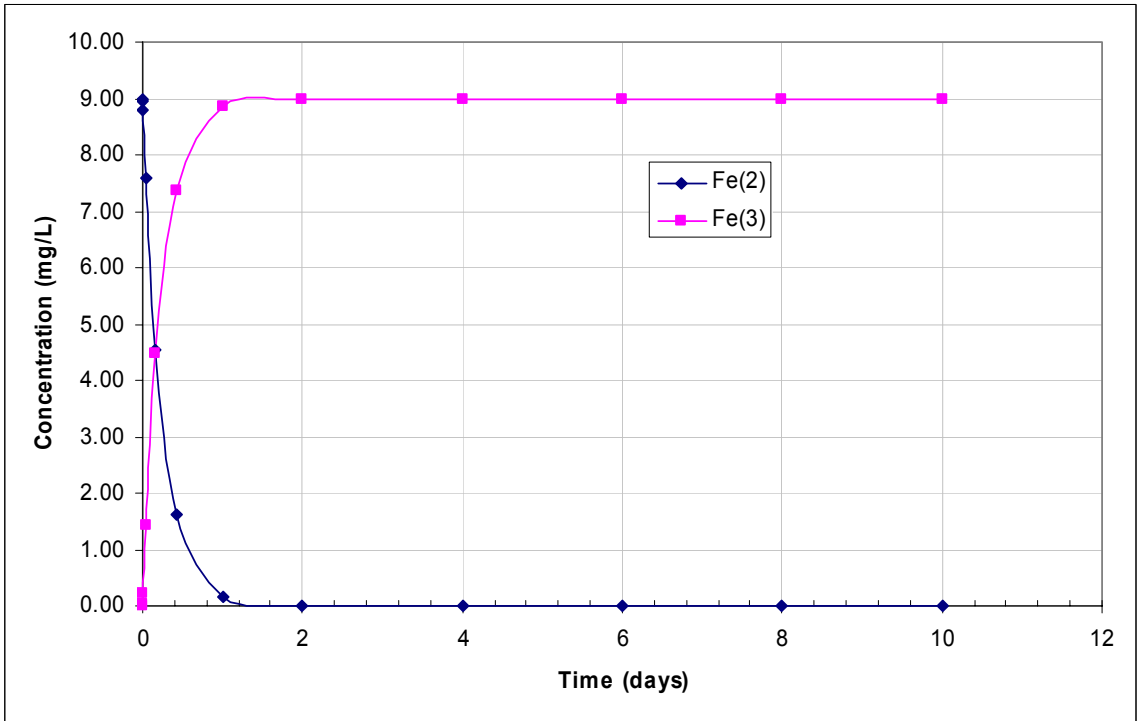


Figure 5-8: Model of Mantua iron oxidation kinetics

results. Figure 5-8 shows that after one day there is virtually no ferrous iron (0.15 mg/L) remaining in the reservoir water and after only four hours half of the ferrous iron dissolved in the water has been oxidized to ferric iron. This matches both observations and laboratory experiments. This also matches the staining events in the Brigham City cemetery, where staining occurred overnight and no stain build-up was noticed.

I propose that the explanation for the difference in the rate constants between the PHREEQC example model and the Mantua water model is the catalytic effects of microorganisms. As Okereke and Stevens (1991) proved with their research, the presence of iron oxidizing bacteria greatly increases the rate of iron oxidation. The presence of microbes can accelerate the reaction rate by a factor of  $10^6$  (Singer and Stumm 1970). *Thiobacillus ferrooxidans* are the most common microbes that oxidize ferric iron. Based on the research of Okereke and Stevens (1991), the right microbes could easily accelerate the kinetics of iron oxidation by an order of magnitude which would account for the differences found.



## 6 Conclusions

The purpose of this research was to confirm the capacity of Mantua Reservoir to achieve anaerobic conditions, causing the reduction and eventual oxidation of iron, and to determine the ferrous iron oxidation kinetics and thus how quickly staining could occur. Knowing the rate of the oxidation reaction will assist in the determination of practical remediation efforts by determining the residence time of the water after treatment before it could be used in the irrigation system.

The efforts to confirm the potential for Mantua Reservoir revealed that even in early fall, the DO concentration in the hypolimnion fluctuates severely. Though the study was conducted when the water temperature was already decreasing, causing an increase in the potential equilibrium DO concentration, the fact that the DO levels oscillated gave evidence that anaerobic conditions are likely in the lower water layers of Mantua Reservoir during the warmer summer conditions. The field data collected confirmed the results obtained by Loveless *et al* (1997) as part of the Clean Lakes Study. Their field work found DO levels as low as 3.0 mg/L within a meter of the bottom. Anaerobic conditions are required for the reduction of ferric iron, which is found in abundance in Mantua sediments. Reduced iron, in the ferrous state, is much more soluble than ferric iron and dissolves into the water only to be oxidized upon re-aeration through the irrigation system (Sawyer *et al* 2003).

The iron oxidation kinetics for Mantua Reservoir were determined using three different methods. The first method was a qualitative observation of the staining caused by iron precipitation on a cement core. Though the conditions of the experimentally derived staining differed from the field conditions, iron precipitation was evident after only two hours of observation. This showed that if the anaerobic conditions existed in Mantua Reservoir resulting in high amounts of dissolved iron, the use of the pressurized irrigation system would cause staining to appear on the headstones within a matter of hours.

The experimental results of the iron oxidation for Mantua yielded results that showed the iron was quickly oxidized and precipitated from the Mantua water. The ferrous iron was almost completely gone after 26 hours and had been reduced by over a third in just a couple of hours. Fitting a simple first order kinetics equation to the experimental data yielded a rate constant of  $0.0029 \text{ min}^{-1}$ , giving a half life of 239 minutes or approximately 4 hours. As with the qualitative results, the kinetics experiment has proved that the iron will precipitate out of the water and cause staining in Brigham City.

The creation of a geochemical computer model, using PHREEQC, also confirmed the speed of the iron oxidation kinetics. Using an example provided with the software as a foundation, and modifying the example to match the measured physical and chemical properties of Mantua Reservoir, resulted in a model in which the computed ferrous iron concentration dropped by fifty percent over the course of five days. This was not a good fit to the experimental data and therefore the model was calibrated to the experimental results from the actual Mantua water. The rate constant in the calibrated model was

$4 \times 10^{13}$  /atm x min. With the rate constant calibrated to experimental results and a computer model of the oxidation kinetics, the oxidation of iron was predicted for any changing conditions of the reservoir. Model calculations showed that the majority of the iron would precipitate in a few hours.

## 6.1 Application

Knowing the iron oxidation kinetics of Mantua Reservoir water makes remediation recommendations possible. The purpose of this section is not to exhaustively study all of the technology available for the removal of dissolved iron in water but rather to provide an overview of possibilities for Brigham City to employ at Mantua Reservoir or in their irrigation system. (For a comprehensive study on iron treatments refer to *Iron and Manganese Treatment for Small Systems*, a thesis prepared by Harry Campbell for Brigham Young University, 1989).

There are two general approaches that could be applied. The first and recommended approach is to change conditions at Mantua Reservoir so that the hypolimnion does not become anaerobic. In addition to addressing the staining problem, this approach has the potential to address several other problems noted at Mantua including water quality and aesthetics. The second approach is to treat iron rich water after it leaves Mantua Reservoir before being used for irrigation.

The simplest and preferred solution to the staining problem would be to prevent iron from dissolving from the sediment under anaerobic conditions. Prevention would involve precluding the reservoir from becoming anaerobic in the hypolimnion by aeration or circulation. There are numerous commercial systems designed to aerate lagoons and

reservoirs that could potentially be used at Mantua. During the course of my lab experiments, there were numerous failed attempts to conduct the experimental phase of the kinetics investigation. Invariably the failure was a consequence of excessive DO in the water preventing iron from dissolving from the sediments, as little as 2.0 mg/L, in the water sample. (The one successful attempt had a DO concentration of 1.0 mg/L after opening the bucket and mixing to a small degree by using a field DO probe which might have caused some of the DO in solution). In any cases where the water contained measurable amounts of DO, after testing with the spectrophotometer, these failed tests only included trace amounts of iron because the iron was never dissolved from the sediments.

From these failures, I learned that very little oxygen is necessary to prevent the dissolution of iron from the sediments. As a result, remediation methods that increase the dissolved oxygen in the hypolimnion would successfully prevent ferric iron from being reduced and then dissolved as ferrous iron into the water column. Diffusers laid on the bed of the reservoir, near the outlet, would prevent the system from going anaerobic and also oxidize any iron already dissolved in the water causing it to precipitate and settle out before reaching the irrigation system. Another preventative measure would be to put a floating mixer anchored in the area of the outlet (this area is already restricted to recreational activities). This would have the effect of mixing the DO saturated surface waters with lower layers that have the greatest potential for becoming anaerobic. Like the diffusers this would prevent the microorganisms from using the ferric iron found in the reservoir sediments as an electron acceptor and would oxidize any ferrous iron

dissolved in the water. Both types of systems, and others such as sprayers and mixers, are commercially available.

The second general category is treating the water before irrigation. The basic idea of iron removal most commonly employed is the oxidation of the ferrous iron and subsequent clarification of the water, either using filtration or precipitation (Campbell 1989). This is exactly the process that is occurring in the system comprising Mantua Reservoir and the Brigham City secondary irrigation system. The major difference is the location of the removal of the iron hydroxide precipitates. In an engineered process they will be either removed in a settling basin or using a filtration system (Campbell 1989). In Brigham City's system the iron precipitates settle out on the headstones of the cemetery.

A solution would be to cause the iron to settle out, after oxidation, in a controlled location. This could be as simple as cascading the water over rocks, or other obstacles, far enough up the system to allow the iron (III) a chance to settle out. Immediately below the dam, before entering the penstock would allow treatment while retaining the pressure head required for power generation. The cascading water would be re-aerated and cause the oxidation of the ferrous iron. The reaction rate is fast enough, as determined by this study, to cause the iron to oxidize and settle out before entering the penstock and reaching the sprinklers of the city irrigation system. To prevent the iron precipitates from causing problems in the pipe distribution network a small settling pond, with a hydraulic detention time of a couple of hours, could be placed after the cascade to give the majority of the iron hydroxides a place to settle out.





## References

- American public Health Association (APHA) (1995). *Standard Methods for the Examination of Water and Wastewater*. 15 ed. AWWA –WPCF, Washington D.C.
- Bigelow, W.S. (2002). *Cemetery Headstone Staining Report*. Hansen, Allen, and Luce Inc. SaltLake City, Utah. (Report to the Brigham City Water Superintendent).
- Bigelow, W.S. (2005). *Proposal for Water Quality Study for Brigham City Pressurized Irrigation System*. Hansen, Allen, and Luce Inc. SaltLake City, Utah. (Letter to Dr. Gus Williams, BYU).
- Campbell, H. (1989). *Iron and Manganese Treatments for Small Systems*. Brigham Young University, Provo, UT.
- Davidson, W. and G. Seed (1983) “The Kinetics of the Oxidation of Ferrous iron in Synthetic and Natural Waters.” *Geochimica et Cosmochimica Acta*. Vol 47.
- Houben, G. J. (2004). “Modeling the Buildup of Iron Oxide Encrustations in Wells.” *Groundwater*. Vol. 42 No. 1.
- Laxen, D.P.H. and E.R. Sholkovitz (1982). “Adsorption (Co-precipitation) of Trace Metals in natural Concentrations of Hydrated Ferric Oxide in Lake Water Samples.” *Environmental Technology Letters*. Vol. 2.
- Liang, L., J.A McNabb, J.M. Paulk, B. Gu, and J.F McCarthy (1993). “Kinetics of Fe(II) Oxygenation at Low Partial Pressure of Oxygen in the Presence of Natural Organic Matter.” *Environmental Science Technology*. Vol. 27 No. 9.
- Loveless, R.M., R. Jones, and D. Wham (1997). *Phase I Clean Lakes Study: Diagnostic and Feasibility Report on Mantua Reservoir* Utah Department of Environmental Quality, Salt Lake City, Utah (in conjunction with US Environmental Protection Agency, Region VIII).
- Millero, F.J., S. Sotolongo, and M. Izaguirre (1987). “The Oxidation Kinetics of Fe(II) in Seawater.” *Geochimica et Cosmochimica Acta*. Vol. 51.

- Mindness, S., J. F. Young, and D. Darwin. (2003) *Concrete*. Prentice Hall: Upper Saddle River, NJ.
- Okereke, A. and S. E. Stevens Jr. (1991). "Kinetics of iron Oxidation by *Thiobacillus ferrooxidans*." *Applied and Environmental Microbiology*. Vol. 57.
- O'Neil, P. (1985). *Environmental Chemistry, second edition*. Chapman and Hall: London.
- Parkhurst, D.L. and C.A.J. Appelo (1999). *User' Guide to PHREEQC (version 2)—A Computer Program for Speciation, Batch-Reaction, One-Dimensional Transport, and Inverse Geochemical Calculations*. United States Geological Survey, Water-Resources Investigations Report 99-4259, Denver, Colorado.
- Sawyer, C.N., P.L. McCarty, and G.F. Parkin (2003). *Chemistry for Environmental Engineering and Science, fifth edition*, McGraw Hill, Burr Ridge, IL.
- Singer, P.C. and W. Stumm (1970). "Acidic Mine Drainage: The Rate-Determining Step." *Science*. Vol. 167.
- Stumm, W. and G.F. Lee (1961). "Oxygenation of Ferrous Iron." *Industrial and Engineering Chemistry*. Vol. 53 No. 2
- Stumm, W. and J.J. Morgan (1996). *Aquatic Chemistry: Chemical Equilibria and Rates in Natural Waters, third edition*. John Wiley and Sons, New York.
- Tamura H., K. Goto, and M. Nagayama (1976). "The Effect of Ferric Hydroxide on the Oxygenation of ferrous Ions in Neutral Solutions." *Corrosion Science*. Vol. 16.
- Utah Department of Environmental Quality (2000). *Mantua Reservoir TMDL*. Division of Water Quality: TMDL Section. Salt Lake City, UT.
- Utah Department of Air Quality (2006) Brigham City Monitoring Station. Brigham City, UT
- Wallace, R.D. (2006). *Dynamic Interaction of Iron Chemistry in Mantua Reservoir and Ferric Staining in the Secondary Water System of Brigham City, Utah*. Brigham Young University, Provo, UT.
- Wood, C. (2002). "Cemetery Stone Discoloration." Brigham City Cemetery Report. Brigham City, UT.
- YSI Incorporated (2006). "6-Series Environmental Monitoring System" *YSI Environmental Operations Manual*. Yellow Springs, OH.

## Appendix A. Field Data

**Table A-1: Field Data Collected from Mantua Reservoir (24 hour period, 9/11/2006)**

DateTime M/D/Y	Temp C	ODO Conc (mg/L)	Resistivity KOhm.cm	TDS g/L	Salinity ppt	SpCond mS/cm	ODO% %
9/11/2006 0:00	19.39	7.97	5.83	0.125	0.09	0.192	86.7
9/11/2006 0:15	19.38	8.07	5.84	0.125	0.09	0.192	87.7
9/11/2006 0:30	19.38	7.93	5.84	0.125	0.09	0.192	86.2
9/11/2006 0:45	19.37	7.86	5.84	0.125	0.09	0.192	85.4
9/11/2006 1:00	19.37	7.81	5.84	0.125	0.09	0.192	84.9
9/11/2006 1:15	19.37	7.93	5.84	0.125	0.09	0.192	86.1
9/11/2006 1:30	19.33	7.85	5.84	0.125	0.09	0.192	85.2
9/11/2006 1:45	19.31	7.8	5.85	0.125	0.09	0.192	84.6
9/11/2006 2:00	19.29	7.75	5.85	0.125	0.09	0.192	84
9/11/2006 2:15	19.25	7.52	5.85	0.125	0.09	0.192	81.5
9/11/2006 2:30	19.24	7.41	5.85	0.125	0.09	0.192	80.3
9/11/2006 2:45	19.22	7.3	5.85	0.125	0.09	0.192	79.1
9/11/2006 3:00	19.21	7.33	5.85	0.125	0.09	0.192	79.4
9/11/2006 3:15	19.19	7.13	5.86	0.125	0.09	0.192	77.2
9/11/2006 3:30	19.14	6.98	5.86	0.125	0.09	0.192	75.5
9/11/2006 3:45	19.14	6.92	5.86	0.125	0.09	0.192	74.9
9/11/2006 4:00	19.14	7.03	5.86	0.125	0.09	0.192	76.1
9/11/2006 4:15	19.11	6.91	5.86	0.125	0.09	0.192	74.7
9/11/2006 4:30	19.12	6.96	5.86	0.125	0.09	0.192	75.2
9/11/2006 4:45	19.07	6.81	5.86	0.125	0.09	0.192	73.5
9/11/2006 5:00	19.02	6.66	5.87	0.125	0.09	0.192	71.8
9/11/2006 5:15	19.01	6.6	5.86	0.125	0.09	0.193	71.2
9/11/2006 5:30	19.02	6.68	5.86	0.125	0.09	0.193	72.1
9/11/2006 5:45	19	6.77	5.87	0.125	0.09	0.193	73
9/11/2006 6:00	18.97	6.72	5.88	0.125	0.09	0.192	72.5
9/11/2006 6:15	18.92	6.57	5.88	0.125	0.09	0.192	70.7
9/11/2006 6:30	18.91	6.64	5.89	0.125	0.09	0.192	71.4
9/11/2006 6:45	18.93	6.7	5.88	0.125	0.09	0.192	72.1
9/11/2006 7:00	18.93	6.77	5.88	0.125	0.09	0.192	72.9
9/11/2006 7:15	18.88	6.68	5.89	0.125	0.09	0.192	71.9
9/11/2006 7:30	18.9	6.71	5.89	0.125	0.09	0.192	72.2
9/11/2006 7:45	18.86	6.75	5.9	0.125	0.09	0.192	72.6
9/11/2006 8:00	18.91	6.84	5.89	0.125	0.09	0.192	73.6
9/11/2006 8:15	18.94	6.75	5.89	0.125	0.09	0.192	72.7
9/11/2006 8:30	18.85	6.71	5.9	0.125	0.09	0.192	72.2
9/11/2006 8:45	18.84	6.64	5.9	0.125	0.09	0.192	71.4
9/11/2006 9:00	18.86	6.95	5.9	0.125	0.09	0.192	74.7
9/11/2006 9:15	18.91	7.05	5.9	0.125	0.09	0.192	75.9
9/11/2006 9:30	18.88	7.18	5.9	0.125	0.09	0.192	77.3
9/11/2006 9:45	18.94	7.31	5.89	0.125	0.09	0.192	78.7
9/11/2006 10:00	19	7.45	5.89	0.125	0.09	0.192	80.3
9/11/2006 10:15	19.09	7.7	5.87	0.125	0.09	0.192	83.2
9/11/2006 10:30	19.16	7.82	5.87	0.125	0.09	0.192	84.6
9/11/2006 10:45	19.25	7.88	5.85	0.125	0.09	0.192	85.4
9/11/2006 11:00	19.31	7.87	5.84	0.125	0.09	0.192	85.4
9/11/2006 11:15	19.3	7.88	5.85	0.125	0.09	0.192	85.5
9/11/2006 11:30	19.27	7.87	5.86	0.125	0.09	0.192	85.3
9/11/2006 11:45	19.27	7.87	5.86	0.125	0.09	0.192	85.3
9/11/2006 12:00	19.27	7.89	5.86	0.125	0.09	0.192	85.6
9/11/2006 12:15	19.27	8	5.86	0.125	0.09	0.192	86.8
9/11/2006 12:30	19.3	8.14	5.86	0.124	0.09	0.192	88.3

9/11/2006 12:45	19.3	8.25	5.86	0.125	0.09	0.192	89.6
9/11/2006 13:00	19.28	8.28	5.86	0.125	0.09	0.192	89.8
9/11/2006 13:15	19.27	8.29	5.85	0.125	0.09	0.192	89.9
9/11/2006 13:30	19.27	8.28	5.86	0.124	0.09	0.192	89.8
9/11/2006 13:45	19.27	8.24	5.86	0.125	0.09	0.192	89.3
9/11/2006 14:00	19.28	8.18	5.86	0.124	0.09	0.191	88.7
9/11/2006 14:15	19.25	7.98	5.86	0.125	0.09	0.192	86.5
9/11/2006 14:30	19.24	7.77	5.86	0.125	0.09	0.192	84.3
9/11/2006 14:45	19.23	7.65	5.86	0.125	0.09	0.192	82.9
9/11/2006 15:00	19.22	7.5	5.86	0.125	0.09	0.192	81.2
9/11/2006 15:15	19.21	7.23	5.86	0.125	0.09	0.192	78.3
9/11/2006 15:30	19.2	7.12	5.86	0.125	0.09	0.192	77.1
9/11/2006 15:45	19.2	6.65	5.84	0.125	0.09	0.192	72
9/11/2006 16:00	19.19	6.74	5.83	0.125	0.09	0.193	72.9
9/11/2006 16:15	19.2	5.83	5.82	0.126	0.09	0.193	63.1
9/11/2006 16:30	19.19	5.62	5.8	0.126	0.09	0.194	60.8
9/11/2006 16:45	19.19	5.49	5.8	0.126	0.09	0.194	59.4
9/11/2006 17:00	19.18	5.03	5.77	0.127	0.09	0.195	54.5
9/11/2006 17:15	19.18	4.33	5.72	0.128	0.09	0.197	46.9
9/11/2006 17:30	19.18	3.62	5.68	0.129	0.09	0.198	39.2
9/11/2006 17:45	19.19	3.97	5.66	0.129	0.09	0.199	42.9
9/11/2006 18:00	19.19	3.84	5.66	0.129	0.09	0.199	41.6
9/11/2006 18:15	19.2	3.91	5.66	0.129	0.09	0.199	42.4
9/11/2006 18:30	19.21	3.97	5.66	0.129	0.09	0.199	43
9/11/2006 18:45	19.23	4.05	5.69	0.128	0.09	0.197	43.9
9/11/2006 19:00	19.24	4.5	5.8	0.126	0.09	0.194	48.8
9/11/2006 19:15	19.27	6.51	5.8	0.126	0.09	0.194	70.6
9/11/2006 19:30	19.28	6.47	5.79	0.126	0.09	0.194	70.2
9/11/2006 19:45	19.28	6.16	5.76	0.127	0.09	0.195	66.8
9/11/2006 20:00	19.3	6.05	5.75	0.127	0.09	0.195	65.6
9/11/2006 20:15	19.29	5.89	5.75	0.127	0.09	0.195	63.9
9/11/2006 20:30	19.34	6.89	5.78	0.126	0.09	0.194	74.8
9/11/2006 20:45	19.39	7.61	5.8	0.126	0.09	0.193	82.7
9/11/2006 21:00	19.47	7.41	5.78	0.126	0.09	0.193	80.7
9/11/2006 21:15	19.51	7.72	5.79	0.125	0.09	0.193	84.1
9/11/2006 21:30	19.53	7.84	5.79	0.125	0.09	0.193	85.4
9/11/2006 21:45	19.55	7.93	5.79	0.125	0.09	0.193	86.4
9/11/2006 22:00	19.56	8.06	5.79	0.125	0.09	0.193	87.9
9/11/2006 22:15	19.55	8.1	5.79	0.125	0.09	0.193	88.3
9/11/2006 22:30	19.54	8.09	5.8	0.125	0.09	0.193	88.2
9/11/2006 22:45	19.54	8.08	5.8	0.125	0.09	0.193	88.1
9/11/2006 23:00	19.52	7.98	5.8	0.125	0.09	0.193	86.9
9/11/2006 23:15	19.48	7.91	5.8	0.125	0.09	0.193	86.2
9/11/2006 23:30	19.44	7.86	5.81	0.125	0.09	0.193	85.5
9/11/2006 23:45	19.39	7.78	5.81	0.125	0.09	0.193	84.6

## Appendix B. PHREEQC Files

### B-1: Partial input file for Example 9 (Parkhurst and Appelo 1999)

```
TITLE Example 9.--Kinetically controlled oxidation of ferrous iron.
# Decoupled valence states of iron.
SOLUTION_MASTER_SPECIES
Fe_di          Fe_di+2    0.0    Fe_di          55.847
Fe_tri         Fe_tri+3   0.0    Fe_tri         55.847
SOLUTION_SPECIES
Fe_di+2 = Fe_di+2
          log_k    0.0
Fe_tri+3 = Fe_tri+3
          log_k    0.0
#
# Fe+2 species
#
Fe_di+2 + H2O = Fe_diOH+ + H+
          log_k    -9.5
          delta_h 13.20    kcal
#
#... and also other Fe+2 species
#
#
# Fe+3 species
#
Fe_tri+3 + H2O = Fe_triOH+2 + H+
          log_k    -2.19
          delta_h 10.4    kcal
#
#... and also other Fe+3 species
#
PHASES
Goethite
          Fe_triOOH + 3 H+ = Fe_tri+3 + 2 H2O
          log_k    -1.0
END
SOLUTION 1
pH 7.0
pe 10.0 O2(g) -0.67
Fe_di 0.1
Na 10.
Cl 10. charge
EQUILIBRIUM_PHASES 1
O2(g) -0.67
RATES
Fe_di_ox
-start
10 Fe_di = TOT("Fe_di")
20 if (Fe_di <= 0) then goto 200
30 p_o2 = 10^(SI("O2(g)"))
40 moles = (2.91e-9 + 1.33e12 * (ACT("OH-"))^2 * p_o2) * Fe_di * TIME
200 SAVE moles
-end
KINETICS 1
Fe_di_ox
```

```
-formula Fe_di -1.0 Fe_tri 1.0
-steps 100 400 3100 10800 21600 5.04e4 8.64e4 1.728e5 1.728e5 1.728e5
1.728e5
INCREMENTAL_REACTIONS true
SELECTED_OUTPUT
-file ex9.sel
-reset false
USER_PUNCH
-headings Days Fe(2) Fe(3) pH si_goethite
10 PUNCH SIM_TIME/3600/24 TOT("Fe_di")*1e6, TOT("Fe_tri")*1e6, -LA("H+"),
SI("Goethite")
END
```

## B-2: Mantua PHREEQC model complete input and output file

Input file: F:\Thesis\Kinetics17.ppt  
 Output file: F:\Thesis\Kinetics17.ppt  
 Database file: E:\Program Files\UGS\Phreeqc Interactive 2.12.5\phreeqc.dat

Reading data base.

```
SOLUTION_MASTER_SPECIES
SOLUTION_SPECIES
PHASES
EXCHANGE_MASTER_SPECIES
EXCHANGE_SPECIES
SURFACE_MASTER_SPECIES
SURFACE_SPECIES
RAVIES
END
```

Reading input data for simulation 1.

DATABASE E:\Program Files\UGS\Phreeqc Interactive  
 2.12.5\phreeqc.dat  
 TITLE Example 9.--Kinetically controlled oxidation of ferrous  
 iron. Decoupled valence states of iron.

```
SOLUTION_MASTER_SPECIES
Fe_di      Fe_di+2  0.0    Fe_di
55.847     Fe_tri    Fe_tri+3  0.0    Fe_tri
55.847
```

```
SOLUTION_SPECIES
Fe_di+2 = Fe_di+2
log_k 0.0
Fe_tri+3 = Fe_tri+3
log_k 0.0
Fe_di+2 + H2O = Fe_diOH+ + H+
log_k -9.5
delta_h 13.20 kcal
Fe_di+2 + Cl- = Fe_diCl+
log_k 0.14
Fe_di+2 + CD3-2 = Fe_diCO3
log_k 4.38
Fe_di+2 + HCO3- = Fe_diHCO3+
log_k 2.0
Fe_di+2 + SO4-2 = Fe_diSO4
log_k 2.25
delta_h 3.230 kcal
Fe_di+2 + HSO4- = Fe_diHSO4+
log_k 1.08
Fe_di+2 + ZHS- = Fe_di(HS)2
log_k 8.95
Fe_di+2 + FHS- = Fe_di(HS)3-
log_k 10.987
Fe_di+2 + HFO4-2 = Fe_diHFO4
log_k 3.6
Fe_di+2 + H2FO4- = Fe_diH2FO4+
log_k 2.7
Fe_di+2 + F- = Fe_diF+
log_k 1.0
Fe_tri+3 + H2O = Fe_triOH2+ + H+
log_k -2.19
delta_h 10.4 kcal
Fe_tri+3 + 2 H2O = Fe_tri(OH)2+ + 2 H+
log_k -5.67
delta_h 17.1 kcal
Fe_tri+3 + 3 H2O = Fe_tri(OH)3 + 3 H+
log_k -12.56
delta_h 24.8 kcal
Fe_tri+3 + 4 H2O = Fe_tri(OH)4- + 4 H+
log_k -21.6
delta_h 31.9 kcal
2 Fe_tri+3 + 2 H2O = Fe_tri2(OH)2+4 + 2 H+
log_k -2.95
delta_h 13.5 kcal
3 Fe_tri+3 + 4 H2O = Fe_tri3(OH)4+5 + 4 H+
log_k -6.3
delta_h 14.3 kcal
Fe_tri+3 + Cl- = Fe_triCl+2
log_k 1.48
delta_h 5.6 kcal
Fe_tri+3 + 2 Cl- = Fe_triCl2+
log_k 2.13
Fe_tri+3 + 3 Cl- = Fe_triCl3
log_k 1.13
Fe_tri+3 + SO4-2 = Fe_triSO4+
log_k 4.04
delta_h 3.91 kcal
Fe_tri+3 + HSO4- = Fe_triHSO4+2
log_k 2.48
Fe_tri+3 + 2 SO4-2 = Fe_tri(SO4)2-
log_k 5.38
delta_h 4.60 kcal
Fe_tri+3 + HFO4-2 = Fe_triHFO4+
log_k 5.43
delta_h 5.76 kcal
Fe_tri+3 + H2FO4- = Fe_triH2FO4+2
log_k 5.43
Fe_tri+3 + F- = Fe_triF+2
log_k 6.2
delta_h 2.7 kcal
Fe_tri+3 + 2 F- = Fe_triF2+
log_k 10.8
delta_h 4.8 kcal
Fe_tri+3 + 3 F- = Fe_triF3
log_k 14.0
delta_h 5.4 kcal
EQUILIBRIUM_PHASES 3
Fe(CH)3(a) 0 10
END
```

=====

Example 9.--Kinetically controlled oxidation of ferrous  
 iron. Decoupled valence states of iron.

End of simulation.

Reading input data for simulation 2.

```
SOLUTION 1
pH 4.535
pe -0.924 O2(g) -0.785
Fe_di 0.161
Na 0.4183
Cl 0.3216 charge
K 0.0527
Mg 0.9719
Mn 0.0003951
Ca 147.6
Alkalinity 29.67
C 138.9
S 15.79
EQUILIBRIUM_PHASES 1
O2(g) -0.785
RAVIES
Fe_di_ox
start
10 Fe_di = TOT("Fe_di")
20 if (Fe_di <= 0) then goto 200
30 p_c2 = 10*(SI("O2(g)"))
40 moles = (2.91e-9 + 4e13 * (ACT("H-"))^2 * p_c2) * Fe_di *
TIME
200 SAVE moles
end
KINETICS 1
Fe_di_ox
formula Fe_di -1.0 Fe_tri 1.0
steps 100 400 3100 10800 21600 5.04e4 8.64e4 1.728e5
1.728e5 1.728e5 1.728e5
INCREMENTAL_REACTIONS true
SELECTED_OUTPUT
file kin17.sel
reset false
USER_PUNCH
headings Days Fe(2) Fe(3) pH si_Fe(CH)3(a)
10 PUNCH SIM_TIME/3600/24 TOT("Fe_di")*1e6, TOT("Fe_tri")*1e6,
-IA("H-"), SI("Fe(CH)3(a)")
END
```

Beginning of initial solution calculations.

Initial solution 1.

pH will be adjusted to obtain desired alkalinity.

Solution composition				
Elements	Molality	Moles		
Alkalinity	2.967e-002	2.967e-002		
C	1.389e-001	1.389e-001		
Ca	1.476e-001	1.476e-001		
Cl	2.367e-001	2.367e-001	Charge balance	
Fe_di	1.610e-004	1.610e-004		
K	5.270e-005	5.270e-005		
Mg	9.719e-004	9.719e-004		
Mn	3.951e-007	3.951e-007		
Na	4.183e-004	4.183e-004		
S	1.579e-002	1.579e-002		
Description of solution				
O2(g)	pH = 5.434	Adjust alkalinity		
	pe = 15.168	Equilibrium with		
	Activity of water = 0.991			
	Ionic strength = 4.068e-001			
	Mass of water (kg) = 1.000e+000			
	Total CO2 (mol/kg) = 1.389e-001			
	Temperature (deg C) = 25.000			
	Electrical balance (eq) = -3.112e-015			
	Percent error, 100*(Cat-[An])/(Cat+[An]) = -0.00			
	Iterations = 19			
	Total H = 1.110421e+002			
	Total O = 5.587722e+001			
Distribution of species				
Log	Species	Molality	Activity	
Gamma				
	H+	4.766e-006	3.678e-006	-5.322 -5.434
-0.113	OH-	4.154e-009	2.698e-009	-8.382 -8.569
-0.187	H2O	5.551e+001	9.911e-001	1.744 -0.004
0.000				
C(-4)	0.000e+000			
0.041	CH4	0.000e+000	0.000e+000	-141.384 -141.344
C(4)	1.389e-001			



0.041	CO2	1.092e-001	1.200e-001	-0.962	-0.921
-0.152	HCO3-	2.043e-002	1.438e-002	-1.690	-1.842
-0.152	CaHCO3+	9.116e-003	6.417e-003	-2.040	-2.193
-0.136	MgHCO3+	5.781e-005	4.225e-005	-4.238	-4.374
-0.136	Fe_dihHCO3+	5.274e-005	3.854e-005	-4.278	-4.414
-0.136	CaCO3	9.811e-006	1.077e-005	-5.008	-4.968
0.041	NaHCO3	2.172e-006	2.386e-006	-5.663	-5.622
0.041	CO3-2	7.466e-007	1.834e-007	-6.127	-6.737
-0.610	Fe_diiCO3	1.074e-007	1.179e-007	-6.969	-6.928
0.041	MnHCO3+	1.037e-007	7.582e-008	-6.984	-7.120
-0.136	MgCO3	4.001e-008	4.394e-008	-7.398	-7.357
-0.136	NaCO3-	1.378e-009	1.007e-009	-8.861	-8.997
0.041	MnCO3	7.846e-010	8.617e-010	-9.105	-9.065
0.041	Ca	1.476e-001			
-0.568	Ca+2	1.293e-001	3.498e-002	-0.889	-1.456
0.041	CaSO4	9.212e-003	1.012e-002	-2.036	-1.995
-0.152	CaHCO3+	9.116e-003	6.417e-003	-2.040	-2.193
0.041	CaCO3	9.811e-006	1.077e-005	-5.008	-4.968
-0.136	CaHSO4+	2.982e-007	2.180e-007	-6.525	-6.662
-0.136	CaOH+	2.141e-009	1.565e-009	-8.669	-8.806
-0.136	Cl	2.367e-001			
-0.181	Cl-	2.367e-001	1.559e-001	-0.626	-0.807
-0.136	Fe_diiCl+	7.893e-006	5.768e-006	-5.103	-5.239
-0.136	MnCl+	5.141e-008	3.757e-008	-7.289	-7.425
-0.136	MnCl2	2.328e-009	2.557e-009	-8.633	-8.592
0.041	MnCl3-	1.502e-010	1.098e-010	-9.823	-9.960
-0.136	Fe_dii	1.610e-004			
-0.545	Fe_dii+2	9.396e-005	2.681e-005	-4.027	-4.572
-0.136	Fe_diiHCO3+	5.274e-005	3.854e-005	-4.278	-4.414
-0.136	Fe_diiCl+	7.893e-006	5.768e-006	-5.103	-5.239
-0.136	Fe_diiSO4	6.292e-006	6.909e-006	-5.201	-5.161
0.041	Fe_diiCO3	1.074e-007	1.179e-007	-6.969	-6.928
0.041	Fe_diiOH+	3.126e-009	2.284e-009	-8.505	-8.641
-0.136	Fe_diiHSO4+	2.285e-010	1.670e-010	-9.641	-9.777
-0.136	Fe_dii(HS)2	0.000e+000	0.000e+000	-274.519	-274.479
0.041	Fe_dii(HS)3-	0.000e+000	0.000e+000	-411.734	-411.870
-0.136	H(0)	0.000e+000			
0.041	H2	0.000e+000	0.000e+000	-44.396	-44.355
0.041	K	5.270e-005			
-0.181	K+	5.222e-005	3.439e-005	-4.282	-4.464
-0.136	KSO4-	4.793e-007	3.503e-007	-6.319	-6.456
0.041	KOH	2.927e-014	3.214e-014	-13.534	-13.493
0.041	Mg	9.719e-004			
-0.523	Mg+2	8.364e-004	2.511e-004	-3.078	-3.600
0.041	MgSO4	7.770e-005	8.532e-005	-4.110	-4.069
-0.136	MgHCO3+	5.781e-005	4.225e-005	-4.238	-4.374
-0.136	MgCO3	4.001e-008	4.394e-008	-7.398	-7.357
0.041	MgOH+	3.362e-010	2.457e-010	-9.473	-9.610
-0.136	Mn(2)	3.951e-007			
-0.576	Mn+2	2.228e-007	5.916e-008	-6.652	-7.228
-0.136	MnHCO3+	1.037e-007	7.582e-008	-6.984	-7.120
-0.136	MnCl+	5.141e-008	3.757e-008	-7.289	-7.425
0.041	MnSO4	1.389e-008	1.525e-008	-7.857	-7.817
0.041	MnCl2	2.328e-009	2.557e-009	-8.633	-8.592
0.041	MnCO3	7.846e-010	8.617e-010	-9.105	-9.065
0.041	MnCl3-	1.502e-010	1.098e-010	-9.823	-9.960
-0.136	MnOH+	5.608e-013	4.098e-013	-12.251	-12.387
-0.136	Mn(3)	4.528e-017			
-1.226	Mn+3	4.528e-017	2.693e-018	-16.344	-17.570
-0.146	Na	4.183e-004			
-0.146	Na+	4.132e-004	2.950e-004	-3.384	-3.530
-0.136	NaSO4-	2.933e-006	2.143e-006	-5.533	-5.669
0.041	NaHCO3	2.172e-006	2.386e-006	-5.663	-5.622
-0.136	NaCO3-	1.378e-009	1.007e-009	-8.861	-8.997

0.041	NaOH	4.784e-013	5.253e-013	-12.320	-12.280
0(0)	3.828e-004				
0.041	O2	1.914e-004	2.102e-004	-3.718	-3.677
0.041	S(-2)	0.000e+000			
0.041	H2S	0.000e+000	0.000e+000	-137.962	-137.921
-0.187	HS-	0.000e+000	0.000e+000	-139.241	-139.429
-0.635	S-2	0.000e+000	0.000e+000	-146.277	-146.912
0.041	Fe_dii(HS)2	0.000e+000	0.000e+000	-274.519	-274.479
-0.136	Fe_dii(HS)3-	0.000e+000	0.000e+000	-411.734	-411.870
0.041	CaSO4	9.212e-003	1.012e-002	-2.036	-1.995
0.041	SO4-2	6.490e-003	1.449e-003	-2.188	-2.839
-0.651	MgSO4	7.770e-005	8.532e-005	-4.110	-4.069
0.041	Fe_diiSO4	6.292e-006	6.909e-006	-5.201	-5.161
-0.136	NaSO4-	2.933e-006	2.143e-006	-5.533	-5.669
-0.136	HSO4-	7.091e-007	5.183e-007	-6.149	-6.285
-0.136	KSO4-	4.793e-007	3.503e-007	-6.319	-6.456
-0.136	CaHSO4+	2.982e-007	2.180e-007	-6.525	-6.662
0.041	MnSO4	1.389e-008	1.525e-008	-7.857	-7.817
-0.136	Fe_diiHSO4+	2.285e-010	1.670e-010	-9.641	-9.777

Saturation indices

Phase	SI	log IAP	log KI	
Anhydrite	0.07	-4.29	-4.36	CaSO4
Aragonite	0.14	-8.19	-8.34	CaCO3
Calcite	0.29	-8.19	-8.48	CaCO3
CHA(g)	-138.48	-141.34	-2.86	CHA
CO2(g)	0.55	-0.92	-1.47	CO2
Dolomite	-1.44	-18.53	-17.09	CaMg(CO3)2
Gypsum	0.28	-4.30	-4.58	CaSO4.2H2O
H2(g)	-41.21	-44.36	-3.15	H2
H2O(g)	-1.51	-0.00	1.51	H2O
H2S(g)	-136.92	-137.92	-1.00	H2S
Halite	-5.92	-4.34	1.58	NaCl
Hausmannite	-8.92	52.11	61.03	Mn3O4
Manganite	-1.10	24.24	25.34	MnOOH
O2(g)	-0.78	-3.68	-2.89	O2
Pyrochroite	-11.57	3.63	15.20	Mn(OH)2
Pyrolusite	3.46	44.84	41.38	MnO2
Rhodochrosite	-2.83	-13.96	-11.13	MnCO3
Sulfur	-101.60	-96.72	4.88	S

Beginning of batch-reaction calculations.

Reaction step 1.

Using solution 1.  
Using pure phase assemblage 1.  
Using kinetics 1. Kinetics defined in simulation 2.

Kinetics 1. Kinetics defined in simulation 2.

Time step: 100 seconds (Incremented time: 100 seconds)

Coefficient	Rate name	Delta Moles	Total Moles	Reactant
-1	Fe_dii_cx	-7.679e-007	1.000e+000	Fe_dii
1				Fe_tri

Phase assemblage

Delta	Phase	SI	log IAP	log KI	Moles in assemblage	Initial	Final
1.920e-007	O2(g)	-0.78	-3.68	-2.89	1.000e+001	1.000e+001-	

Solution composition

Elements	Molality	Moles
C	1.389e-001	1.389e-001
Ca	1.476e-001	1.476e-001
Cl	2.367e-001	2.367e-001
Fe_dii	1.602e-004	1.602e-004
Fe_tri	7.679e-007	7.679e-007
K	5.270e-005	5.270e-005
Mg	9.719e-004	9.719e-004
Mn	3.951e-007	3.951e-007
Na	4.183e-004	4.183e-004
S	1.579e-002	1.579e-002

Description of solution

equilibrium	pH =	5.434	Charge balance
	pe =	15.168	Adjusted to redox
	Activity of water =	0.991	
	Ionic strength =	4.068e-001	
	Mass of water (kg) =	1.000e+000	

Total alkalinity (eq/kg) = 2.967e-002  
 Total CO2 (mol/kg) = 1.389e-001  
 Temperature (deg C) = 25.000  
 Electrical balance (eq) = -1.008e-014  
 Percent error, 100\*(Cat-[An])/[Cat+[An]] = -0.00  
 Iterations = 41  
 Total H = 1.110421e+002  
 Total O = 5.587722e+001

Distribution of species

Log Gamma	Species	Molality	Activity	Log Molality	Log Activity
-0.113	H+	4.767e-006	3.678e-006	-5.322	-5.434
-0.187	OH-	4.154e-009	2.698e-009	-8.382	-8.569
0.000	H2O	5.551e+001	9.911e-001	1.744	-0.004
C(-4)	0.000e+000				
0.041	CH4	0.000e+000	0.000e+000	-141.384	-141.344
C(4)	1.389e-001				
0.041	CO2	1.092e-001	1.200e-001	-0.962	-0.921
-0.152	HCO3-	2.043e-002	1.438e-002	-1.690	-1.842
-0.152	CaHCO3+	9.116e-003	6.417e-003	-2.040	-2.193
-0.136	MgHCO3+	5.781e-005	4.225e-005	-4.238	-4.374
-0.136	Fe_dihCO3+	5.249e-005	3.836e-005	-4.280	-4.416
-0.136	CaCO3	9.811e-006	1.077e-005	-5.008	-4.968
0.041	NaHCO3	2.172e-006	2.386e-006	-5.663	-5.622
0.041	CO3-2	7.466e-007	1.833e-007	-6.127	-6.737
-0.610	Fe_dico3	1.068e-007	1.173e-007	-6.971	-6.931
0.041	MnHCO3+	1.037e-007	7.582e-008	-6.984	-7.120
-0.136	MgCO3	4.001e-008	4.393e-008	-7.398	-7.357
0.041	NaCO3-	1.378e-009	1.007e-009	-8.861	-8.997
-0.136	MnCO3	7.846e-010	8.617e-010	-9.105	-9.065
0.041	Ca	1.476e-001			
-0.568	Ca+2	1.293e-001	3.498e-002	-0.889	-1.456
0.041	CaSO4	9.212e-003	1.012e-002	-2.036	-1.995
-0.152	CaHCO3+	9.116e-003	6.417e-003	-2.040	-2.193
0.041	CaCO3	9.811e-006	1.077e-005	-5.008	-4.968
-0.136	CaHSO4+	2.982e-007	2.180e-007	-6.525	-6.662
-0.136	CaOH+	2.141e-009	1.564e-009	-8.669	-8.806
0.041	Cl-	2.367e-001	1.559e-001	-0.626	-0.807
-0.181	Fe_dicl+	7.855e-006	5.741e-006	-5.105	-5.241
-0.136	MnCl+	5.141e-008	3.757e-008	-7.289	-7.425
-0.136	MnCl2	2.328e-009	2.557e-009	-8.633	-8.592
0.041	MnCl3-	1.502e-010	1.098e-010	-9.823	-9.960
-0.136	Fe_triCl+2	5.669e-011	1.617e-011	-10.246	-10.791
-0.545	Fe_triCl2+	1.541e-011	1.126e-011	-10.812	-10.948
-0.136	Fe_triCl3	1.599e-013	1.756e-013	-12.796	-12.756
0.041	Fe_di	1.602e-004			
-0.545	Fe_di+2	9.352e-005	2.668e-005	-4.029	-4.574
-0.136	Fe_dihCO3+	5.249e-005	3.836e-005	-4.280	-4.416
-0.136	Fe_dicl+	7.855e-006	5.741e-006	-5.105	-5.241
-0.136	Fe_dico3	6.262e-006	6.876e-006	-5.203	-5.163
0.041	Fe_dico3	1.068e-007	1.173e-007	-6.971	-6.931
0.041	Fe_dioH+	3.111e-009	2.274e-009	-8.507	-8.643
-0.136	Fe_dihSO4+	2.275e-010	1.662e-010	-9.643	-9.779
-0.136	Fe_di(HS)2	0.000e+000	0.000e+000	-274.522	-274.481
0.041	Fe_di(HS)3-	0.000e+000	0.000e+000	-411.736	-411.872
-0.136	Fe_tri	7.679e-007			
-0.136	Fe_tri(CH)2+	7.299e-007	5.334e-007	-6.137	-6.273
-0.545	Fe_triCH+2	2.095e-008	5.978e-009	-7.679	-8.223
-0.545	Fe_tri(CH)3	1.686e-008	1.852e-008	-7.773	-7.732
0.041	Fe_triso4+	7.471e-011	5.460e-011	-10.127	-10.263
-0.136	Fe_tri+3	5.776e-011	3.436e-012	-10.238	-11.464
-1.226	Fe_triCl+2	5.669e-011	1.617e-011	-10.246	-10.791
-0.545	Fe_triCl2+	1.541e-011	1.126e-011	-10.812	-10.948
-0.136	Fe_tri(CH)4-	6.228e-012	4.551e-012	-11.206	-11.342

-0.136	Fe_tri(SO4)2-	2.369e-012	1.731e-012	-11.625	-11.762
0.041	Fe_triCl3	1.599e-013	1.756e-013	-12.796	-12.756
-2.179	Fe_tri2(CH)2+4	1.452e-013	9.618e-016	-12.838	-15.017
-0.545	Fe_trihSO4+2	1.885e-015	5.377e-016	-14.725	-15.269
-3.405	Fe_tri3(CH)4+5	2.721e-016	1.072e-019	-15.565	-18.970
H(0)	0.000e+000				
0.041	H2	0.000e+000	0.000e+000	-44.396	-44.355
K	5.270e-005				
-0.181	K+	5.222e-005	3.439e-005	-4.282	-4.464
-0.136	KSO4-	4.793e-007	3.503e-007	-6.319	-6.456
0.041	KOH	2.927e-014	3.214e-014	-13.534	-13.493
Mg	9.719e-004				
-0.523	Mg+2	8.364e-004	2.511e-004	-3.078	-3.600
0.041	MgSO4	7.770e-005	8.532e-005	-4.110	-4.069
-0.136	MgHCO3+	5.781e-005	4.225e-005	-4.238	-4.374
0.041	MgCO3	4.001e-008	4.393e-008	-7.398	-7.357
-0.136	MgOH+	3.362e-010	2.457e-010	-9.473	-9.610
Mn(2)	3.951e-007				
-0.576	Mn+2	2.228e-007	5.916e-008	-6.652	-7.228
-0.136	MnHCO3+	1.037e-007	7.582e-008	-6.984	-7.120
-0.136	MnCl+	5.141e-008	3.757e-008	-7.289	-7.425
0.041	MnSO4	1.389e-008	1.525e-008	-7.857	-7.817
0.041	MnCl2	2.328e-009	2.557e-009	-8.633	-8.592
0.041	MnCO3	7.846e-010	8.617e-010	-9.105	-9.065
-0.136	MnCl3-	1.502e-010	1.098e-010	-9.823	-9.960
-0.136	MnOH+	5.608e-013	4.098e-013	-12.251	-12.387
Mn(3)	4.528e-017				
-1.226	Mn+3	4.528e-017	2.693e-018	-16.344	-17.570
Na	4.183e-004				
-0.146	Na+	4.132e-004	2.950e-004	-3.384	-3.530
-0.136	NaSO4-	2.933e-006	2.143e-006	-5.533	-5.669
0.041	NaHCO3	2.172e-006	2.386e-006	-5.663	-5.622
-0.136	NaCO3-	1.378e-009	1.007e-009	-8.861	-8.997
0.041	NaOH	4.784e-013	5.253e-013	-12.320	-12.280
O(0)	3.828e-004				
0.041	O2	1.914e-004	2.102e-004	-3.718	-3.677
S(-2)	0.000e+000				
0.041	H2S	0.000e+000	0.000e+000	-137.962	-137.921
-0.187	HS-	0.000e+000	0.000e+000	-139.241	-139.428
-0.635	S-2	0.000e+000	0.000e+000	-146.277	-146.912
0.041	Fe_di(HS)2	0.000e+000	0.000e+000	-274.522	-274.481
-0.136	Fe_di(HS)3-	0.000e+000	0.000e+000	-411.736	-411.872
S(6)	1.579e-002				
0.041	CaSO4	9.212e-003	1.012e-002	-2.036	-1.995
-0.651	SO4-2	6.490e-003	1.449e-003	-2.188	-2.839
0.041	MgSO4	7.770e-005	8.532e-005	-4.110	-4.069
0.041	Fe_diso4	6.262e-006	6.876e-006	-5.203	-5.163
-0.136	NaSO4-	2.933e-006	2.143e-006	-5.533	-5.669
-0.136	HSO4-	7.092e-007	5.183e-007	-6.149	-6.285
-0.136	KSO4-	4.793e-007	3.503e-007	-6.319	-6.456
-0.136	CaHSO4+	2.982e-007	2.180e-007	-6.525	-6.662
-0.136	MnSO4	1.389e-008	1.525e-008	-7.857	-7.817
-0.136	Fe_dihSO4+	2.275e-010	1.662e-010	-9.643	-9.779
-0.136	Fe_triso4+	7.471e-011	5.460e-011	-10.127	-10.263
-0.136	Fe_tri(SO4)2-	2.369e-012	1.731e-012	-11.625	-11.762
-0.545	Fe_trihSO4+2	1.885e-015	5.377e-016	-14.725	-15.269

Saturation indices

Phase	SI	log IAP	log KI
Anhydrite	0.07	-4.29	-4.36
Aragonite	0.14	-8.19	-8.34
Calcite	0.29	-8.19	-8.48
CH4(g)	-138.48	-141.34	-2.86
CO2(g)	0.55	-0.92	-1.47
Dolomite	-1.44	-18.53	-17.09
Gypsum	0.28	-4.30	-4.58
H2(g)	-41.21	-44.36	-3.15
H2O(g)	-1.51	-0.00	1.51
H2S(g)	-136.92	-137.92	-1.00

Halite	-5.92	-4.34	1.58	NaCl
Hausmannite	-8.92	52.11	61.03	Mn3O4
Manganite	-1.10	24.24	25.34	MnOOH
O2(g)	-0.78	-3.68	-2.89	O2
Pyrochroite	-11.57	3.63	15.20	Mn(OH)2
Pyrolusite	3.46	44.84	41.38	MnO2
Rhodochrosite	-2.83	-13.96	-11.13	MnCO3
Sulfur	-101.60	-96.72	4.88	S

Reaction step 2.

Using solution 1.

Using pure phase assemblage 1.

Using Kinetics 1. Kinetics defined in simulation 2.

Kinetics 1. Kinetics defined in simulation 2.

Time step: 400 seconds (Incremented time: 500 seconds)

Coefficient	Rate name	Delta	Moles	Total Moles	Reactant
-1	Fe_di_ox	-3.032e-006	1.000e+000		Fe_di
1					Fe_tri

-----Phase assemblage-----

Delta	Phase	Moles in assemblage			
		SI	log IAP	log KT	Initial Final
7.581e-007	O2(g)	-0.79	-3.68	-2.89	1.000e+001 1.000e+001

-----Solution composition-----

Elements	Molality	Moles
C	1.389e-001	1.389e-001
Ca	1.476e-001	1.476e-001
Cl	2.367e-001	2.367e-001
Fe_di	1.572e-004	1.572e-004
Fe_tri	3.800e-006	3.800e-006
K	5.270e-005	5.270e-005
Mg	9.719e-004	9.719e-004
Mn	3.951e-007	3.951e-007
Na	4.183e-004	4.183e-004
S	1.579e-002	1.579e-002

-----Description of solution-----

equilibrium	pH =	5.434	Charge balance
	pe =	15.168	Adjusted to redox
	Activity of water =	0.991	
	Ionic strength =	4.068e-001	
	Mass of water (kg) =	1.000e+000	
	Total alkalinity (eq/kg) =	2.967e-002	
	Total CO2 (mol/kg) =	1.389e-001	
	Temperature (deg C) =	25.000	
	Electrical balance (eq) =	2.518e-014	
	Percent error, 100*(Cat- An )/( Cat+ An ) =	0.00	
	Iterations =	47	
	Total H =	1.110421e+002	
	Total O =	5.587723e+001	

-----Distribution of species-----

Log Gamma	Species	Log			
		Molality	Activity	Molality	Activity
-0.113	H+	4.767e-006	3.678e-006	-5.322	-5.434
-0.187	OH-	4.154e-009	2.698e-009	-8.382	-8.569
0.000	H2O	5.551e+001	9.911e-001	1.744	-0.004
C(-4)	0.000e+000				
0.041	CH4	0.000e+000	0.000e+000	-141.384	-141.344
0.041	CO2	1.389e-001	1.092e-001	1.200e-001	-0.962
-0.152	HCO3-	2.042e-002	1.438e-002	-1.690	-1.842
-0.152	CaHCO3+	9.115e-003	6.417e-003	-2.040	-2.193
-0.136	MgHCO3+	5.780e-005	4.225e-005	-4.238	-4.374
-0.136	Fe_diHCO3+	5.149e-005	3.763e-005	-4.288	-4.424
0.041	CaCO3	9.809e-006	1.077e-005	-5.008	-4.968
0.041	NaHCO3	2.172e-006	2.385e-006	-5.663	-5.622
-0.610	CO3-2	7.464e-007	1.833e-007	-6.127	-6.737
0.041	Fe_diCO3	1.048e-007	1.151e-007	-6.980	-6.939
-0.136	MnHCO3+	1.037e-007	7.581e-008	-6.984	-7.120
0.041	MgCO3	4.000e-008	4.393e-008	-7.398	-7.357
-0.136	NaCO3-	1.378e-009	1.007e-009	-8.861	-8.997
0.041	MnCO3	7.845e-010	8.615e-010	-9.105	-9.065
-0.568	Ca	1.476e-001	1.293e-001	3.498e-002	-0.889
	Ca+2				-1.456

0.041	CaSO4	9.212e-003	1.012e-002	-2.036	-1.995
-0.152	CaHCO3+	9.115e-003	6.417e-003	-2.040	-2.193
0.041	CaCO3	9.809e-006	1.077e-005	-5.008	-4.968
-0.136	CaHSO4+	2.983e-007	2.180e-007	-6.525	-6.662
-0.136	CaOH+	2.140e-009	1.564e-009	-8.669	-8.806
-0.181	Cl	2.367e-001	1.559e-001	-0.626	-0.807
-0.136	Fe_diCl+	7.707e-006	5.632e-006	-5.113	-5.249
-0.136	MnCl+	5.141e-008	3.757e-008	-7.289	-7.425
0.041	MnCl2	2.328e-009	2.557e-009	-8.633	-8.592
-0.545	Fe_triCl+2	2.806e-010	8.005e-011	-9.552	-10.097
-0.136	MnCl3-	1.502e-010	1.098e-010	-9.823	-9.959
-0.136	Fe_triCl2+	7.627e-011	5.574e-011	-10.118	-10.254
0.041	Fe_triCl3	7.912e-013	8.689e-013	-12.102	-12.061
-0.545	Fe_di	1.572e-004	1.572e-004		
-0.136	Fe_di+2	9.175e-005	2.617e-005	-4.037	-4.582
-0.136	Fe_diHCO3+	5.149e-005	3.763e-005	-4.288	-4.424
-0.136	Fe_diCl+	7.707e-006	5.632e-006	-5.113	-5.249
0.041	Fe_diSO4	6.143e-006	6.746e-006	-5.212	-5.171
-0.136	Fe_diCO3	1.048e-007	1.151e-007	-6.980	-6.939
-0.136	Fe_diOH+	3.052e-009	2.230e-009	-8.515	-8.652
-0.136	Fe_diHSO4+	2.232e-010	1.631e-010	-9.651	-9.788
0.041	Fe_di(HS)2	0.000e+000	0.000e+000	-274.530	-274.489
-0.136	Fe_di(HS)3-	0.000e+000	0.000e+000	-411.744	-411.880
-0.136	Fe_tri	3.800e-006	3.800e-006		
-0.136	Fe_tri(H)2+	3.612e-006	2.640e-006	-5.442	-5.578
-0.545	Fe_triOH+2	1.037e-007	2.958e-008	-6.984	-7.529
0.041	Fe_tri(H)3	8.344e-008	9.163e-008	-7.079	-7.038
-0.136	Fe_triSO4+	3.698e-010	2.702e-010	-9.432	-9.568
-1.226	Fe_tri+3	2.859e-010	1.700e-011	-9.544	-10.769
-0.545	Fe_triCl+2	2.806e-010	8.005e-011	-9.552	-10.097
-0.136	Fe_triCl2+	7.627e-011	5.574e-011	-10.118	-10.254
-0.136	Fe_tri(H)4-	3.081e-011	2.252e-011	-10.511	-10.647
-0.136	Fe_tri(SO4)2-	1.173e-011	8.569e-012	-10.931	-11.067
-0.136	Fe_tri2(H)2+4	3.556e-012	2.355e-014	-11.449	-13.628
-2.179	Fe_triCl3	7.912e-013	8.689e-013	-12.102	-12.061
0.041	Fe_tri3(H)4+5	3.297e-014	1.299e-017	-13.482	-16.886
-3.405	Fe_triHSO4+2	9.330e-015	2.662e-015	-14.030	-14.575
-0.545	H(O)	0.000e+000	0.000e+000		
-0.545	H2	0.000e+000	0.000e+000	-44.396	-44.355
0.041	K	5.270e-005	5.270e-005		
-0.181	K+	5.222e-005	3.439e-005	-4.282	-4.464
-0.136	KSO4-	4.793e-007	3.503e-007	-6.319	-6.456
0.041	KOH	2.926e-014	3.214e-014	-13.534	-13.493
-0.523	Mg	9.719e-004	9.719e-004		
0.041	Mg+2	8.364e-004	2.511e-004	-3.078	-3.600
0.041	MgSO4	7.770e-005	8.533e-005	-4.110	-4.069
-0.136	MgHCO3+	5.780e-005	4.225e-005	-4.238	-4.374
0.041	MgCO3	4.000e-008	4.393e-008	-7.398	-7.357
-0.136	MgOH+	3.362e-010	2.457e-010	-9.473	-9.610
-0.136	Mn	3.951e-007	3.951e-007		
-0.576	Mn+2	2.228e-007	5.917e-008	-6.652	-7.228
-0.136	MnHCO3+	1.037e-007	7.581e-008	-6.984	-7.120
-0.136	MnCl+	5.141e-008	3.757e-008	-7.289	-7.425
0.041	MnSO4	1.389e-008	1.525e-008	-7.857	-7.817
0.041	MnCl2	2.328e-009	2.557e-009	-8.633	-8.592
0.041	MnCO3	7.845e-010	8.615e-010	-9.105	-9.065
-0.136	MnCl3-	1.502e-010	1.098e-010	-9.823	-9.959
-0.136	MnOH+	5.607e-013	4.098e-013	-12.251	-12.387
-1.226	Mn(3)	4.528e-017	4.528e-017		
-0.146	Mn+3	4.528e-017	2.693e-018	-16.344	-17.570
-0.146	Na	4.183e-004	4.183e-004		
-0.146	Na+	4.132e-004	2.950e-004	-3.384	-3.530
-0.136	NaSO4-	2.933e-006	2.143e-006	-5.533	-5.669

0.041	NaHCO3	2.172e-006	2.385e-006	-5.663	-5.622
-0.136	NaCO3-	1.378e-009	1.007e-009	-8.861	-8.997
0.041	NaOH	4.783e-013	5.253e-013	-12.320	-12.280
0(0)	3.828e-004				
0.041	O2	1.914e-004	2.102e-004	-3.718	-3.677
0.041	S(-2)	0.000e+000	0.000e+000	-137.962	-137.921
0.041	H2S	0.000e+000	0.000e+000	-137.962	-137.921
-0.187	HS-	0.000e+000	0.000e+000	-139.241	-139.428
-0.635	S-2	0.000e+000	0.000e+000	-146.277	-146.912
-0.635	Fe_di(HS)2	0.000e+000	0.000e+000	-274.530	-274.489
0.041	Fe_di(HS)3-	0.000e+000	0.000e+000	-411.744	-411.880
-0.136	S(6)	1.579e-002			
0.041	CaSO4	9.212e-003	1.012e-002	-2.036	-1.995
-0.651	SO4-2	6.490e-003	1.449e-003	-2.188	-2.839
0.041	MgSO4	7.770e-005	8.533e-005	-4.110	-4.069
0.041	Fe_diSO4	6.143e-006	6.746e-006	-5.212	-5.171
-0.136	NaSO4-	2.933e-006	2.143e-006	-5.533	-5.669
-0.136	HSO4-	7.092e-007	5.183e-007	-6.149	-6.285
-0.136	KSO4-	4.793e-007	3.503e-007	-6.319	-6.456
-0.136	CaHSO4+	2.983e-007	2.180e-007	-6.525	-6.662
-0.136	MnSO4	1.389e-008	1.525e-008	-7.857	-7.817
0.041	Fe_triSO4+	3.698e-010	2.702e-010	-9.432	-9.568
-0.136	Fe_diHSO4+	2.232e-010	1.631e-010	-9.651	-9.788
-0.136	Fe_tri(SO4)2-	1.173e-011	8.569e-012	-10.931	-11.067
-0.136	Fe_triHSO4+2	9.330e-015	2.662e-015	-14.030	-14.575

----- Saturation indices -----

Phase	SI	log IAP	log KT	
Anhydrite	0.07	-4.29	-4.36	CaSO4
Aragonite	0.14	-8.19	-8.34	CaCO3
Calcite	0.29	-8.19	-8.48	CaCO3
CH4(g)	-138.48	-141.34	-2.86	CH4
CO2(g)	0.55	-0.92	-1.47	CO2
Dolomite	-1.44	-18.53	-17.09	CaMg(CO3)2
Gypsum	0.28	-4.30	-4.58	CaSO4.2H2O
H2(g)	-41.21	-44.36	-3.15	H2
H2O(g)	-1.51	-0.00	1.51	H2O
H2S(g)	-136.92	-137.92	-1.00	H2S
Halite	-5.92	-4.34	1.58	NaCl
Hausmannite	-8.92	52.11	61.03	Mn3O4
Manganite	-1.10	24.24	25.34	MnOOH
O2(g)	-0.79	-3.68	-2.89	O2
Pyrochroite	-11.57	3.63	15.20	Mn(OH)2
Pyrolusite	3.46	44.84	41.38	MnO2
Rhodochrosite	-2.83	-13.96	-11.13	MnCO3
Sulfur	-101.60	-96.72	4.88	S

Reaction step 3.  
Using solution 1.  
Using pure phase assemblage 1.  
Using kinetics 1. Kinetics defined in simulation 2.

Kinetics 1. Kinetics defined in simulation 2.

Time step: 3100 seconds (Incremented time: 3600 seconds)

Rate name	Delta Moles	Total Moles	Reactant
Fe_di_ox	-2.162e-005	1.000e+000	Fe_di
			Fe_tri

----- Phase assemblage -----

Phase	SI	log IAP	log KT	Moles in assemblage	
				Initial	Final
O2(g)	-0.79	-3.68	-2.89	1.000e+001	1.000e+001-

----- Solution composition -----

Elements	Molality	Moles
C	1.389e-001	1.389e-001
Ca	1.476e-001	1.476e-001
Cl	2.367e-001	2.367e-001
Fe_di	1.356e-004	1.356e-004
Fe_tri	2.542e-005	2.542e-005
K	5.270e-005	5.270e-005
Mg	9.719e-004	9.719e-004
Mn	3.951e-007	3.951e-007
Na	4.183e-004	4.183e-004
S	1.579e-002	1.579e-002

----- Description of solution -----

pH = 5.434  
pe = 15.169  
Change balance Adjusted to redox

equilibrium  
Activity of water = 0.991  
Ionic strength = 4.068e-001  
Mass of water (kg) = 1.000e+000  
Total alkalinity (eq/kg) = 2.970e-002  
Total CO2 (mol/kg) = 1.389e-001  
Temperature (deg C) = 25.000  
Electrical balance (eq) = 2.519e-014  
Percent error, 100\*(Cat-|An|)/(Cat+|An|) = 0.00  
Iterations = 44  
Total H = 1.110421e+002  
Total O = 5.587724e+001

----- Distribution of species -----

Log Gamma	Species	Molality	Activity	Log Molality	Log Activity
	H+	4.770e-006	3.681e-006	-5.321	-5.434
-0.113	OH-	4.151e-009	2.696e-009	-8.382	-8.569
-0.187	H2O	5.551e+001	9.911e-001	1.744	-0.004
0.000	C(-4)	0.000e+000	0.000e+000	-141.384	-141.344
0.041	C(4)	1.389e-001			
0.041	CO2	1.093e-001	1.200e-001	-0.962	-0.921
-0.152	HCO3-	2.041e-002	1.437e-002	-1.690	-1.843
-0.152	CaHCO3+	9.111e-003	6.414e-003	-2.040	-2.193
-0.152	MgHCO3+	5.778e-005	4.223e-005	-4.238	-4.374
-0.136	Fe_diHCO3+	4.440e-005	3.245e-005	-4.353	-4.489
-0.136	CaCO3	9.798e-006	1.076e-005	-5.009	-4.968
0.041	NaHCO3	2.171e-006	2.384e-006	-5.663	-5.623
0.041	CO3-2	7.456e-007	1.831e-007	-6.128	-6.737
-0.610	MnHCO3+	1.037e-007	7.579e-008	-6.984	-7.120
-0.136	Fe_diCO3	9.031e-008	9.917e-008	-7.044	-7.004
0.041	MgCO3	3.995e-008	4.388e-008	-7.398	-7.358
0.041	NaCO3-	1.376e-009	1.006e-009	-8.861	-8.997
-0.136	MnCO3	7.837e-010	8.606e-010	-9.106	-9.065
0.041	Ca	1.476e-001			
-0.568	Ca+2	1.293e-001	3.498e-002	-0.889	-1.456
0.041	CaSO4	9.213e-003	1.012e-002	-2.036	-1.995
-0.152	CaHCO3+	9.111e-003	6.414e-003	-2.040	-2.193
0.041	CaCO3	9.798e-006	1.076e-005	-5.009	-4.968
-0.136	CaHSO4+	2.985e-007	2.182e-007	-6.525	-6.661
-0.136	CaOH+	2.139e-009	1.563e-009	-8.670	-8.806
-0.136	Cl	2.367e-001			
-0.181	Cl-	2.367e-001	1.559e-001	-0.626	-0.807
-0.136	Fe_diCl+	6.648e-006	4.859e-006	-5.177	-5.313
-0.136	MnCl+	5.142e-008	3.758e-008	-7.289	-7.425
0.041	MnCl2	2.329e-009	2.557e-009	-8.633	-8.592
-0.545	Fe_triCl+2	1.879e-009	5.362e-010	-8.726	-9.271
-0.136	Fe_triCl2+	5.109e-010	3.733e-010	-9.292	-9.428
-0.136	MnCl3-	1.502e-010	1.098e-010	-9.823	-9.959
-0.136	Fe_triCl3	5.300e-012	5.820e-012	-11.276	-11.235
0.041	Fe_di	1.356e-004			
-0.545	Fe_di+2	7.915e-005	2.258e-005	-4.102	-4.646
-0.136	Fe_diHCO3+	4.440e-005	3.245e-005	-4.353	-4.489
-0.136	Fe_diCl+	6.648e-006	4.859e-006	-5.177	-5.313
-0.136	Fe_diSO4	5.300e-006	5.820e-006	-5.276	-5.235
0.041	Fe_diCO3	9.031e-008	9.917e-008	-7.044	-7.004
0.041	Fe_diOH+	2.631e-009	1.923e-009	-8.580	-8.716
-0.136	Fe_diHSO4+	1.927e-010	1.408e-010	-9.715	-9.851
-0.136	Fe_di(HS)2	0.000e+000	0.000e+000	-274.593	-274.553
-0.136	Fe_tri	2.542e-005			
-0.136	Fe_tri(OH)2+	2.416e-005	1.766e-005	-4.617	-4.753
-0.136	Fe_triOH+2	6.941e-007	1.980e-007	-6.159	-6.703
-0.545	Fe_tri(OH)3	5.577e-007	6.125e-007	-6.254	-6.213
0.041	Fe_triSO4+	2.477e-009	1.810e-009	-8.606	-8.742
-0.136	Fe_tri+3	1.915e-009	1.139e-010	-8.718	-9.944

-0.545	Fe_triCl+2	1.879e-009	5.362e-010	-8.726	-9.271
-0.136	Fe_triCl2+	5.109e-010	3.733e-010	-9.292	-9.428
-0.136	Fe_tri(H)4-	2.058e-010	1.504e-010	-9.687	-9.823
-2.179	Fe_tri2(H)2+4	1.593e-010	1.055e-012	-9.798	-11.977
-0.136	Fe_tri(SO4)2-	7.854e-011	5.740e-011	-10.105	-10.241
-3.405	Fe_tri3(H)4+5	9.880e-012	3.893e-015	-11.005	-14.410
0.041	Fe_triCl3	5.300e-012	5.820e-012	-11.276	-11.235
-0.545	Fe_triHSO4+2	6.254e-014	1.784e-014	-13.204	-13.749
H(0)	0.000e+000				
0.041	H2	0.000e+000	0.000e+000	-44.396	-44.355
K	5.270e-005				
-0.181	K+	5.222e-005	3.440e-005	-4.282	-4.464
-0.136	KSO4-	4.793e-007	3.503e-007	-6.319	-6.456
0.041	KOH	2.924e-014	3.211e-014	-13.534	-13.493
Mg	9.719e-004				
-0.523	Mg+2	8.364e-004	2.511e-004	-3.078	-3.600
0.041	MgSO4	7.770e-005	8.533e-005	-4.110	-4.069
-0.136	MgHCO3+	5.778e-005	4.223e-005	-4.238	-4.374
0.041	MgCO3	3.995e-008	4.388e-008	-7.398	-7.358
0.041	MgOH+	3.359e-010	2.455e-010	-9.474	-9.610
Mn(2)	3.951e-007				
-0.576	Mn+2	2.228e-007	5.917e-008	-6.652	-7.228
-0.136	MnHCO3+	1.037e-007	7.579e-008	-6.984	-7.120
-0.136	MnCl+	5.142e-008	3.758e-008	-7.289	-7.425
0.041	MnSO4	1.389e-008	1.525e-008	-7.857	-7.817
0.041	MnCl2	2.329e-009	2.557e-009	-8.633	-8.592
0.041	MnCO3	7.837e-010	8.606e-010	-9.106	-9.065
-0.136	MnCl3-	1.502e-010	1.098e-010	-9.823	-9.959
-0.136	MnOH+	5.604e-013	4.096e-013	-12.251	-12.388
Mn(3)	4.532e-017				
-1.226	Mn+3	4.532e-017	2.696e-018	-16.344	-17.569
Na	4.183e-004				
-0.146	Na+	4.132e-004	2.950e-004	-3.384	-3.530
-0.136	NaSO4-	2.933e-006	2.143e-006	-5.533	-5.669
0.041	NaHCO3	2.171e-006	2.384e-006	-5.663	-5.623
-0.136	NaCO3-	1.376e-009	1.006e-009	-8.861	-8.997
0.041	NaOH	4.780e-013	5.249e-013	-12.321	-12.280
O(0)	3.828e-004				
0.041	O2	1.914e-004	2.102e-004	-3.718	-3.677
S(-2)	0.000e+000				
0.041	H2S	0.000e+000	0.000e+000	-137.961	-137.921
-0.187	HS-	0.000e+000	0.000e+000	-139.241	-139.428
-0.635	S-2	0.000e+000	0.000e+000	-146.277	-146.912
0.041	Fe_di(HS)2	0.000e+000	0.000e+000	-274.593	-274.553
-0.136	Fe_di(HS)3-	0.000e+000	0.000e+000	-411.808	-411.944
S(6)	1.579e-002				
0.041	CaSO4	9.213e-003	1.012e-002	-2.036	-1.995
-0.651	SO4-2	6.490e-003	1.449e-003	-2.188	-2.839
0.041	MgSO4	7.770e-005	8.533e-005	-4.110	-4.069
0.041	Fe_diSO4	5.300e-006	5.820e-006	-5.276	-5.235
-0.136	NaSO4-	2.933e-006	2.143e-006	-5.533	-5.669
-0.136	HSO4-	7.097e-007	5.187e-007	-6.149	-6.285
-0.136	KSO4-	4.793e-007	3.503e-007	-6.319	-6.456
-0.136	CaHSO4+	2.985e-007	2.182e-007	-6.525	-6.661
0.041	MnSO4	1.389e-008	1.525e-008	-7.857	-7.817
-0.136	Fe_triSO4+	2.477e-009	1.810e-009	-8.606	-8.742
-0.136	Fe_diHSO4+	1.927e-010	1.408e-010	-9.715	-9.851
-0.136	Fe_tri(SO4)2-	7.854e-011	5.740e-011	-10.105	-10.241
-0.545	Fe_triHSO4+2	6.254e-014	1.784e-014	-13.204	-13.749

Saturation indices

Phase	SI	log IAP	log KT	
Anhydrite	0.07	-4.29	-4.36	CaSO4
Aragonite	0.14	-8.19	-8.34	CaCO3
Calcite	0.29	-8.19	-8.48	CaCO3
CH4(g)	-138.48	-141.34	-2.86	CH4

CO2(g)	0.55	-0.92	-1.47	CO2
Dolomite	-1.44	-18.53	-17.09	CaMg(CO3)2
Gypsum	0.28	-4.30	-4.58	CaSO4·2H2O
H2(g)	-41.21	-44.36	-3.15	H2
H2O(g)	-1.51	-0.00	1.51	H2O
H2S(g)	-136.92	-137.92	1.00	H2S
Halite	-5.92	-4.34	1.58	NaCl
Hausmannite	-8.92	52.11	61.03	Mn3O4
Manganite	-1.10	24.24	25.34	MnOOH
O2(g)	-0.79	-3.68	-2.89	O2
Pyrochroite	-11.57	3.63	15.20	Mn(OH)2
Pyrolusite	3.46	44.84	41.38	MnO2
Rhodochromite	-2.84	-13.97	-11.13	MnCO3
Sulfur	-101.60	-96.72	4.88	S

Reaction step 4.

Using solution 1.

Using pure phase assemblage 1.

Using kinetics 1.

Kinetics defined in simulation 2.

Kinetics 1. Kinetics defined in simulation 2.

Time step: 10800 seconds (Incremented time: 14400 seconds)

Coefficient	Rate name	Delta Moles	Total Moles	Reactant
-1	Fe_di_ox	-5.450e-005	9.999e-001	Fe_di
1				Fe_tri

Phase assemblage

Delta	Phase	SI	log IAP	log KT	Moles in assemblage	Initial	Final
1.363e-005	O2(g)	-0.79	-3.68	-2.89	1.000e+001	1.000e+001-	

Solution composition

Elements	Molality	Moles
C	1.389e-001	1.389e-001
Ca	1.476e-001	1.476e-001
Cl	2.367e-001	2.367e-001
Fe_di	8.109e-005	8.109e-005
Fe_tri	7.991e-005	7.991e-005
K	5.270e-005	5.270e-005
Mg	9.719e-004	9.719e-004
Mn	3.951e-007	3.951e-007
Na	4.183e-004	4.183e-004
S	1.579e-002	1.579e-002

Description of solution

equilibrium	pH =	5.433	Charge balance
	pe =	15.169	Adjusted to redox
	Activity of water =	0.991	
	Ionic strength =	4.067e-001	
	Mass of water (kg) =	1.000e+000	
	Total alkalinity (eq/kg) =	2.975e-002	
	Total CO2 (mol/kg) =	1.389e-001	
	Temperature (deg C) =	25.000	
	Electrical balance (eq) =	2.542e-014	
	Percent error, 100*(Cat-[An])/[Cat+[An]] =	0.00	
	Iterations =	34	
	Total H =	1.110421e+002	
	Total O =	5.587726e+001	

Distribution of species

Log Gamma	Species	Molality	Activity	Log Molality	Log Activity
-0.113	H+	4.778e-006	3.687e-006	-5.321	-5.433
-0.187	OH-	4.143e-009	2.691e-009	-8.383	-8.570
0.000	H2O	5.551e+001	9.911e-001	1.744	-0.004
0.041	CH4	0.000e+000	0.000e+000	-141.384	-141.343
0.041	CO2	1.093e-001	1.200e-001	-0.961	-0.921
-0.152	HCO3-	2.039e-002	1.435e-002	-1.691	-1.843
-0.152	CaHCO3+	9.101e-003	6.407e-003	-2.041	-2.193
-0.136	MgHCO3+	5.771e-005	4.218e-005	-4.239	-4.375
-0.136	Fe_diHCO3+	2.653e-005	1.939e-005	-4.576	-4.712
-0.136	CaCO3	9.770e-006	1.073e-005	-5.010	-4.969
0.041	NaHCO3	2.168e-006	2.381e-006	-5.664	-5.623
-0.610	CO3-2	7.433e-007	1.826e-007	-6.129	-6.739
-0.136	MnHCO3+	1.036e-007	7.572e-008	-6.985	-7.121
0.041	Fe_diCO3	5.387e-008	5.916e-008	-7.269	-7.228
0.041	MgCO3	3.984e-008	4.375e-008	-7.400	-7.359
-0.136	NaCO3-	1.372e-009	1.003e-009	-8.863	-8.999

0.041	MnCO3	7.816e-010	8.584e-010	-9.107	-9.066
Ca	1.476e-001				
-0.568	Ca+2	1.293e-001	3.499e-002	-0.888	-1.456
0.041	CaSO4	9.215e-003	1.012e-002	-2.036	-1.995
-0.152	CaHCO3+	9.101e-003	6.407e-003	-2.041	-2.193
0.041	CaCO3	9.770e-006	1.073e-005	-5.010	-4.969
-0.136	CaHSO4+	2.991e-007	2.186e-007	-6.524	-6.660
-0.136	CaOH+	2.136e-009	1.561e-009	-8.670	-8.807
-0.136	Cl-	2.367e-001			
-0.181	Cl-	2.367e-001	1.559e-001	-0.626	-0.807
-0.136	Fe_diCl+	3.978e-006	2.907e-006	-5.400	-5.537
-0.136	MnCl+	5.144e-008	3.759e-008	-7.289	-7.425
-0.545	Fe_triCl+2	5.929e-009	1.692e-009	-8.227	-8.772
0.041	MnCl2	2.329e-009	2.558e-009	-8.633	-8.592
-0.136	Fe_triCl2+	1.612e-009	1.178e-009	-8.793	-8.929
-0.136	MnCl3-	1.503e-010	1.098e-010	-9.823	-9.959
-0.136	Fe_triCl3	1.672e-011	1.836e-011	-10.777	-10.736
0.041	Fe_di				
-0.545	Fe_di+2	8.109e-005			
-0.136	Fe_diHCO3+	4.735e-005	1.351e-005	-4.325	-4.869
-0.136	Fe_diCl+	2.653e-005	1.939e-005	-4.576	-4.712
-0.136	Fe_diSO4	3.171e-006	3.482e-006	-5.499	-5.458
0.041	Fe_diCO3	5.387e-008	5.916e-008	-7.269	-7.228
0.041	Fe_diOH+	1.571e-009	1.148e-009	-8.804	-8.940
-0.136	Fe_diHSO4+	1.155e-010	8.440e-011	-9.937	-10.074
-0.136	Fe_di(HS)2	0.000e+000	0.000e+000	-274.815	-274.774
0.041	Fe_di(HS)3-	0.000e+000	0.000e+000	-412.028	-412.164
-0.136	Fe_tri	7.991e-005			
-0.136	Fe_tri(H)2+	7.595e-005	5.551e-005	-4.119	-4.256
-0.545	Fe_triOH+2	2.186e-006	6.236e-007	-5.660	-6.205
0.041	Fe_tri(H)3	1.750e-006	1.922e-006	-5.757	-5.716
-0.136	Fe_triSO4+	7.814e-009	5.711e-009	-8.107	-8.243
-1.226	Fe_tri+3	6.041e-009	3.593e-010	-8.219	-9.445
-0.545	Fe_triCl+2	5.929e-009	1.692e-009	-8.227	-8.772
-0.136	Fe_triCl2+	1.612e-009	1.178e-009	-8.793	-8.929
-2.179	Fe_tri2(H)2+4	1.580e-009	1.047e-011	-8.801	-10.980
-0.136	Fe_tri(H)4-	6.448e-010	4.713e-010	-9.191	-9.327
-3.405	Fe_tri3(H)4+5	3.081e-010	1.214e-013	-9.511	-12.916
-0.136	Fe_tri(SO4)2-	2.478e-010	1.811e-010	-9.606	-9.742
0.041	Fe_triCl3	1.672e-011	1.836e-011	-10.777	-10.736
-0.545	Fe_triHSO4+2	1.976e-013	5.639e-014	-12.704	-13.249
0.041	H(0)	0.000e+000			
0.041	H2	0.000e+000	0.000e+000	-44.396	-44.355
-0.181	K+	5.270e-005			
-0.136	KSO4-	4.794e-007	3.503e-007	-6.319	-6.456
0.041	KOH	2.919e-014	3.206e-014	-13.535	-13.494
-0.523	Mg	9.719e-004			
0.041	Mg+2	8.364e-004	2.511e-004	-3.078	-3.600
-0.136	MgSO4	7.772e-005	8.535e-005	-4.109	-4.069
-0.136	MgHCO3+	5.771e-005	4.218e-005	-4.239	-4.375
0.041	MgCO3	3.984e-008	4.375e-008	-7.400	-7.359
-0.136	MgOH+	3.354e-010	2.451e-010	-9.474	-9.611
-0.576	Mn(2)	3.951e-007			
-0.136	Mn+2	2.229e-007	5.919e-008	-6.652	-7.228
-0.136	MnHCO3+	1.036e-007	7.572e-008	-6.985	-7.121
-0.136	MnCl+	5.144e-008	3.759e-008	-7.289	-7.425
0.041	MnSO4	1.390e-008	1.526e-008	-7.857	-7.816
0.041	MnCl2	2.329e-009	2.558e-009	-8.633	-8.592
0.041	MnCO3	7.816e-010	8.584e-010	-9.107	-9.066
-0.136	MnCl3-	1.503e-010	1.098e-010	-9.823	-9.959
-0.136	MnOH+	5.596e-013	4.090e-013	-12.252	-12.388
-1.226	Mn(3)	4.541e-017			
-1.226	Mn+3	4.541e-017	2.701e-018	-16.343	-17.568

Na	4.183e-004				
-0.146	Na+	4.132e-004	2.951e-004	-3.384	-3.530
-0.136	NaSO4-	2.933e-006	2.144e-006	-5.533	-5.669
0.041	NaHCO3	2.168e-006	2.381e-006	-5.664	-5.623
-0.136	NaCO3-	1.372e-009	1.003e-009	-8.863	-8.999
0.041	NaOH	4.772e-013	5.240e-013	-12.321	-12.281
0(0)	O2	3.828e-004			
0.041	O2	1.914e-004	2.102e-004	-3.718	-3.677
0.041	S(-2)	0.000e+000			
0.041	H2S	0.000e+000	0.000e+000	-137.960	-137.919
-0.187	HS-	0.000e+000	0.000e+000	-139.240	-139.427
-0.635	S-2	0.000e+000	0.000e+000	-146.277	-146.912
0.041	Fe_di(HS)2	0.000e+000	0.000e+000	-274.815	-274.774
-0.136	Fe_di(HS)3-	0.000e+000	0.000e+000	-412.028	-412.164
0.041	CaSO4	1.579e-002			
0.041	SO4-2	9.215e-003	1.012e-002	-2.036	-1.995
-0.651	MgSO4	6.490e-003	1.450e-003	-2.188	-2.839
0.041	Fe_diSO4	7.772e-005	8.535e-005	-4.109	-4.069
0.041	Fe_diSO4	3.171e-006	3.482e-006	-5.499	-5.458
-0.136	NaSO4-	2.933e-006	2.144e-006	-5.533	-5.669
-0.136	HSD4-	7.110e-007	5.196e-007	-6.148	-6.284
-0.136	KSD4-	4.794e-007	3.503e-007	-6.319	-6.456
-0.136	CaHSO4+	2.991e-007	2.186e-007	-6.524	-6.660
0.041	MnSO4	1.390e-008	1.526e-008	-7.857	-7.816
-0.136	Fe_triSO4+	7.814e-009	5.711e-009	-8.107	-8.243
-0.136	Fe_tri(SO4)2-	2.478e-010	1.811e-010	-9.606	-9.742
-0.136	Fe_diHSO4+	1.155e-010	8.440e-011	-9.937	-10.074
-0.545	Fe_triHSO4+2	1.976e-013	5.639e-014	-12.704	-13.249

Saturation indices

Phase	SI	log IAP	log KI	
Anhydrite	0.07	-4.29	-4.36	CaSO4
Aragonite	0.14	-8.19	-8.34	CaCO3
Calcite	0.29	-8.19	-8.48	CaCO3
CH4(g)	-138.48	-141.34	-2.86	CH4
CO2(g)	0.55	-0.92	-1.47	CO2
Dolomite	-1.44	-18.53	-17.09	CaMg(CO3)2
Gypsum	0.28	-4.30	-4.58	CaSO4.2H2O
H2(g)	-41.21	-44.36	-3.15	H2
H2O(g)	-1.51	-0.00	1.51	H2O
H2S(g)	-136.92	-137.92	-1.00	H2S
Halite	-5.92	-4.34	1.58	NaCl
Hauserite	-8.92	52.11	61.03	Mn3O4
Manganite	-1.11	24.23	25.34	MnOOH
O2(g)	-0.79	-3.68	-2.89	O2
Pyrochroite	-11.57	3.63	15.20	Mn(CH)2
Pyrolusite	3.46	44.84	41.38	MnO2
Rhodochrosite	-2.84	-13.97	-11.13	MnCO3
Sulfur	-101.60	-96.71	4.88	S

Reaction step 5.

Using solution 1.  
Using pure phase assemblage 1.  
Using kinetics 1. Kinetics defined in simulation 2.

Kinetics 1. Kinetics defined in simulation 2.

Time step: 21600 seconds (Incremented time: 36000 seconds)

Coefficient	Rate name	Delta Moles	Total Moles	Reactant
-1	Fe_di_ox	-5.198e-005	9.999e-001	Fe_di
1				Fe_tri

Phase assemblage

Delta	Phase	SI	log IAP	log KI	Moles in assemblage	
					Initial	Final
1.300e-005	O2(g)	-0.78	-3.68	-2.89	1.000e+001	1.000e+001-

Solution composition

Elements	Molality	Moles
C	1.389e-001	1.389e-001
Ca	1.476e-001	1.476e-001
Cl	2.367e-001	2.367e-001
Fe_di	2.911e-005	2.911e-005
Fe_tri	1.319e-004	1.319e-004
K	5.270e-005	5.270e-005
Mg	9.719e-004	9.719e-004
Mn	3.951e-007	3.951e-007
Na	4.183e-004	4.183e-004

S 1.579e-002 1.579e-002

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Description of solution  
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pH = 5.433 Charge balance  
pe = 15.170 Adjusted to redox

equilibrium

Activity of water = 0.991  
Ionic strength = 4.067e-001  
Mass of water (kg) = 1.000e+000  
Total alkalinity (eq/kg) = 2.980e-002  
Total CO2 (mol/kg) = 1.389e-001  
Temperature (deg C) = 25.000  
Electrical balance (eq) = 2.537e-014  
Percent error, 100\*(Cat-|An|)/(Cat+|An|) = 0.00  
Iterations = 85  
Total H = 1.110421e+002  
Total O = 5.587729e+001

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Distribution of species  
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Log Gamma	Species	Molality	Activity	Log Molality	Log Activity
	H+	4.786e-006	3.693e-006	-5.320	-5.433
-0.113	OH-	4.137e-009	2.687e-009	-8.383	-8.571
-0.187	H2O	5.551e+001	9.911e-001	1.744	-0.004
0.000	0.000e+000				
C(-4)	CH4	0.000e+000	0.000e+000	-141.384	-141.343
0.041	1.389e-001				
C(4)	CO2	1.094e-001	1.201e-001	-0.961	-0.920
0.041	HCO3-	2.036e-002	1.434e-002	-1.691	-1.844
-0.152	CaHCO3+	9.090e-003	6.399e-003	-2.041	-2.194
-0.152	MgHCO3+	5.765e-005	4.213e-005	-4.239	-4.375
-0.136	CaCO3	9.743e-006	1.070e-005	-5.011	-4.971
0.041	Fe_dihCO3+	9.515e-006	6.954e-006	-5.022	-5.158
-0.136	NaHCO3	2.166e-006	2.379e-006	-5.664	-5.624
0.041	CO3-2	7.412e-007	1.820e-007	-6.130	-6.740
-0.610	MnHCO3+	1.035e-007	7.565e-008	-6.985	-7.121
-0.136	MgCO3	3.973e-008	4.363e-008	-7.401	-7.360
0.041	Fe_dihCO3	1.929e-008	2.118e-008	-7.715	-7.674
0.041	NaCO3-	1.369e-009	1.000e-009	-8.864	-9.000
-0.136	MnCO3	7.797e-010	8.562e-010	-9.108	-9.067
0.041	Ca	1.476e-001			
Ca+2	Ca+2	1.293e-001	3.499e-002	-0.888	-1.456
-0.568	CaSO4	9.216e-003	1.012e-002	-2.035	-1.995
0.041	CaHCO3+	9.090e-003	6.399e-003	-2.041	-2.194
-0.152	CaCO3	9.743e-006	1.070e-005	-5.011	-4.971
0.041	CaHSO4+	2.996e-007	2.190e-007	-6.523	-6.660
-0.136	CaOH+	2.132e-009	1.558e-009	-8.671	-8.807
-0.136	Cl	2.367e-001			
Cl-	Cl-	2.367e-001	1.559e-001	-0.626	-0.807
-0.181	Fe_dihCl+	1.428e-006	1.044e-006	-5.845	-5.981
-0.136	MnCl+	5.146e-008	3.761e-008	-7.289	-7.425
-0.136	Fe_triCl+2	9.818e-009	2.801e-009	-8.008	-8.553
-0.545	Fe_triCl2+	2.669e-009	1.950e-009	-8.574	-8.710
-0.136	MnCl2	2.330e-009	2.559e-009	-8.633	-8.592
0.041	MnCl3-	1.504e-010	1.099e-010	-9.823	-9.959
-0.136	Fe_triCl3	2.769e-011	3.041e-011	-10.558	-10.517
0.041	Fe_di	2.911e-005			
Fe_di+2	Fe_di+2	1.700e-005	4.851e-006	-4.769	-5.314
-0.545	Fe_dihCO3+	9.515e-006	6.954e-006	-5.022	-5.158
-0.136	Fe_dihCl+	1.428e-006	1.044e-006	-5.845	-5.981
-0.136	Fe_dihSO4	1.139e-006	1.251e-006	-5.944	-5.903
0.041	Fe_dihCO3	1.929e-008	2.118e-008	-7.715	-7.674
0.041	Fe_dihOH+	5.633e-010	4.117e-010	-9.249	-9.385
-0.136	Fe_dihSO4+	4.154e-011	3.036e-011	-10.382	-10.518
-0.136	Fe_di(HS)2	0.000e+000	0.000e+000	-275.258	-275.217
0.041	Fe_di(HS)3-	0.000e+000	0.000e+000	-412.471	-412.607
-0.136	Fe_tri	1.319e-004			
Fe_tri(H)2+	Fe_tri(H)2+	1.253e-004	9.161e-005	-3.902	-4.038
-0.136	Fe_triOH+2	3.614e-006	1.031e-006	-5.442	-5.987
-0.545					

0.041	Fe_tri(H)3	2.884e-006	3.167e-006	-5.540	-5.499
-0.136	Fe_triSO4+	1.294e-008	9.457e-009	-7.888	-8.024
-1.226	Fe_tri+3	1.000e-008	5.949e-010	-8.000	-9.226
-0.545	Fe_triCl+2	9.818e-009	2.801e-009	-8.008	-8.553
-2.179	Fe_tri2(H)2+4	4.318e-009	2.860e-011	-8.365	-10.544
-0.136	Fe_triCl2+	2.669e-009	1.950e-009	-8.574	-8.710
-3.405	Fe_tri3(H)4+5	1.390e-009	5.474e-013	-8.857	-12.262
-0.136	Fe_tri(H)4-	1.061e-009	7.752e-010	-8.974	-9.111
-0.136	Fe_tri(SO4)2-	4.104e-010	3.000e-010	-9.387	-9.523
0.041	Fe_triCl3	2.769e-011	3.041e-011	-10.558	-10.517
-0.545	Fe_triHSO4+2	3.278e-013	9.353e-014	-12.484	-13.029
0.000	H(0)	0.000e+000	0.000e+000		
0.041	K	5.270e-005			
K+	K+	5.222e-005	3.440e-005	-4.282	-4.463
-0.181	KSO4-	4.794e-007	3.504e-007	-6.319	-6.455
-0.136	KOH	2.915e-014	3.201e-014	-13.535	-13.495
0.041	Mg	9.719e-004			
Mg+2	Mg+2	8.365e-004	2.512e-004	-3.078	-3.600
-0.522	MgSO4	7.773e-005	8.536e-005	-4.109	-4.069
0.041	MgHCO3+	5.765e-005	4.213e-005	-4.239	-4.375
-0.136	MgCO3	3.973e-008	4.363e-008	-7.401	-7.360
0.041	MgOH+	3.349e-010	2.447e-010	-9.475	-9.611
-0.136	Mn(2)	3.951e-007			
Mn+2	Mn+2	2.230e-007	5.921e-008	-6.652	-7.228
-0.576	MnHCO3+	1.035e-007	7.565e-008	-6.985	-7.121
-0.136	MnCl+	5.146e-008	3.761e-008	-7.289	-7.425
-0.136	MnSO4	1.390e-008	1.527e-008	-7.857	-7.816
0.041	MnCl2	2.330e-009	2.559e-009	-8.633	-8.592
0.041	MnCO3	7.797e-010	8.562e-010	-9.108	-9.067
0.041	MnCl3-	1.504e-010	1.099e-010	-9.823	-9.959
-0.136	MnOH+	5.589e-013	4.085e-013	-12.253	-12.389
-0.136	Mn(3)	4.550e-017			
Mn+3	Mn+3	4.550e-017	2.707e-018	-16.342	-17.568
-1.226	Na	4.183e-004			
Na+	Na+	4.132e-004	2.951e-004	-3.384	-3.530
-0.146	NaSO4-	2.933e-006	2.144e-006	-5.533	-5.669
-0.136	NaHCO3	2.166e-006	2.379e-006	-5.664	-5.624
0.041	NaCO3-	1.369e-009	1.000e-009	-8.864	-9.000
-0.136	NaOH	4.764e-013	5.232e-013	-12.322	-12.281
0.041	O(0)	3.828e-004			
O2	O2	1.914e-004	2.102e-004	-3.718	-3.677
0.041	S(-2)	0.000e+000	0.000e+000		
H2S	H2S	0.000e+000	0.000e+000	-137.958	-137.918
0.041	HS-	0.000e+000	0.000e+000	-139.239	-139.427
-0.187	S-2	0.000e+000	0.000e+000	-146.277	-146.912
-0.635	Fe_di(HS)2	0.000e+000	0.000e+000	-275.258	-275.217
0.041	Fe_di(HS)3-	0.000e+000	0.000e+000	-412.471	-412.607
-0.136	S(6)	1.579e-002			
CaSO4	CaSO4	9.216e-003	1.012e-002	-2.035	-1.995
0.041	SO4-2	6.490e-003	1.450e-003	-2.188	-2.839
-0.651	MgSO4	7.773e-005	8.536e-005	-4.109	-4.069
0.041	NaSO4-	2.933e-006	2.144e-006	-5.533	-5.669
-0.136	Fe_dihSO4	1.139e-006	1.251e-006	-5.944	-5.903
0.041	HSO4-	7.123e-007	5.206e-007	-6.147	-6.284
-0.136	KSO4-	4.794e-007	3.504e-007	-6.319	-6.455
-0.136	CaHSO4+	2.996e-007	2.190e-007	-6.523	-6.660
-0.136	MnSO4	1.390e-008	1.527e-008	-7.857	-7.816
0.041	Fe_triSO4+	1.294e-008	9.457e-009	-7.888	-8.024
-0.136	Fe_tri(SO4)2-	4.104e-010	3.000e-010	-9.387	-9.523
-0.136	Fe_dihSO4+	4.154e-011	3.036e-011	-10.382	-10.518
-0.545	Fe_triHSO4+2	3.278e-013	9.353e-014	-12.484	-13.029

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Saturation indices  
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Phase	SI	log IAP	log KT	
Anhydrite	0.07	-4.29	-4.36	CaSO4
Aragonite	0.14	-8.20	-8.34	CaCO3
Calcite	0.28	-8.20	-8.48	CaCO3
CH4(g)	-138.48	-141.34	-2.86	CH4
CO2(g)	0.55	-0.92	-1.47	CO2
Dolomite	-1.45	-18.54	-17.09	CaMg(CO3)2
Gypsum	0.28	-4.30	-4.58	CaSO4·2H2O
H2O(g)	-41.21	-44.36	-3.15	H2
H2O(l)	-1.51	-0.00	1.51	H2O
H2S(g)	-136.92	-137.92	-1.00	H2S
Halite	-5.92	-4.34	1.58	NaCl
Hausmannite	-8.93	52.10	61.03	Mn3O4
Manganite	-1.11	24.23	25.34	MnOOH
O2(g)	-0.78	-3.68	-2.89	O2
Pyrochroite	-11.57	3.63	15.20	Mn(CH)2
Pyrochroite	3.46	44.84	41.38	MnO2
Rhodochrosite	-2.84	-13.97	-11.13	MnCO3
Sulfur	-101.59	-96.71	4.88	S

Reaction step 6.

WARNING: Element Fe\_di has negative moles in solution, -4.123295e-006.  
Erroneous mole balance occurs as moles are added to produce zero moles.

Usually caused by KINETICS, REACTION, or diffuse layer calculation.

May be due to large time steps in early part of KINETICS simulation or negative concentrations in the diffuse layer.

Using solution 1.

Using pure phase assemblage 1.

Using kinetics 1. Kinetics defined in simulation 2.

Kinetics 1. Kinetics defined in simulation 2.

Time step: 50400 seconds (Incremented time: 86400 seconds)

Coefficient	Rate name	Delta Moles	Total Moles	Reactant
-1	Fe_di_ox	-2.642e-005	9.998e-001	Fe_di
1				Fe_tri

Phase assemblage				
Delta	Phase	Moles in assemblage		
		SI	log IAP	log KT
6.607e-006	O2(g)	-0.78	-3.68	-2.89

Solution composition			
Elements	Molality	Moles	
C	1.389e-001	1.389e-001	
Ca	1.476e-001	1.476e-001	
Cl	2.367e-001	2.367e-001	
Fe_di	2.681e-006	2.681e-006	
Fe_tri	1.583e-004	1.583e-004	
K	5.270e-005	5.270e-005	
Mg	9.719e-004	9.719e-004	
Mn	3.951e-007	3.951e-007	
Na	4.183e-004	4.183e-004	
S	1.579e-002	1.579e-002	

Description of solution			
	pH =	5.432	Charge balance
	pe =	15.170	Adjusted to redox
equilibrium	Activity of water =	0.991	
	Tonic strength =	4.065e-001	
	Mass of water (kg) =	1.000e+000	
	Total alkalinity (eq/kg) =	2.983e-002	
	Total CO2 (mol/kg) =	1.389e-001	
	Temperature (deg C) =	25.000	
	Electrical balance (eq) =	1.721e-013	
Percent error, 100*(Cat- An )/(Cat+ An )	=	0.00	
	Iterations =	85	
	Total H =	1.110421e+002	
	Total O =	5.587730e+001	

Distribution of species					
Log	Species	Molality	Activity	Log	Log
Gamma					
-0.113	H+	4.790e-006	3.696e-006	-5.320	-5.432
-0.187	OH-	4.133e-009	2.684e-009	-8.384	-8.571
0.000	H2O	5.551e+001	9.911e-001	1.744	-0.004
C(-4)	0.000e+000				
0.041	CH4	0.000e+000	0.000e+000	-141.384	-141.343
C(4)	1.389e-001				
0.041	CO2	1.094e-001	1.201e-001	-0.961	-0.920
-0.152	HCO3-	2.035e-002	1.433e-002	-1.691	-1.844
-0.152	CaHCO3+	9.085e-003	6.396e-003	-2.042	-2.194
-0.136	MgHCO3+	5.761e-005	4.211e-005	-4.239	-4.376
0.041	CaCO3	9.730e-006	1.068e-005	-5.012	-4.971

0.041	NaHCO3	2.165e-006	2.377e-006	-5.665	-5.624
-0.136	Fe_diHCO3+	8.762e-007	6.403e-007	-6.057	-6.194
-0.610	CO3-2	7.401e-007	1.818e-007	-6.131	-6.740
-0.136	MnHCO3+	1.035e-007	7.562e-008	-6.985	-7.121
0.041	MgCO3	3.967e-008	4.357e-008	-7.401	-7.361
0.041	Fe_diCO3	1.775e-009	1.949e-009	-8.751	-8.710
0.041	NaCO3-	1.367e-009	9.987e-010	-8.864	-9.001
-0.136	MnCO3	7.787e-010	8.551e-010	-9.109	-9.068
0.041	Ca	1.476e-001			
-0.568	Ca+2	1.293e-001	3.499e-002	-0.888	-1.456
0.041	CaSO4	9.217e-003	1.012e-002	-2.035	-1.995
0.041	CaHCO3+	9.085e-003	6.396e-003	-2.042	-2.194
-0.152	CaCO3	9.730e-006	1.068e-005	-5.012	-4.971
0.041	CaHSO4+	2.999e-007	2.192e-007	-6.523	-6.659
-0.136	CaOH+	2.131e-009	1.557e-009	-8.672	-8.808
-0.136	Cl-	2.367e-001	1.559e-001	-0.626	-0.807
-0.181	Fe_diCl+	1.316e-007	9.618e-008	-6.881	-7.017
-0.136	MnCl+	5.147e-008	3.761e-008	-7.288	-7.425
-0.136	Fe_triCl+2	1.180e-008	3.368e-009	-7.928	-8.473
-0.545	Fe_triCl2+	3.209e-009	2.345e-009	-8.494	-8.630
-0.136	MnCl2	2.331e-009	2.560e-009	-8.632	-8.592
-0.136	MnCl3-	1.504e-010	1.099e-010	-9.823	-9.959
0.041	Fe_triCl3	3.329e-011	3.656e-011	-10.478	-10.437
0.041	Fe_di	2.681e-006			
-0.545	Fe_di+2	1.567e-006	4.470e-007	-5.805	-6.350
-0.136	Fe_diHCO3+	8.762e-007	6.403e-007	-6.057	-6.194
-0.136	Fe_diCl+	1.316e-007	9.618e-008	-6.881	-7.017
0.041	Fe_diSO4	1.049e-007	1.152e-007	-6.979	-6.938
0.041	Fe_diCO3	1.775e-009	1.949e-009	-8.751	-8.710
-0.136	Fe_diOH+	5.186e-011	3.790e-011	-10.285	-10.421
-0.136	Fe_diHSO4+	3.831e-012	2.800e-012	-11.417	-11.553
-0.136	Fe_di(HS)2	0.000e+000	0.000e+000	-276.293	-276.252
0.041	Fe_di(HS)3-	0.000e+000	0.000e+000	-413.505	-413.641
-0.136	Fe_tri	1.583e-004			
-0.136	Fe_tri(H)2+	1.505e-004	1.100e-004	-3.823	-3.959
-0.136	Fe_triOH+2	4.341e-006	1.238e-006	-5.362	-5.907
-0.545	Fe_tri(H)3	3.459e-006	3.798e-006	-5.461	-5.420
0.041	Fe_triSO4+	1.556e-008	1.137e-008	-7.808	-7.944
-0.136	Fe_tri+3	1.203e-008	7.153e-010	-7.920	-9.146
-1.226	Fe_triCl+2	1.180e-008	3.368e-009	-7.928	-8.473
-0.545	Fe_tri2(H)2+4	6.232e-009	4.128e-011	-8.205	-10.384
-2.179	Fe_triCl2+	3.209e-009	2.345e-009	-8.494	-8.630
-0.136	Fe_tri3(H)4+5	2.407e-009	9.483e-013	-8.619	-12.023
-3.405	Fe_tri(H)4-	1.271e-009	9.289e-010	-8.896	-9.032
-0.136	Fe_tri(SO4)2-	4.935e-010	3.607e-010	-9.307	-9.443
0.041	Fe_triCl3	3.329e-011	3.656e-011	-10.478	-10.437
-0.545	Fe_triHSO4+2	3.945e-013	1.125e-013	-12.404	-12.949
-0.545	H(0)	0.000e+000			
0.041	H2	0.000e+000	0.000e+000	-44.396	-44.355
0.041	K	5.270e-005			
-0.181	K+	5.222e-005	3.440e-005	-4.282	-4.463
-0.136	KSO4-	4.794e-007	3.504e-007	-6.319	-6.455
0.041	KOH	2.912e-014	3.198e-014	-13.536	-13.495
0.041	Mg	9.719e-004			
-0.522	Mg+2	8.365e-004	2.512e-004	-3.078	-3.600
0.041	MgSO4	7.774e-005	8.537e-005	-4.109	-4.069
-0.136	MgHCO3+	5.761e-005	4.211e-005	-4.239	-4.376
0.041	MgCO3	3.967e-008	4.357e-008	-7.401	-7.361
-0.136	MgOH+	3.346e-010	2.445e-010	-9.475	-9.612
-0.576	Mn(2)	3.951e-007			
-0.136	Mn+2	2.230e-007	5.922e-008	-6.652	-7.228
-0.136	MnHCO3+	1.035e-007	7.562e-008	-6.985	-7.121



-0.136	MnCl+	5.147e-008	3.761e-008	-7.288	-7.425
0.041	MnSO4	1.390e-008	1.527e-008	-7.857	-7.816
0.041	MnCl2	2.331e-009	2.560e-009	-8.632	-8.592
0.041	MnCO3	7.787e-010	8.551e-010	-9.109	-9.068
0.041	MnCl3-	1.504e-010	1.099e-010	-9.823	-9.959
-0.136	MnOH+	5.585e-013	4.082e-013	-12.253	-12.389
-0.136	Mn(3)	4.555e-017			
-1.226	Mn+3	4.555e-017	2.709e-018	-16.342	-17.567
-0.146	Na+	4.183e-004			
-0.146	NaSO4-	4.132e-004	2.951e-004	-3.384	-3.530
-0.136	NaSO4-	2.934e-006	2.144e-006	-5.533	-5.669
0.041	NaHCO3	2.165e-006	2.377e-006	-5.665	-5.624
-0.136	NaCO3-	1.367e-009	9.987e-010	-8.864	-9.001
0.041	NaOH	4.760e-013	5.227e-013	-12.322	-12.282
0.041	O(0)	3.828e-004			
0.041	O2	1.914e-004	2.102e-004	-3.718	-3.677
0.041	S(-2)	0.000e+000			
0.041	H2S	0.000e+000	0.000e+000	-137.957	-137.917
-0.187	HS-	0.000e+000	0.000e+000	-139.239	-139.426
-0.635	S-2	0.000e+000	0.000e+000	-146.277	-146.912
0.041	Fe_di(HS)2	0.000e+000	0.000e+000	-276.293	-276.252
-0.136	Fe_di(HS)3-	0.000e+000	0.000e+000	-413.505	-413.641
0.041	S(6)	1.579e-002			
0.041	CaSO4	9.217e-003	1.012e-002	-2.035	-1.995
-0.651	SO4-2	6.491e-003	1.450e-003	-2.188	-2.839
0.041	MgSO4	7.774e-005	8.537e-005	-4.109	-4.069
-0.136	NaSO4-	2.934e-006	2.144e-006	-5.533	-5.669
-0.136	HSO4-	7.129e-007	5.210e-007	-6.147	-6.283
-0.136	FSO4-	4.794e-007	3.504e-007	-6.319	-6.455
-0.136	CaHSO4+	2.999e-007	2.192e-007	-6.523	-6.659
0.041	Fe_diSO4	1.049e-007	1.152e-007	-6.979	-6.938
-0.136	Fe_triSO4+	1.556e-008	1.137e-008	-7.808	-7.944
0.041	MnSO4	1.390e-008	1.527e-008	-7.857	-7.816
-0.136	Fe_tri(SO4)2-	4.935e-010	3.607e-010	-9.307	-9.443
-0.136	Fe_dihSO4+	3.831e-012	2.800e-012	-11.417	-11.553
-0.136	Fe_trihSO4+2	3.945e-013	1.125e-013	-12.404	-12.949
-0.545					

Saturation indices

Phase	SI	log IAP	log KT	
Anhydrite	0.07	-4.29	-4.36	CaSO4
Aragonite	0.14	-8.20	-8.34	CaCO3
Calcite	0.28	-8.20	-8.48	CaCO3
CH4(g)	-138.48	-141.34	-2.86	CH4
CO2(g)	0.55	-0.92	-1.47	CO2
Dolomite	-1.45	-18.54	-17.09	CaMg(CO3)2
Gypsum	0.28	-4.30	-4.58	CaSO4·2H2O
H2(g)	-41.21	-44.36	-3.15	H2
H2O(g)	-1.51	-0.00	1.51	H2O
H2S(g)	-136.92	-137.92	-1.00	H2S
Halite	-5.92	-4.34	1.58	NaCl
Hausmannite	-8.93	52.10	61.03	Mn3O4
Manganite	-1.11	24.23	25.34	MnOOH
O2(g)	-0.78	-3.68	-2.89	O2
Pyrochroite	-11.57	3.63	15.20	Mn(OH)2
Pyrolusite	3.45	44.83	41.38	MnO2
Rhodochrosite	-2.84	-13.97	-11.13	MnCO3
Sulfur	-101.59	-96.71	4.88	S

Reaction step 7.

WARNING: Element Fe\_di has negative moles in solution, -5.710494e-006. Erroneous mole balance occurs as moles are added to produce zero moles.

Usually caused by KINETICS, REACTION, or diffuse layer calculation.

May be due to large time steps in early part of KINETICS simulation or negative concentrations in the diffuse layer.

Using solution 1. Kinetics defined in simulation 2.

Using pure phase assemblage 1. Kinetics defined in simulation 1.

Kinetics 1. Kinetics defined in simulation 2. Time step: 86400 seconds (Incremented time: 172800 seconds)

Coefficient	Rate name	Delta Moles	Total Moles	Reactant
-1	Fe_di_ox	-2.636e-006	9.998e-001	Fe_di
1				Fe_tri

Phase assemblage

Delta	Phase	Moles in assemblage			
		SI	log IAP	log KT	Initial Final
6.591e-007	O2(g)	-0.79	-3.68	-2.89	1.000e+001 1.000e+001-

Solution composition

Elements	Molality	Moles
C	1.389e-001	1.389e-001
Ca	1.476e-001	1.476e-001
Cl	2.367e-001	2.367e-001
Fe_di	4.531e-008	4.531e-008
Fe_tri	1.610e-004	1.610e-004
K	5.270e-005	5.270e-005
Mg	9.719e-004	9.719e-004
Mn	3.951e-007	3.951e-007
Na	4.183e-004	4.183e-004
S	1.579e-002	1.579e-002

Description of solution

equilibrium	pH	= 5.432	Charge balance
	pe	= 15.170	Adjusted to redox
	Activity of water	= 0.991	
	Ionic strength	= 4.066e-001	
	Mass of water (kg)	= 1.000e+000	
	Total alkalinity (eq/kg)	= 2.983e-002	
	Total CO2 (mol/kg)	= 1.389e-001	
	Temperature (deg C)	= 25.000	
	Electrical balance (eq)	= 3.342e-013	
	Percent error, 100*(Cat- An )/(Cat+ An )	= 0.00	
	Iterations	= 92	
	Total H	= 1.110421e+002	
	Total O	= 5.587731e+001	

Distribution of species

Log Gamma	Species	Molality	Activity	Log Molality	Log Activity
	H+	4.791e-006	3.697e-006	-5.320	-5.432
-0.113	OH-	4.133e-009	2.684e-009	-8.384	-8.571
-0.187	H2O	5.551e+001	9.911e-001	1.744	-0.004
0.000	0.000e+000				
C(-4)	CH4	0.000e+000	0.000e+000	-141.384	-141.343
0.041	C(4)	1.389e-001			
0.041	CO2	1.094e-001	1.201e-001	-0.961	-0.920
-0.152	HCO3-	2.035e-002	1.433e-002	-1.691	-1.844
-0.152	CaHCO3+	9.085e-003	6.396e-003	-2.042	-2.194
-0.136	MgHCO3+	5.761e-005	4.210e-005	-4.239	-4.376
0.041	CaCO3	9.729e-006	1.068e-005	-5.012	-4.971
0.041	NaHCO3	2.165e-006	2.377e-006	-5.665	-5.624
-0.610	CO3-2	7.400e-007	1.818e-007	-6.131	-6.741
-0.136	MnHCO3+	1.035e-007	7.562e-008	-6.985	-7.121
-0.136	MgCO3	3.967e-008	4.356e-008	-7.402	-7.361
0.041	Fe_diHCO3+	1.481e-008	1.082e-008	-7.830	-7.966
-0.136	NaCO3-	1.366e-009	9.986e-010	-8.864	-9.001
-0.136	MnCO3	7.786e-010	8.550e-010	-9.109	-9.068
0.041	Ca	1.476e-001			
-0.568	Ca+2	1.293e-001	3.499e-002	-0.888	-1.456
0.041	CaSO4	9.217e-003	1.012e-002	-2.035	-1.995
-0.152	CaHCO3+	9.085e-003	6.396e-003	-2.042	-2.194
-0.136	CaCO3	9.729e-006	1.068e-005	-5.012	-4.971
-0.136	CaHSO4+	2.999e-007	2.192e-007	-6.523	-6.659
-0.136	CaOH+	2.130e-009	1.557e-009	-8.672	-8.808
-0.181	Cl-	2.367e-001	1.559e-001	-0.626	-0.807
-0.136	MnCl+	5.147e-008	3.761e-008	-7.288	-7.425
-0.545	Fe_triCl+2	1.200e-008	3.424e-009	-7.921	-8.465
-0.136	Fe_triCl2+	3.263e-009	2.385e-009	-8.486	-8.623
0.041	MnCl2	2.331e-009	2.560e-009	-8.632	-8.592
-0.136	Fe_diCl+	2.224e-009	1.625e-009	-8.653	-8.789
-0.136	MnCl3-	1.504e-010	1.099e-010	-9.823	-9.959
0.041	Fe_triCl3	3.385e-011	3.718e-011	-10.470	-10.430
-0.545	Fe_di	4.531e-008			
	Fe_di+2	2.648e-008	7.553e-009	-7.577	-8.122

-0.136	Fe_diHCO3+	1.481e-008	1.082e-008	-7.830	-7.966
-0.136	Fe_diCl+	2.224e-009	1.625e-009	-8.653	-8.789
0.041	Fe_diSO4	1.773e-009	1.947e-009	-8.751	-8.711
0.041	Fe_diCO3	2.999e-011	3.293e-011	-10.523	-10.482
-0.136	Fe_diOH+	8.763e-013	6.404e-013	-12.057	-12.194
-0.136	Fe_diHSO4+	6.474e-014	4.732e-014	-13.189	-13.325
-0.136	Fe_di(HS)2	0.000e+000	0.000e+000	-278.065	-278.024
0.041	Fe_di(HS)3-	0.000e+000	0.000e+000	-415.277	-415.413
-0.136	Fe_tri	1.610e-004			
-0.136	Fe_tri(CH)2+	1.530e-004	1.118e-004	-3.815	-3.952
-0.545	Fe_triOH+	4.414e-006	1.259e-006	-5.355	-5.900
-0.545	Fe_tri(H)3	3.516e-006	3.861e-006	-5.454	-5.413
0.041	Fe_triSO4+	1.582e-008	1.156e-008	-7.801	-7.937
-0.136	Fe_tri+3	1.223e-008	7.273e-010	-7.913	-9.138
-1.226	Fe_triCl+2	1.200e-008	3.424e-009	-7.921	-8.465
-0.545	Fe_tri2(CH)2+4	6.442e-009	4.267e-011	-8.191	-10.370
-2.179	Fe_triCl2+	3.263e-009	2.385e-009	-8.486	-8.623
-0.136	Fe_tri3(CH)4+5	2.530e-009	9.966e-013	-8.597	-12.001
-3.405	Fe_tri(CH)4-	1.292e-009	9.442e-010	-8.889	-9.025
-0.136	Fe_tri(SO4)2-	5.018e-010	3.667e-010	-9.299	-9.436
-0.136	Fe_triCl3	3.385e-011	3.718e-011	-10.470	-10.430
0.041	Fe_triHSO4+2	4.012e-013	1.145e-013	-12.397	-12.941
-0.545	H(0)	0.000e+000			
0.041	H2	0.000e+000	0.000e+000	-44.396	-44.355
0.041	K	5.270e-005			
-0.181	K+	5.222e-005	3.440e-005	-4.282	-4.463
-0.136	KSO4-	4.794e-007	3.504e-007	-6.319	-6.455
0.041	KOH	2.912e-014	3.198e-014	-13.536	-13.495
0.041	Mg	9.719e-004			
-0.522	Mg+2	8.365e-004	2.512e-004	-3.078	-3.600
0.041	MgSO4	7.774e-005	8.537e-005	-4.109	-4.069
-0.136	MgHCO3+	5.761e-005	4.210e-005	-4.239	-4.376
0.041	MgCO3	3.967e-008	4.356e-008	-7.402	-7.361
-0.136	MgOH+	3.346e-010	2.445e-010	-9.476	-9.612
0.041	Mn(2)	3.951e-007			
-0.576	Mn+2	2.230e-007	5.922e-008	-6.652	-7.228
-0.136	MnHCO3+	1.035e-007	7.562e-008	-6.985	-7.121
-0.136	MnCl+	5.147e-008	3.761e-008	-7.288	-7.425
0.041	MnSO4	1.390e-008	1.527e-008	-7.857	-7.816
0.041	MnCl2	2.331e-009	2.560e-009	-8.632	-8.592
0.041	MnCO3	7.786e-010	8.550e-010	-9.109	-9.068
-0.136	MnCl3-	1.504e-010	1.099e-010	-9.823	-9.959
-0.136	MnOH+	5.585e-013	4.082e-013	-12.253	-12.389
-1.226	Mn(3)	4.555e-017			
-1.226	Mn+3	4.555e-017	2.710e-018	-16.341	-17.567
0.041	Na	4.183e-004			
-0.146	Na+	4.132e-004	2.951e-004	-3.384	-3.530
-0.136	NaSO4-	2.934e-006	2.144e-006	-5.533	-5.669
0.041	NaHCO3	2.165e-006	2.377e-006	-5.665	-5.624
-0.136	NaCO3-	1.366e-009	9.986e-010	-8.864	-9.001
0.041	NaOH	4.760e-013	5.227e-013	-12.322	-12.282
0.041	O(0)	3.828e-004			
0.041	O2	1.914e-004	2.102e-004	-3.718	-3.677
0.041	S(-2)	0.000e+000			
0.041	H2S	0.000e+000	0.000e+000	-137.957	-137.917
-0.187	HS-	0.000e+000	0.000e+000	-139.239	-139.426
-0.635	S-2	0.000e+000	0.000e+000	-146.277	-146.912
0.041	Fe_di(HS)2	0.000e+000	0.000e+000	-278.065	-278.024
-0.136	Fe_di(HS)3-	0.000e+000	0.000e+000	-415.277	-415.413
0.041	S(6)	1.579e-002			
0.041	CaSO4	9.217e-003	1.012e-002	-2.035	-1.995
-0.651	SO4-2	6.491e-003	1.450e-003	-2.188	-2.839
0.041	MgSO4	7.774e-005	8.537e-005	-4.109	-4.069
-0.136	NaSO4-	2.934e-006	2.144e-006	-5.533	-5.669

-0.136	HSO4-	7.130e-007	5.211e-007	-6.147	-6.283
-0.136	KSO4-	4.794e-007	3.504e-007	-6.319	-6.455
-0.136	CaHSO4+	2.999e-007	2.192e-007	-6.523	-6.659
-0.136	Fe_triSO4+	1.582e-008	1.156e-008	-7.801	-7.937
-0.136	MnSO4	1.390e-008	1.527e-008	-7.857	-7.816
0.041	Fe_diSO4	1.773e-009	1.947e-009	-8.751	-8.711
0.041	Fe_tri(SO4)2-	5.018e-010	3.667e-010	-9.299	-9.436
-0.136	Fe_triHSO4+2	4.012e-013	1.145e-013	-12.397	-12.941
-0.545	Fe_diHSO4+	6.474e-014	4.732e-014	-13.189	-13.325

Saturation indices

Phase	SI	log IAP	log KT	
Anhydrite	0.07	-4.29	-4.36	CaSO4
Aragonite	0.14	-8.20	-8.34	CaCO3
Calcite	0.28	-8.20	-8.48	CaCO3
CH4(g)	-138.48	-141.34	-2.86	CH4
CO2(g)	0.55	-0.92	-1.47	CO2
Dolomite	-1.45	-18.54	-17.09	CaMg(CO3)2
Gypsum	0.28	-4.30	-4.58	CaSO4.2H2O
H2(g)	-41.21	-44.36	-3.15	H2
H2O(g)	-1.51	-0.00	1.51	H2O
H2S(g)	-136.92	-137.92	-1.00	H2S
Halite	-5.92	-4.34	1.58	NaCl
Hausermannite	-8.93	52.10	61.03	MnSO4
Manganite	-1.11	24.23	25.34	MnOOH
CO(g)	-0.79	-3.68	-2.89	CO
Pyrochroite	-11.57	3.63	15.20	Mn(OH)2
Pyroalusite	3.45	44.83	41.38	MnO2
Rhodochrosite	-2.84	-13.97	-11.13	MnCO3
Sulfur	-101.59	-96.71	4.88	S

Reaction step 8.

WARNING: Element Fe\_di has negative moles in solution, -2.872895e-008.  
 Erroneous mole balance occurs as moles are added to produce zero moles.  
 Usually caused by KINETICS, REACTION, or diffuse layer calculation.  
 May be due to large time steps in early part of KINETICS simulation or negative concentrations in the diffuse layer.  
 WARNING: Element Fe\_di has negative moles in solution, -1.971399e-009.  
 Erroneous mole balance occurs as moles are added to produce zero moles.  
 Usually caused by KINETICS, REACTION, or diffuse layer calculation.  
 May be due to large time steps in early part of KINETICS simulation or negative concentrations in the diffuse layer.  
 WARNING: Element Fe\_di has negative moles in solution, -3.030945e-009.  
 Erroneous mole balance occurs as moles are added to produce zero moles.  
 Usually caused by KINETICS, REACTION, or diffuse layer calculation.  
 May be due to large time steps in early part of KINETICS simulation or negative concentrations in the diffuse layer.  
 WARNING: Element Fe\_di has negative moles in solution, -1.478622e-009.  
 Erroneous mole balance occurs as moles are added to produce zero moles.  
 Usually caused by KINETICS, REACTION, or diffuse layer calculation.  
 May be due to large time steps in early part of KINETICS simulation or negative concentrations in the diffuse layer.  
 WARNING: Element Fe\_di has negative moles in solution, -7.499156e-010.  
 Erroneous mole balance occurs as moles are added to produce zero moles.  
 Usually caused by KINETICS, REACTION, or diffuse layer calculation.  
 May be due to large time steps in early part of KINETICS simulation or negative concentrations in the diffuse layer.  
 WARNING: Element Fe\_di has negative moles in solution, -3.589512e-011.  
 Erroneous mole balance occurs as moles are added to produce zero moles.  
 Usually caused by KINETICS, REACTION, or diffuse layer calculation.  
 May be due to large time steps in early part of KINETICS simulation or negative concentrations in the diffuse layer.  
 Using solution 1.  
 Using pure phase assemblage 1.  
 Kinetics defined in simulation 2.

Kinetics 1. Kinetics defined in simulation 2.  
 Time step: 172800 seconds (Incremented time: 345600 seconds)

Coefficient	Rate name	Delta Moles	Total Moles	Reactant
-1	Fe_di_ox	-4.530e-008	9.998e-001	Fe_di
1				Fe_tri

-----Phase assemblage-----

Delta	Phase	Moles in assemblage			
		SI	log IAP	log KT	Initial Final
1.132e-008	O2(g)	-0.78	-3.68	-2.89	1.000e+001 1.000e+001-

Solution composition

Elements	Molality	Moles
C	1.389e-001	1.389e-001
Ca	1.476e-001	1.476e-001
Cl	2.367e-001	2.367e-001
Fe_di	1.298e-011	1.298e-011
Fe_tri	1.610e-004	1.610e-004
K	5.270e-005	5.270e-005
Mg	9.719e-004	9.719e-004
Mn	3.951e-007	3.951e-007
Na	4.183e-004	4.183e-004
S	1.579e-002	1.579e-002

Description of solution

pH	=	5.432	Charge balance
pe	=	15.170	Adjusted to redox
equilibrium	Activity of water	=	0.991
	Ionic strength	=	4.066e-001
	Mass of water (kg)	=	1.000e+000
	Total alkalinity (eq/kg)	=	2.983e-002
	Total CO2 (mol/kg)	=	1.389e-001
	Temperature (deg C)	=	25.000
	Electrical balance (eq)	=	-1.264e-009
Percent error, 100*(Cat-[An])/(Cat+[An])		=	-0.00
	Iterations	=	236
	Total H	=	1.110421e+002
	Total O	=	5.587731e+001

Distribution of species

Log Gamma	Species	Molality	Activity	Log Molality	Log Activity
-0.113	H+	4.791e-006	3.697e-006	-5.320	-5.432
-0.187	OH-	4.133e-009	2.684e-009	-8.384	-8.571
0.000	H2O	5.551e+001	9.911e-001	1.744	-0.004
C(-4)	0.000e+000				
C(4)	1.389e-001				
0.041	CO2	1.094e-001	1.201e-001	-0.961	-0.920
-0.152	HCO3-	2.035e-002	1.433e-002	-1.691	-1.844
-0.152	CaHCO3+	9.085e-003	6.396e-003	-2.042	-2.194
-0.136	MgHCO3+	5.761e-005	4.210e-005	-4.239	-4.376
0.041	CaCO3	9.729e-006	1.068e-005	-5.012	-4.971
0.041	NaHCO3	2.165e-006	2.377e-006	-5.665	-5.624
-0.610	CO3-2	7.400e-007	1.818e-007	-6.131	-6.741
-0.136	MnHCO3+	1.035e-007	7.562e-008	-6.985	-7.121
0.041	MgCO3	3.967e-008	4.356e-008	-7.402	-7.361
-0.136	NaCO3-	1.366e-009	9.986e-010	-8.864	-9.001
0.041	MnCO3	7.786e-010	8.550e-010	-9.109	-9.068
-0.136	Fe_diHCO3+	4.243e-012	3.101e-012	-11.372	-11.509
0.041	Fe_diCO3	8.593e-015	9.436e-015	-14.066	-14.025
-0.568	Ca+2	1.293e-001	3.499e-002	-0.888	-1.456
0.041	CaSO4	9.217e-003	1.012e-002	-2.035	-1.995
-0.152	CaHCO3+	9.085e-003	6.396e-003	-2.042	-2.194
0.041	CaCO3	9.729e-006	1.068e-005	-5.012	-4.971
-0.136	CaHSO4+	2.999e-007	2.192e-007	-6.523	-6.659
-0.136	CaOH+	2.130e-009	1.557e-009	-8.672	-8.808
-0.181	Cl-	2.367e-001	1.559e-001	-0.626	-0.807
-0.136	MnCl+	5.147e-008	3.761e-008	-7.288	-7.425
-0.545	Fe_triCl+2	1.201e-008	3.425e-009	-7.921	-8.465
-0.136	Fe_triCl2+	3.264e-009	2.385e-009	-8.486	-8.622
0.041	MnCl2	2.331e-009	2.560e-009	-8.632	-8.592
-0.136	MnCl3-	1.504e-010	1.099e-010	-9.823	-9.959
0.041	Fe_triCl3	3.386e-011	3.719e-011	-10.470	-10.430
-0.136	Fe_diCl+	6.373e-013	4.658e-013	-12.196	-12.332
-0.545	Fe_di+2	1.298e-011	7.587e-012	-11.120	-11.665
-0.136	Fe_diHCO3+	4.243e-012	3.101e-012	-11.372	-11.509
-0.136	Fe_diCl+	6.373e-013	4.658e-013	-12.196	-12.332
0.041	Fe_diSO4	5.081e-013	5.580e-013	-12.294	-12.253

0.041	Fe_diCO3	8.593e-015	9.436e-015	-14.066	-14.025	
-0.136	Fe_diOH+	2.511e-016	1.835e-016	-15.600	-15.736	
-0.136	Fe_diHSO4+	1.855e-017	1.356e-017	-16.732	-16.868	
0.041	Fe_di(HS)2	0.000e+000	0.000e+000	-281.608	-281.567	
-0.136	Fe_di(HS)3-	0.000e+000	0.000e+000	-418.820	-418.956	
-0.136	Fe_tri	1.610e-004				
-0.136	Fe_tri(OH)2+	1.530e-004	1.118e-004	-3.815	-3.951	
-0.545	Fe_triOH+2	4.415e-006	1.259e-006	-5.355	-5.900	
0.041	Fe_tri(OH)3	3.517e-006	3.862e-006	-5.454	-5.413	
-0.136	Fe_triSO4+	1.583e-008	1.157e-008	-7.801	-7.937	
-1.226	Fe_tri+3	1.223e-008	7.275e-010	-7.913	-9.138	
-0.545	Fe_triCl+2	1.201e-008	3.425e-009	-7.921	-8.465	
-2.179	Fe_tri2(OH)2+4	6.446e-009	4.269e-011	-8.191	-10.370	
-0.136	Fe_triCl2+	3.264e-009	2.385e-009	-8.486	-8.622	
-3.405	Fe_tri3(OH)4+5	2.532e-009	9.974e-013	-8.597	-12.001	
-0.136	Fe_tri(OH)4-	1.292e-009	9.444e-010	-8.889	-9.025	
-0.136	Fe_tri(SO4)2-	5.020e-010	3.668e-010	-9.299	-9.436	
0.041	Fe_triCl3	3.386e-011	3.719e-011	-10.470	-10.430	
-0.545	Fe_triHSO4+2	4.013e-013	1.145e-013	-12.397	-12.941	
0.041	H2	0.000e+000	0.000e+000	-44.396	-44.355	
-0.181	K+	5.270e-005	5.222e-005	3.440e-005	-4.282	-4.463
-0.136	KSO4-	4.794e-007	3.504e-007	-6.319	-6.455	
0.041	KOH	2.912e-014	3.198e-014	-13.536	-13.495	
-0.522	Mg+2	9.719e-004	8.365e-004	2.512e-004	-3.078	-3.600
0.041	MgSO4	7.774e-005	8.537e-005	-4.109	-4.069	
-0.136	MgHCO3+	5.761e-005	4.210e-005	-4.239	-4.376	
0.041	MgCO3	3.967e-008	4.356e-008	-7.402	-7.361	
-0.136	MgOH+	3.346e-010	2.445e-010	-9.476	-9.612	
-0.576	Mn+2	3.951e-007	2.230e-007	5.922e-008	-6.652	-7.228
-0.136	MnHCO3+	1.035e-007	7.562e-008	-6.985	-7.121	
-0.136	MnCl+	5.147e-008	3.761e-008	-7.288	-7.425	
0.041	MnSO4	1.390e-008	1.527e-008	-7.857	-7.816	
0.041	MnCl2	2.331e-009	2.560e-009	-8.632	-8.592	
0.041	MnCO3	7.786e-010	8.550e-010	-9.109	-9.068	
-0.136	MnCl3-	1.504e-010	1.099e-010	-9.823	-9.959	
-0.136	MnOH+	5.585e-013	4.082e-013	-12.253	-12.389	
-1.226	Mn+3	4.555e-017	4.555e-017	2.710e-018	-16.341	-17.567
-0.146	Na+	4.183e-004	4.132e-004	2.951e-004	-3.384	-3.530
-0.136	NaSO4-	2.934e-006	2.144e-006	-5.533	-5.669	
0.041	NaHCO3	2.165e-006	2.377e-006	-5.665	-5.624	
-0.136	NaCO3-	1.366e-009	9.986e-010	-8.864	-9.001	
0.041	NaOH	4.760e-013	5.227e-013	-12.322	-12.282	
0.041	O(0)	3.828e-004	1.914e-004	2.102e-004	-3.718	-3.677
0.041	S(-2)	0.000e+000	0.000e+000			
0.041	H2S	0.000e+000	0.000e+000	-137.957	-137.917	
-0.187	HS-	0.000e+000	0.000e+000	-139.239	-139.426	
-0.635	S-2	0.000e+000	0.000e+000	-146.277	-146.912	
0.041	Fe_di(HS)2	0.000e+000	0.000e+000	-281.608	-281.567	
-0.136	Fe_di(HS)3-	0.000e+000	0.000e+000	-418.820	-418.956	
0.041	CaSO4	9.217e-003	1.012e-002	-2.035	-1.995	
-0.651	SO4-2	6.491e-003	1.450e-003	-2.188	-2.839	
0.041	MgSO4	7.774e-005	8.537e-005	-4.109	-4.069	
-0.136	NaSO4-	2.934e-006	2.144e-006	-5.533	-5.669	
-0.136	HSO4-	7.130e-007	5.211e-007	-6.147	-6.283	
-0.136	KSO4-	4.794e-007	3.504e-007	-6.319	-6.455	
-0.136	CaHSO4+	2.999e-007	2.192e-007	-6.523	-6.659	

-0.136	Fe_triSO4+	1.583e-008	1.157e-008	-7.801	-7.937
0.041	MnSO4	1.390e-008	1.527e-008	-7.857	-7.816
-0.136	Fe_tri(SO4)2-	5.020e-010	3.668e-010	-9.299	-9.436
0.041	Fe_diSO4	5.081e-013	5.580e-013	-12.294	-12.253
-0.545	Fe_triHSO4+2	4.013e-013	1.145e-013	-12.397	-12.941
-0.136	Fe_diHSO4+	1.855e-017	1.356e-017	-16.732	-16.868

Saturation indices

Phase	SI	log IAP	log KT		
Anhydrite	0.07	-4.29	-4.36	CaSO4	
Aragonite	0.14	-8.20	-8.34	CaCO3	
Calcite	0.28	-8.20	-8.48	CaCO3	
CH4(g)	-138.48	-141.34	-2.86	CH4	
CO2(g)	0.55	-0.92	-1.47	CO2	
Dolomite	-1.45	-18.54	-17.09	CaMg(CO3)2	
Gypsum	0.28	-4.30	-4.58	CaSO4·2H2O	
H2(g)	-41.21	-44.36	-3.15	H2	
H2O(g)	-1.51	-0.00	1.51	H2O	
H2S(g)	-136.92	-137.92	-1.00	H2S	
Halite	-5.92	-4.34	1.58	NaCl	
Hausmannite	-8.93	52.10	61.03	Mn3O4	
Manganite	-1.11	24.23	25.34	MnOOH	
O2(g)	-0.78	-3.68	-2.89	O2	
Pyrochroite	-11.57	3.63	15.20	Mn(CH)2	
Pyrolusite	3.45	44.83	41.38	MnO2	
Rhodochrosite	-2.84	-13.97	-11.13	MnCO3	
Sulfur	-101.59	-96.71	4.88	S	

Reaction step 9.

WARNING: Element Fe\_di has negative moles in solution, -8.232164e-012.  
 Erroneous mole balance occurs as moles are added to produce zero moles.  
 Usually caused by KINETICS, REACTION, or diffuse layer calculation.  
 May be due to large time steps in early part of KINETICS simulation or negative concentrations in the diffuse layer.  
 WARNING: Element Fe\_di has negative moles in solution, -5.648819e-013.  
 Erroneous mole balance occurs as moles are added to produce zero moles.  
 Usually caused by KINETICS, REACTION, or diffuse layer calculation.  
 May be due to large time steps in early part of KINETICS simulation or negative concentrations in the diffuse layer.  
 WARNING: Element Fe\_di has negative moles in solution, -8.685081e-013.  
 Erroneous mole balance occurs as moles are added to produce zero moles.  
 Usually caused by KINETICS, REACTION, or diffuse layer calculation.  
 May be due to large time steps in early part of KINETICS simulation or negative concentrations in the diffuse layer.  
 WARNING: Element Fe\_di has negative moles in solution, -6.920311e-013.  
 Erroneous mole balance occurs as moles are added to produce zero moles.  
 Usually caused by KINETICS, REACTION, or diffuse layer calculation.  
 May be due to large time steps in early part of KINETICS simulation or negative concentrations in the diffuse layer.  
 WARNING: Element Fe\_di has negative moles in solution, -2.148874e-013.  
 Erroneous mole balance occurs as moles are added to produce zero moles.  
 Usually caused by KINETICS, REACTION, or diffuse layer calculation.  
 May be due to large time steps in early part of KINETICS simulation or negative concentrations in the diffuse layer.  
 Using solution 1.  
 Using pure phase assemblage 1.  
 Using kinetics 1. Kinetics defined in simulation 2.

Kinetics 1. Kinetics defined in simulation 2.

Time step: 172800 seconds (Incremented time: 518400 seconds)

Coefficient	Rate name	Delta Moles	Total Moles	Reactant
-1	Fe_di_cx	-1.298e-011	9.998e-001	Fe_di
1				Fe_tri

Phase assemblage

Delta	Phase	Moles in assemblage			
		SI	log IAP	log KT	Initial Final
3.196e-012	O2(g)	-0.78	-3.68	-2.89	1.000e+001 1.000e+001-

Solution composition

Elements	Molality	Moles
----------	----------	-------

C	1.389e-001	1.389e-001
Ca	1.476e-001	1.476e-001
Cl	2.367e-001	2.367e-001
Fe_di	3.720e-015	3.720e-015
Fe_tri	1.610e-004	1.610e-004
K	5.270e-005	5.270e-005
Mg	9.719e-004	9.719e-004
Mn	3.951e-007	3.951e-007
Na	4.183e-004	4.183e-004
S	1.579e-002	1.579e-002

Description of solution

pH = 5.432  
 pe = 15.170  
 Charge balance Adjusted to redox

equilibrium

Activity of water = 0.991  
 Ionic strength = 4.066e-001  
 Mass of water (kg) = 1.000e+000  
 Total alkalinity (eq/kg) = 2.983e-002  
 Total CO2 (mol/kg) = 1.389e-001  
 Temperature (deg C) = 25.000  
 Electrical balance (eq) = -1.265e-009  
 Percent error, 100\*(Cat-[An])/([Cat+[An])) = -0.00  
 Iterations = 233  
 Total H = 1.110421e+002  
 Total O = 5.587731e+001

Distribution of species

Log Gamma	Species	Molality	Activity	Log Molality	Log Activity
-0.113	H+	4.791e-006	3.697e-006	-5.320	-5.432
-0.187	OH-	4.133e-009	2.684e-009	-8.384	-8.571
0.000	C(-4)	0.000e+000	0.000e+000	-141.384	-141.343
0.041	CH4	0.000e+000	0.000e+000	-141.384	-141.343
0.041	CO2	1.094e-001	1.201e-001	-0.961	-0.920
-0.152	HCO3-	2.035e-002	1.433e-002	-1.691	-1.844
-0.152	CaHCO3+	9.085e-003	6.396e-003	-2.042	-2.194
-0.136	MgHCO3+	5.761e-005	4.210e-005	-4.239	-4.376
0.041	CaCO3	9.729e-006	1.068e-005	-5.012	-4.971
0.041	NaHCO3	2.165e-006	2.377e-006	-5.665	-5.624
-0.610	CO3-2	7.400e-007	1.818e-007	-6.131	-6.741
-0.136	MnHCO3+	1.035e-007	7.562e-008	-6.985	-7.121
0.041	MgCO3	3.967e-008	4.356e-008	-7.402	-7.361
-0.136	NaCO3-	1.366e-009	9.986e-010	-8.864	-9.001
0.041	MnCO3	7.786e-010	8.550e-010	-9.109	-9.068
-0.136	Fe_diHCO3+	1.216e-015	8.885e-016	-14.915	-15.051
0.041	Fe_diCO3	2.462e-018	2.704e-018	-17.609	-17.568
-0.568	Ca+2	1.293e-001	3.499e-002	-0.888	-1.456
0.041	CaSO4	9.217e-003	1.012e-002	-2.035	-1.995
-0.152	CaHCO3+	9.085e-003	6.396e-003	-2.042	-2.194
0.041	CaCO3	9.729e-006	1.068e-005	-5.012	-4.971
-0.136	CaHSO4+	2.999e-007	2.192e-007	-6.523	-6.659
-0.136	CaOH+	2.130e-009	1.557e-009	-8.672	-8.808
-0.181	Cl-	2.367e-001	1.559e-001	-0.626	-0.807
-0.136	MnCl+	5.147e-008	3.761e-008	-7.288	-7.425
-0.545	Fe_triCl+2	1.201e-008	3.425e-009	-7.921	-8.465
-0.136	Fe_triCl2+	3.264e-009	2.385e-009	-8.486	-8.622
0.041	MnCl2	2.331e-009	2.560e-009	-8.632	-8.592
-0.136	MnCl3-	1.504e-010	1.099e-010	-9.823	-9.959
0.041	Fe_triCl3	3.386e-011	3.719e-011	-10.470	-10.430
-0.136	Fe_diCl+	1.826e-016	1.335e-016	-15.738	-15.875
-0.545	Fe_di+2	3.720e-015	6.202e-016	-14.663	-15.207
-0.136	Fe_diHCO3+	1.216e-015	8.885e-016	-14.915	-15.051
-0.136	Fe_diCl+	1.826e-016	1.335e-016	-15.738	-15.875
0.041	Fe_diSO4	1.456e-016	1.599e-016	-15.837	-15.796
0.041	Fe_diCO3	2.462e-018	2.704e-018	-17.609	-17.568
-0.136	Fe_diOH+	7.195e-020	5.258e-020	-19.143	-19.279
-0.136	Fe_diHSO4+	5.316e-021	3.885e-021	-20.274	-20.411

0.041	Fe_di (HS)2	0.000e+000	0.000e+000	-285.150	-285.110
-0.136	Fe_di (HS)3-	0.000e+000	0.000e+000	-422.363	-422.499
Fe_tri	1.610e-004				
-0.136	Fe_tri (H)2+	1.530e-004	1.118e-004	-3.815	-3.951
-0.545	Fe_triOH+2	4.415e-006	1.259e-006	-5.355	-5.900
0.041	Fe_tri (H)3	3.517e-006	3.862e-006	-5.454	-5.413
-0.136	Fe_trisO4+	1.583e-008	1.157e-008	-7.801	-7.937
-1.226	Fe_tri+3	1.223e-008	7.275e-010	-7.913	-9.138
-0.545	Fe_triCl+2	1.201e-008	3.425e-009	-7.921	-8.465
-2.179	Fe_tri2 (H)2+4	6.446e-009	4.269e-011	-8.191	-10.370
-0.136	Fe_triCl2+	3.264e-009	2.385e-009	-8.486	-8.622
-3.405	Fe_tri3 (H)4+5	2.532e-009	9.974e-013	-8.597	-12.001
-0.136	Fe_tri (H)4-	1.292e-009	9.444e-010	-8.889	-9.025
-0.136	Fe_tri (SO4)2-	5.020e-010	3.668e-010	-9.299	-9.436
0.041	Fe_triCl3	3.386e-011	3.719e-011	-10.470	-10.430
-0.545	Fe_trisO4+2	4.013e-013	1.145e-013	-12.397	-12.941
H(0)	0.000e+000				
0.041	H2	0.000e+000	0.000e+000	-44.396	-44.355
K	5.270e-005				
-0.181	K+	5.222e-005	3.440e-005	-4.282	-4.463
-0.136	KSO4-	4.794e-007	3.504e-007	-6.319	-6.455
0.041	KOH	2.912e-014	3.198e-014	-13.536	-13.495
Mg	9.719e-004				
-0.522	Mg+2	8.365e-004	2.512e-004	-3.078	-3.600
0.041	MgSO4	7.774e-005	8.537e-005	-4.109	-4.069
-0.136	MgHCO3+	5.761e-005	4.210e-005	-4.239	-4.376
0.041	MgCO3	3.967e-008	4.356e-008	-7.402	-7.361
-0.136	MgOH+	3.346e-010	2.445e-010	-9.476	-9.612
Mn(2)	3.951e-007				
-0.576	Mn+2	2.230e-007	5.922e-008	-6.652	-7.228
-0.136	MnHCO3+	1.035e-007	7.562e-008	-6.985	-7.121
-0.136	MnCl+	5.147e-008	3.761e-008	-7.288	-7.425
0.041	MnSO4	1.390e-008	1.527e-008	-7.857	-7.816
0.041	MnCl2	2.331e-009	2.560e-009	-8.632	-8.592
0.041	MnCO3	7.786e-010	8.550e-010	-9.109	-9.068
-0.136	MnCl3-	1.504e-010	1.099e-010	-9.823	-9.959
-0.136	MnOH+	5.585e-013	4.082e-013	-12.253	-12.389
Mn(3)	4.555e-017				
-1.226	Mn+3	4.555e-017	2.710e-018	-16.341	-17.567
Na	4.183e-004				
-0.146	Na+	4.132e-004	2.951e-004	-3.384	-3.530
-0.136	NaSO4-	2.934e-006	2.144e-006	-5.533	-5.669
0.041	NaHCO3	2.165e-006	2.377e-006	-5.665	-5.624
-0.136	NaCO3-	1.366e-009	9.986e-010	-8.864	-9.001
0.041	NaOH	4.760e-013	5.227e-013	-12.322	-12.282
O(0)	3.828e-004				
0.041	O2	1.914e-004	2.102e-004	-3.718	-3.677
S(-2)	0.000e+000				
0.041	H2S	0.000e+000	0.000e+000	-137.957	-137.917
-0.187	HS-	0.000e+000	0.000e+000	-139.239	-139.426
-0.635	S-2	0.000e+000	0.000e+000	-146.277	-146.912
0.041	Fe_di (HS)2	0.000e+000	0.000e+000	-285.150	-285.110
-0.136	Fe_di (HS)3-	0.000e+000	0.000e+000	-422.363	-422.499
S(6)	1.579e-002				
0.041	CaSO4	9.217e-003	1.012e-002	-2.035	-1.995
-0.651	SO4-2	6.491e-003	1.450e-003	-2.188	-2.839
0.041	MgSO4	7.774e-005	8.537e-005	-4.109	-4.069
-0.136	NaSO4-	2.934e-006	2.144e-006	-5.533	-5.669
-0.136	HSO4-	7.130e-007	5.211e-007	-6.147	-6.283
-0.136	KSO4-	4.794e-007	3.504e-007	-6.319	-6.455
-0.136	CaHSO4+	2.999e-007	2.192e-007	-6.523	-6.659
-0.136	Fe_trisO4+	1.583e-008	1.157e-008	-7.801	-7.937
0.041	MnSO4	1.390e-008	1.527e-008	-7.857	-7.816
-0.136	Fe_tri (SO4)2-	5.020e-010	3.668e-010	-9.299	-9.436

-0.545	Fe_trisO4+2	4.013e-013	1.145e-013	-12.397	-12.941
0.041	Fe_disO4	1.456e-016	1.599e-016	-15.837	-15.796
-0.136	Fe_disO4+	5.316e-021	3.885e-021	-20.274	-20.411

Saturation indices

Phase	SI	log IAP	log KT	
Anhydrite	0.07	-4.29	-4.36	CaSO4
Aragonite	0.14	-8.20	-8.34	CaCO3
Calcite	0.28	-8.20	-8.48	CaCO3
CH4(g)	-139.48	-141.34	-2.86	CH4
CO2(g)	0.55	-0.92	-1.47	CO2
Dolomite	-1.45	-18.54	-17.09	CaMg(CO3)2
Gypsum	0.28	-4.30	-4.58	CaSO4·2H2O
H2(g)	-41.21	-44.36	-3.15	H2
H2O(g)	-1.51	-0.00	1.51	H2O
H2S(g)	-136.92	-137.92	-1.00	H2S
Halite	-5.92	-4.34	1.58	NaCl
Hausmannite	-8.93	52.10	61.03	Mn3O4
Manganite	-1.11	24.23	25.34	MnOOH
O2(g)	-0.78	-3.68	-2.89	O2
Pyrochroite	-11.57	3.63	15.20	Mn(OH)2
Pyrolusite	3.45	44.83	41.38	MnO2
Rhodochrosite	-2.84	-13.97	-11.13	MnCO3
Sulfur	-101.59	-96.71	4.88	S

Reaction step 10.

WARNING: Element Fe\_di has negative moles in solution, -2.358917e-015.  
Erroneous mole balance occurs as moles are added to produce zero moles.

Usually caused by KINETICS, REACTION, or diffuse layer calculation.  
May be due to large time steps in early part of KINETICS simulation or negative concentrations in the diffuse layer.

WARNING: Element Fe\_di has negative moles in solution, -1.618662e-016.  
Erroneous mole balance occurs as moles are added to produce zero moles.

Usually caused by KINETICS, REACTION, or diffuse layer calculation.  
May be due to large time steps in early part of KINETICS simulation or negative concentrations in the diffuse layer.

WARNING: Element Fe\_di has negative moles in solution, -2.488700e-016.  
Erroneous mole balance occurs as moles are added to produce zero moles.

Usually caused by KINETICS, REACTION, or diffuse layer calculation.  
May be due to large time steps in early part of KINETICS simulation or negative concentrations in the diffuse layer.

WARNING: Element Fe\_di has negative moles in solution, -1.983007e-016.  
Erroneous mole balance occurs as moles are added to produce zero moles.

Usually caused by KINETICS, REACTION, or diffuse layer calculation.  
May be due to large time steps in early part of KINETICS simulation or negative concentrations in the diffuse layer.

WARNING: Element Fe\_di has negative moles in solution, -1.214100e-016.  
Erroneous mole balance occurs as moles are added to produce zero moles.

Usually caused by KINETICS, REACTION, or diffuse layer calculation.  
May be due to large time steps in early part of KINETICS simulation or negative concentrations in the diffuse layer.

WARNING: Element Fe\_di has negative moles in solution, -6.157574e-017.  
Erroneous mole balance occurs as moles are added to produce zero moles.

Usually caused by KINETICS, REACTION, or diffuse layer calculation.  
May be due to large time steps in early part of KINETICS simulation or negative concentrations in the diffuse layer.

WARNING: Element Fe\_di has negative moles in solution, -2.947357e-018.  
Erroneous mole balance occurs as moles are added to produce zero moles.

Usually caused by KINETICS, REACTION, or diffuse layer calculation.  
May be due to large time steps in early part of KINETICS simulation or negative concentrations in the diffuse layer.

Using solution 1.  
Using pure phase assemblage 1.  
Using kinetics 1. Kinetics defined in simulation 2.

Kinetics 1. Kinetics defined in simulation 2.

Time step: 172800 seconds (Incremented time: 691200 seconds)

Rate name Delta Moles Total Moles Reactant

Coefficient

-1 Fe\_di\_ox -3.886e-015 9.998e-001 Fe\_di

1 Fe\_tri

Phase assemblage

Phase SI log IAP log KT Moles in assemblage Initial Final

Delta

02(g) -0.78 -3.68 -2.89 1.000e+001 1.000e+001

1.048e-013

Solution composition

Elements Molality Moles

C 1.389e-001 1.389e-001

Ca 1.476e-001 1.476e-001

Cl 2.367e-001 2.367e-001

Fe\_di 1.066e-018 1.066e-018

Fe\_tri 1.610e-004 1.610e-004

K 5.270e-005 5.270e-005

Log	Species	Molality	Activity	Log Molality	Log Activity
-0.113	H+	4.791e-006	3.697e-006	-5.320	-5.432
-0.187	OH-	4.133e-009	2.684e-009	-8.384	-8.571
0.000	H2O	5.551e+001	9.911e-001	1.744	-0.004
C(-4)	CH4	0.000e+000	0.000e+000	-141.384	-141.343
0.041	CO2	1.389e-001	1.094e-001	-0.961	-0.920
0.041	HCO3-	2.035e-002	1.433e-002	-1.691	-1.844
-0.152	CaHCO3+	9.085e-003	6.396e-003	-2.042	-2.194
-0.152	MgHCO3+	5.761e-005	4.210e-005	-4.239	-4.376
-0.136	CaCO3	9.729e-006	1.068e-005	-5.012	-4.971
0.041	NaHCO3	2.165e-006	2.377e-006	-5.665	-5.624
-0.610	CO3-2	7.400e-007	1.818e-007	-6.131	-6.741
-0.136	MnHCO3+	1.035e-007	7.562e-008	-6.985	-7.121
0.041	MgCO3	3.967e-008	4.356e-008	-7.402	-7.361
-0.136	NaCO3-	1.366e-009	9.986e-010	-8.864	-9.001
0.041	MnCO3	7.786e-010	8.550e-010	-9.109	-9.068
-0.136	Fe_dihCO3+	3.484e-019	2.546e-019	-18.458	-18.594
0.041	Fe_dico3	7.056e-022	7.748e-022	-21.151	-21.111
-0.568	Ca+2	1.476e-001	1.293e-001	-0.888	-1.456
0.041	CaSO4	9.217e-003	1.012e-002	-2.035	-1.995
-0.152	CaHCO3+	9.085e-003	6.396e-003	-2.042	-2.194
0.041	CaCO3	9.729e-006	1.068e-005	-5.012	-4.971
-0.136	CaHSO4+	2.999e-007	2.192e-007	-6.523	-6.659
-0.136	CaOH+	2.130e-009	1.557e-009	-8.672	-8.808
-0.181	Cl-	2.367e-001	2.367e-001	-0.626	-0.807
-0.136	MnCl+	5.147e-008	3.761e-008	-7.288	-7.425
-0.545	Fe_triCl+2	1.201e-008	3.425e-009	-7.921	-8.465
-0.136	Fe_triCl2+	3.264e-009	2.385e-009	-8.486	-8.622
0.041	MnCl2	2.331e-009	2.560e-009	-8.632	-8.592
-0.136	MnCl3-	1.504e-010	1.099e-010	-9.823	-9.959
0.041	Fe_triCl3	3.386e-011	3.719e-011	-10.470	-10.430
-0.136	Fe_dicl+	5.233e-020	3.824e-020	-19.281	-19.417
-0.545	Fe_dii+2	1.066e-018	6.230e-019	-18.206	-18.750
-0.136	Fe_dihCO3+	3.484e-019	2.546e-019	-18.458	-18.594
-0.136	Fe_dicl+	5.233e-020	3.824e-020	-19.281	-19.417
0.041	Fe_disO4	4.172e-020	4.582e-020	-19.380	-19.339
0.041	Fe_dico3	7.056e-022	7.748e-022	-21.151	-21.111
-0.136	Fe_dioH+	2.062e-023	1.507e-023	-22.686	-22.822
-0.136	Fe_dihSO4+	1.523e-024	1.113e-024	-23.817	-23.953
0.041	Fe_di(HS)2	0.000e+000	0.000e+000	-288.693	-288.653
-0.136	Fe_di(HS)3-	0.000e+000	0.000e+000	-425.906	-426.042
-0.136	Fe_tri(HS)2+	1.610e-004	1.530e-004	-3.815	-3.951

-0.545	Fe_triOH+2	4.415e-006	1.259e-006	-5.355	-5.900
0.041	Fe_tri(OH)3	3.517e-006	3.862e-006	-5.454	-5.413
-0.136	Fe_triSO4+	1.583e-008	1.157e-008	-7.801	-7.937
-1.226	Fe_tri+3	1.223e-008	7.275e-010	-7.913	-9.138
-0.545	Fe_triCl+2	1.201e-008	3.425e-009	-7.921	-8.465
-2.179	Fe_tri2(OH)2+4	6.446e-009	4.269e-011	-8.191	-10.370
-0.136	Fe_triCl2+	3.264e-009	2.385e-009	-8.486	-8.622
-3.405	Fe_tri3(OH)4+5	2.532e-009	9.974e-013	-8.597	-12.001
-0.136	Fe_tri(OH)4-	1.292e-009	9.444e-010	-8.889	-9.025
-0.136	Fe_tri(SO4)2-	5.020e-010	3.668e-010	-9.299	-9.436
0.041	Fe_triCl3	3.386e-011	3.719e-011	-10.470	-10.430
-0.545	Fe_trihSO4+2	4.013e-013	1.145e-013	-12.397	-12.941
0.000e+000	H(0)	0.000e+000	0.000e+000	-44.396	-44.355
0.041	K+	5.270e-005	5.222e-005	-4.282	-4.463
-0.181	KSO4-	4.794e-007	3.504e-007	-6.319	-6.455
-0.136	KOH	2.912e-014	3.198e-014	-13.536	-13.495
0.041	Mg+2	9.719e-004	8.365e-004	-3.078	-3.600
-0.522	MgSO4	7.774e-005	8.537e-005	-4.109	-4.069
0.041	MgHCO3+	5.761e-005	4.210e-005	-4.239	-4.376
-0.136	MgCO3	3.967e-008	4.356e-008	-7.402	-7.361
0.041	MgOH+	3.346e-010	2.445e-010	-9.476	-9.612
-0.136	Mn(2)	3.951e-007	2.230e-007	-5.922e-008	-6.652
-0.576	MnHCO3+	1.035e-007	7.562e-008	-6.985	-7.121
-0.136	MnCl+	5.147e-008	3.761e-008	-7.288	-7.425
-0.136	MnSO4	1.390e-008	1.527e-008	-7.857	-7.816
0.041	MnCl2	2.331e-009	2.560e-009	-8.632	-8.592
0.041	MnCO3	7.786e-010	8.550e-010	-9.109	-9.068
-0.136	MnCl3-	1.504e-010	1.099e-010	-9.823	-9.959
-0.136	MnOH+	5.585e-013	4.082e-013	-12.253	-12.389
-1.226	Mn(3)	4.555e-017	4.555e-017	-2.710e-018	-16.341
-0.146	Na+	4.183e-004	4.132e-004	-2.951e-004	-3.384
-0.136	NaSO4-	2.934e-006	2.144e-006	-5.533	-5.669
0.041	NaHCO3	2.165e-006	2.377e-006	-5.665	-5.624
-0.136	NaCO3-	1.366e-009	9.986e-010	-8.864	-9.001
0.041	NaOH	4.760e-013	5.227e-013	-12.322	-12.282
0.041	O(0)	3.828e-004	1.914e-004	2.102e-004	-3.718
0.041	S(-2)	0.000e+000	0.000e+000	-137.957	-137.917
-0.187	HS-	0.000e+000	0.000e+000	-139.239	-139.426
-0.635	S-2	0.000e+000	0.000e+000	-146.277	-146.912
0.041	Fe_di(HS)2	0.000e+000	0.000e+000	-288.693	-288.653
-0.136	Fe_di(HS)3-	0.000e+000	0.000e+000	-425.906	-426.042
0.041	CaSO4	9.217e-003	1.012e-002	-2.035	-1.995
-0.651	SO4-2	6.491e-003	1.450e-003	-2.188	-2.839
0.041	MgSO4	7.774e-005	8.537e-005	-4.109	-4.069
-0.136	NaSO4-	2.934e-006	2.144e-006	-5.533	-5.669
-0.136	HSO4-	7.130e-007	5.211e-007	-6.147	-6.283
-0.136	KSO4-	4.794e-007	3.504e-007	-6.319	-6.455
-0.136	CaHSO4+	2.999e-007	2.192e-007	-6.523	-6.659
-0.136	Fe_triSO4+	1.583e-008	1.157e-008	-7.801	-7.937
0.041	MnSO4	1.390e-008	1.527e-008	-7.857	-7.816
-0.136	Fe_tri(SO4)2-	5.020e-010	3.668e-010	-9.299	-9.436
-0.545	Fe_trihSO4+2	4.013e-013	1.145e-013	-12.397	-12.941
0.041	Fe_disO4	4.172e-020	4.582e-020	-19.380	-19.339
-0.136	Fe_dihSO4+	1.523e-024	1.113e-024	-23.817	-23.953



-1.226	Fe_tri+3	1.223e-008	7.275e-010	-7.913	-9.138
-0.545	Fe_triCl+2	1.201e-008	3.425e-009	-7.921	-8.465
-2.179	Fe_tri2(OH)2+4	6.446e-009	4.269e-011	-8.191	-10.370
-0.136	Fe_triCl2+	3.264e-009	2.385e-009	-8.486	-8.622
-3.405	Fe_tri3(OH)4+5	2.532e-009	9.974e-013	-8.597	-12.001
-0.136	Fe_tri(OH)4-	1.292e-009	9.444e-010	-8.889	-9.025
-0.136	Fe_tri(SO4)2-	5.020e-010	3.668e-010	-9.299	-9.436
-0.136	Fe_triCl3	3.386e-011	3.719e-011	-10.470	-10.430
0.041	Fe_triHSO4+2	4.013e-013	1.145e-013	-12.397	-12.941
-0.545	H(0)	0.000e+000			
0.041	H2	0.000e+000	0.000e+000	-44.396	-44.355
K	5.270e-005				
-0.181	K+	5.222e-005	3.440e-005	-4.282	-4.463
-0.136	KSO4-	4.794e-007	3.504e-007	-6.319	-6.455
0.041	KOH	2.912e-014	3.198e-014	-13.536	-13.495
Mg	9.719e-004				
-0.522	Mg+2	8.365e-004	2.512e-004	-3.078	-3.600
0.041	MgSO4	7.774e-005	8.537e-005	-4.109	-4.069
-0.136	MgHCO3+	5.761e-005	4.210e-005	-4.239	-4.376
-0.136	MgCO3	3.967e-008	4.356e-008	-7.402	-7.361
0.041	MgOH+	3.346e-010	2.445e-010	-9.476	-9.612
-0.136	Mn(2)	3.951e-007			
-0.576	Mn+2	2.230e-007	5.922e-008	-6.652	-7.228
-0.136	MnHCO3+	1.035e-007	7.562e-008	-6.985	-7.121
-0.136	MnCl+	5.147e-008	3.761e-008	-7.288	-7.425
0.041	MnSO4	1.390e-008	1.527e-008	-7.857	-7.816
0.041	MnCl2	2.331e-009	2.560e-009	-8.632	-8.592
0.041	MnCO3	7.786e-010	8.550e-010	-9.109	-9.068
-0.136	MnCl3-	1.504e-010	1.099e-010	-9.823	-9.959
-0.136	MnOH+	5.585e-013	4.082e-013	-12.253	-12.389
Mn(3)	4.555e-017				
-1.226	Mn+3	4.555e-017	2.710e-018	-16.341	-17.567
Na	4.183e-004				
-0.146	Na+	4.132e-004	2.951e-004	-3.384	-3.530
-0.136	NaSO4-	2.934e-006	2.144e-006	-5.533	-5.669
0.041	NaHCO3	2.165e-006	2.377e-006	-5.665	-5.624
-0.136	NaCO3-	1.366e-009	9.986e-010	-8.864	-9.001
0.041	NaOH	4.760e-013	5.227e-013	-12.322	-12.282
0(0)	O2	3.828e-004			
0.041	O(-2)	1.914e-004	2.102e-004	-3.718	-3.677
		0.000e+000			

0.041	H2S	0.000e+000	0.000e+000	-137.957	-137.917
-0.187	HS-	0.000e+000	0.000e+000	-139.239	-139.426
-0.635	S-2	0.000e+000	0.000e+000	-146.277	-146.912
0.041	Fe_di(HS)2	0.000e+000	0.000e+000	-292.236	-292.195
-0.136	Fe_di(HS)3-	0.000e+000	0.000e+000	-429.448	-429.585
S(6)	1.579e-002				
0.041	CaSO4	9.217e-003	1.012e-002	-2.035	-1.995
-0.651	SO4-2	6.491e-003	1.450e-003	-2.188	-2.839
0.041	MgSO4	7.774e-005	8.537e-005	-4.109	-4.069
-0.136	NaSO4-	2.934e-006	2.144e-006	-5.533	-5.669
-0.136	HSD4-	7.130e-007	5.211e-007	-6.147	-6.283
-0.136	KSO4-	4.794e-007	3.504e-007	-6.319	-6.455
-0.136	CaHSO4+	2.999e-007	2.192e-007	-6.523	-6.659
-0.136	Fe_triSO4+	1.583e-008	1.157e-008	-7.801	-7.937
-0.136	MnSO4	1.390e-008	1.527e-008	-7.857	-7.816
0.041	Fe_tri(SO4)2-	5.020e-010	3.668e-010	-9.299	-9.436
-0.545	Fe_triHSO4+2	4.013e-013	1.145e-013	-12.397	-12.941
0.041	Fe_diSO4	1.196e-023	1.313e-023	-22.922	-22.882
-0.136	Fe_diHSO4+	4.365e-028	3.190e-028	-27.360	-27.496

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Saturation indices

Phase	SI	log IAP	log KT	
Anhydrite	0.07	-4.29	-4.36	CaSO4
Aragonite	0.14	-8.20	-8.34	CaCO3
Calcite	0.28	-8.20	-8.48	CaCO3
CHA(g)	-138.48	-141.34	-2.86	CHA
CO2(g)	0.55	-0.92	-1.47	CO2
Dolomite	-1.45	-18.54	-17.09	CaMg(CO3)2
Gypsum	0.28	-4.30	-4.58	CaSO4.2H2O
H2(g)	-41.21	-44.36	-3.15	H2
H2O(g)	-1.51	-0.00	1.51	H2O
H2S(g)	-136.92	-137.92	-1.00	H2S
Halite	-5.92	-4.34	1.58	NaCl
Hausmannite	-8.93	52.10	61.03	Mn3O4
Manganite	-1.11	24.23	25.34	MnOOH
O2(g)	-0.78	-3.68	-2.89	O2
Pyrochroite	-11.57	3.63	15.20	Mn(OH)2
Pyrolusite	3.45	44.83	41.38	MnO2
Rhodochrosite	-2.84	-13.97	-11.13	MnCO3
Sulfur	-101.59	-96.71	4.88	S

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End of simulation.

-----  
Reading input data for simulation 3.

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End of nn.

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END



### B-3: PHREEQC Partial Output File

Days	Fe(2)	Fe(3)	pH	si_Fe(OH)3(a)
0.0000e+000	1.6100e+002	0.0000e+000	5.4344e+000	-9.9990e+001
1.1574e-003	1.6023e+002	7.6792e-001	5.4344e+000	-9.9990e+001
5.7870e-003	1.5720e+002	3.7999e+000	5.4344e+000	-9.9990e+001
4.1667e-002	1.3558e+002	2.5417e+001	5.4341e+000	-9.9990e+001
1.6667e-001	8.1085e+001	7.9915e+001	5.4333e+000	-9.9990e+001
4.1667e-001	2.9106e+001	1.3189e+002	5.4326e+000	-9.9990e+001
1.0000e+000	2.6813e+000	1.5832e+002	5.4322e+000	-9.9990e+001
2.0000e+000	4.5311e-002	1.6095e+002	5.4322e+000	-9.9990e+001
4.0000e+000	1.2984e-005	1.6100e+002	5.4322e+000	-9.9990e+001
6.0000e+000	3.7205e-009	1.6100e+002	5.4322e+000	-9.9990e+001
8.0000e+000	1.0661e-012	1.6100e+002	5.4322e+000	-9.9990e+001
1.0000e+001	3.0549e-016	1.6100e+002	5.4322e+000	-9.9990e+001

## Appendix C. Iron Standards Calculations

**Table C-1: Standards Calculations**

<b>Formula Weight, FeCl<sub>3</sub> (g/mol)</b>	270.32
<b>Molar Weight, Fe (g/mol)</b>	55.847
<b>Actual Weight of Compound*, FeCl<sub>3</sub> (g)</b>	0.495
<b>Volume of flask (L)</b>	1
<b>Desired Conc. (mg/L)</b>	100
<b>Desired Mass</b>	100
<b>Mass of Compound to produce desired [Fe] (mg)</b>	484.0367

**Table C-2: Iron Standards**

Stand. [C]	Vol.(mL)	Actual Vol (mL)*	Actual Dilution (ppm)
1	0.977852	1	1.02265
2	1.955704	2	2.0453
5	4.88926	5	5.11325
8	7.822816	8	8.1812
50	48.8926	50	51.1325

\*measured quantity

